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Jilei Liu

# Graphene-Based Composites for Electrochemical Energy Storage



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Jilei Liu

# Graphene-Based Composites for Electrochemical Energy Storage

Doctoral Thesis accepted by  
the Nanyang Technological University, Singapore

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# Supervisor's Foreword

Achieving secure, clean, and sustainable energy production, storage, and consumption are, perhaps, the greatest technical and social challenges that the world are facing. The key achievement is not only to explore renewable and sustainable energy sources, but also, perhaps even more importantly, to store energy efficiently and deliver on demand. The realization of high-performance electrochemical energy storage devices is no doubt strongly dependent on the achievements of multidisciplinary sciences, including materials sciences, chemical sciences, and physical sciences. Graphene, a single atomic layer of  $sp^2$ -bonded carbon atoms, has attracted worldwide interest because of its intrinsic difference from other forms of carbon allotropes. Graphene is particularly suitable for the implementation in electrochemical applications due to its remarkable electrical conductivity, large specific surface area, unique heterogeneous electron transfer and charge carrier rates, and good electrochemical stability.

In this thesis, Dr. Jilei Liu focuses on the synthesis and characterization of various carbon allotropes (e.g., graphene oxide/graphene, graphene foam (GF), and GF/carbon nanotubes (CNTs) hybrids), and their composites for electrochemical energy storage. This thesis is broad sweeping in its scope spanning from materials synthesis to electrochemical analysis to state-of-the-art electrochemical energy storage devices. Major improvements in graphene preparation, electrochemical characterization, and flexible energy storage device design have been obtained: (1) a simple, green and cost-effective electrochemical exfoliation method has been designed for synthesizing high-quality graphene in gram-scale, paving the way for commercial applications of graphene; (2) Three-dimensional graphene foam (GF)/carbon nanotubes (CNTs) hybrid films with good electric and mechanical properties were prepared, opening up new ideas for applications of graphene, especially in flexible energy storage devices; (3) Flexible energy storage devices such as asymmetric supercapacitors and aqueous alkaline nickel/iron batteries have been designed based on GF/CNTs hybrid films. Benefiting from the ultra-light and thin features of the GF/CNTs current collectors, these fabricated cells display high

gravimetric/volumetric energy density/power density and good cycling performance, demonstrating practical significance.

This is exquisite and creative work. The unique experimental procedures and methods, the systematic electrochemical analysis, as well as the creative flexible energy storage device design in this thesis may provide valuable reference for researchers in the field of carbon-based electrochemical energy storage.

Singapore  
May 2016

Prof. Zexiang Shen

**Parts of this thesis have been published in the following journal articles:**

- 1. A Flexible Alkaline Rechargeable Ni/Fe Battery Based on Graphene Foam/Carbon Nanotubes Hybrid Film.** Jilei Liu, Minghua Chen, Lili Zhang, Jian Jiang, Yizhong Huang, Jianyi Lin, Hongjin Fan, Zexiang Shen. *Nano Letters* **2014**, 14(12), 7180–7187. Chapter 5, Copyright 2014, Reprinted with permission from American Chemical Society.
- 2. High-performance flexible asymmetric supercapacitors based on a new graphene foam/carbon nanotube hybrid film.** Jilei Liu, Lili Zhang, Haobin Wu, Jianyi Lin, Zexiang Shen, Xiongwen Lou. *Energy & Environmental Sciences* **2014**, 7 (11), 3709–3719. Chapter 4, Copyright 2014, Reprinted with permission from The Royal Society of Chemistry.
- 3. Three-Dimensional Graphene Foam Supported Fe<sub>3</sub>O<sub>4</sub> Lithium Battery Anodes with Long Cycle Life and High Rate Capability.** Jingshan Luo†, Jilei Liu†, Zhiyuan Zeng, Chi Fan Ng, Lingjie Ma, Hua Zhang, Jianyi Lin, Zexiang Shen, Hongjin Fan. *Nano Letters* **2013**, 13 (12), 6136–6143. (†equal contribution) Chapter 3, Copyright 2013, Reprinted with permission from American Chemical Society.
- 4. Improved synthesis of graphene flakes from the multiple electrochemical exfoliation of graphite rod.** Jilei Liu, Chee Kok Poh, Da Zhan, Linfei Lai, San Hua Lim, Liang Wang, Xiaoxu Liu, Nanda Gopal Sahoo, Changming Li, Zexiang Shen, Jianyi Lin. *Nano Energy* **2013**, 2 (3), 377–386. Chapter 2, Copyright 2013, Reprinted with permission from Elsevier.
- 5. A green approach to the synthesis of high-quality graphene oxide flakes via electrochemical exfoliation of pencil core.** Jilei Liu, Huanping Yang, Saw Giek Zhen, Chee Kok Poh, Alok Chaurasia, Jingshan Luo, Xiangyang Wu, Edwin Kok Lee Yeow, Nanda Gopal Sahoo, Jianyi Lin, Zexiang Shen. *RSC Advances* **2013**, 3 (29), 11745–11750. Chapter 2, Copyright 2013, Reprinted with permission from The Royal Society of Chemistry.



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My Ph.D. journey, albeit a long one, has been a very fulfilling and rewarding experience. Throughout this whole experience, I have encountered multiple challenges, but thankfully I have also learned from each challenge to be better. This has been a wonderful journey, and I am lucky to have this opportunity.

I would like to express my deepest gratitude to my supervisor Prof. Zexiang Shen for taking me under his wing and for his care, guidance, and support throughout my whole graduate career. His vision, patience, and determination have greatly helped me on this journey and would no doubt serve as valuable life lessons in the future.

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Last but not least, and most importantly, I would give my special thanks to my loved ones: my wonderful parents, wife, and younger brother. Words are not sufficient to express my love and appreciation. Thank you for allowing me to pursue my dream, and for constantly supporting and encouraging me when I'm faced with obstacles. Completion of this Ph.D. journey marks the end of a chapter, but opens another in my life. I am looking forward to sharing this new phase of my life with you.

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# Chapter 1

## Introduction and Literature Background

### 1.1 Energy Demands and Challenges

Energy is no doubt the engine that promotes human civilization and development. Achieving secure, clean and sustainable energy production, storage, and consumption are, perhaps, the greatest technical and social challenges that the world are facing [1–6]. Generally, energy sources could be divided into two categories based on their intrinsic nature: non-renewable sources and renewable sources. Non-renewable energies include fossil fuels, nature gas, oil and coal, are available in limited quantities on the earth and could not be re-generated within a short span of time. Renewable energies are energies that are inexhaustible, and could be generated repeatedly when required, such as solar, wind, geothermal, tide and biomass. It is projected by the U.S. Energy Information Administration that the world energy consumption will grow from 524 quadrillion British thermal units (Btu) in 2010 to 820 quadrillion Btu in 2040, a 56 percent increase between 2010 and 2040 (reference case) [7].

With rapidly growing energy demands and concerns over energy security and environmental pollution, it is highly desirable to explore renewable and sustainable energy sources. It is anticipated by Russia International Energy Agency that the share of renewable energies in primary energy consumption will rise from 13% in 2011 to 18% in 2035, resulting from rapidly increasing demand for modern renewable society to produce heat, generate power, and make transport fuels [8].

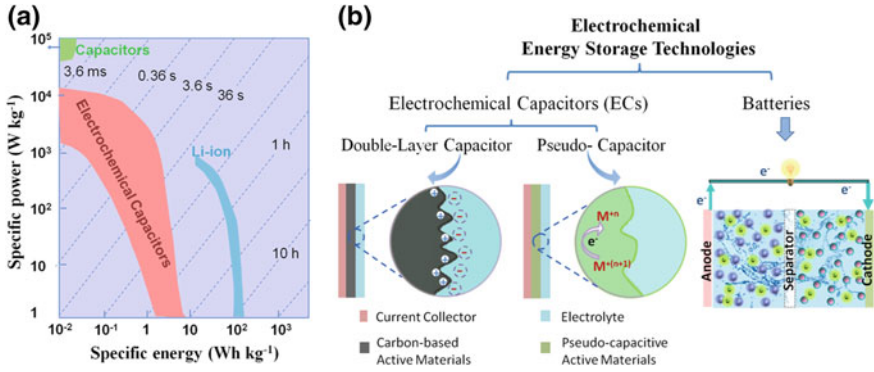
Wind power and solar photovoltaics (PV) are the world's fastest-growing renewable energy. Wind and solar would account for about 19% of global installed power capacity, and reach almost 35% of that of the European Union in 2035 according to the New Policies Scenario [8]. However, unlike dispatchable power generation technologies (fossil fuel-fired, geothermal, hydropower with reservoir and bio-energy), which may be ramped up or down to match demand, the output from wind power and solar PV is only intermittently available and is strongly dependent on the availability of the sources including the time, weather, season and

location, while the demands and consumption of electric energy are relatively constant [8]. Wind power and solar PV are also characterized as variable renewable energies because of their typical properties, such as variability, uncertainty, modularity, low operation cost and non-synchronous generation. Although quite attractive, the variable nature of many renewable sources present great challenge for energy storage and transmission. The key achievement lies in exploring renewable and sustainable energy sources, particularly, storing energy efficiently, and delivering on demand. Consequently, large-scale stationary energy storage systems (ESSs) connected to renewable power plants have become key enablers of improving power reliability and quality as well as taking full advantages of high penetration of renewable energy sources [6, 9, 10]. To be highly efficient, energy storage technologies are required to be adapted for various applications types. EESSs that are available for large-scale applications by far could be categorized into four types: mechanical, chemical, electrical and electrochemical [6, 9, 11–13]. Although mechanical energy storage via pumped hydroelectricity is dominating current energy storage, electrochemical energy storage in terms of electrochemical capacitors and batteries have by far found their wide applications in powering portable electronics and electrification of the transportation sector because of their desirable characteristics such as high round-trip efficiency, controllable power and energy, long cycle life, environmental-friendly feature and low costs [6, 9, 11]. However, there are several challenges that rooted primarily in materials and technologies for coupling electrochemical energy storage with renewable energy sources such as wind and solar for powering the electric grid. The realization of high performance electrochemical energy storage devices is strongly dependent on the achievements of multidisciplinary sciences, including materials sciences, chemical sciences and physical sciences etc. [6, 9, 14].

## 1.2 Electrochemical Energy Storage Systems

### 1.2.1 *Electrochemical Capacitors (ECs)*

Since the first patent released by General Electric on 1957 [15], electrochemical capacitors (ECs) have attracted considerable attentions due to their promising applications in various areas including power storage and supply, power quality and backup applications etc. [16]. Since ECs have high power capability, efficiency and long life span [16–18] (Fig. 1.1). ECs are energy storage devices that are capable of storing and releasing electric charge in a faster way than electrochemical cells/batteries [17]. Based on different work mechanisms, ECs are classified into two categories: (i) electrochemical double layer capacitors (EDLCs) and (ii) pseudocapacitors [16–20]. The so-called EDLCs are based on electrostatic charge separation at the electrochemical interface between electrode and electrolyte, creating two electrostatic capacitors connected in series. Pseudocapacitors are based on



**Fig. 1.1** **a** Ragone Plot and **b** Fundamental mechanisms of different energy storage technologies, include double-layer capacitor, pseudocapacitor and batteries

faradaic pseudocapacitance, that associated with electrosorption or surface/near-surface electrochemical redox processes involving in pseudocapacitive materials such as transition metal oxides and conducting polymers [14, 18, 19, 21].

### 1.2.1.1 Thermodynamic Principles of Electrochemical Capacitors (ECs)

**Double Layer Capacitance.** Different from traditional electrostatic capacitors, EDLCs store and release energy at the interface between electrolyte and electrode, where two capacitors are formed resulting from the reversible adsorption of solvated ions at the electrode surface, and connected in series by electrolyte [19, 21]. This type of charge storage is electrostatic, potential dependent, physicochemical nature of the electrode surface dependent, and no redox reactions are involved [14, 18, 19, 21]. The current during charge storage/release process is essentially a displacement current resulting from the rearrangement of charges in a Helmholtz double layer. Therefore, the process is non-faradaic and physical in nature and the response to potential changes is rapid without diffusion limitations [20, 22]. Thus, EDLCs deliver energy very fast and have high power capability (Fig. 1.1a). However, the energy stored in EDLCs is generally lower than that of pseudocapacitors and batteries because the charge stored in EDL capacitors is confined to the surface (Fig. 1.1b). The EDL capacitance could be described as [14, 16, 17, 19, 21, 23]:

$$C_{dl} = \frac{Q}{V} = \frac{\epsilon_r \epsilon_0 A}{d} \quad (1.1)$$

where  $C_{dl}$  is the double layer capacitance (F) of a single electrode,  $Q$  is the total charge transferred at potential  $V$ ,  $\epsilon_r$  is electrolyte dielectric constant,  $\epsilon_0$  is the vacuum dielectric constant,  $d$  is the charge separation distance, and  $A$  is electrode surface area.

Considering  $C$  is a constant for double layer capacitors, another equation could be derived from (1.1):

$$I = \frac{dQ}{dt} = \frac{d(C_{dl}V)}{dt} = C_{dl} \frac{dV}{dt} + V \frac{dC_{dl}}{dt} = C_{dl} \frac{dV}{dt} \quad (1.2)$$

where  $I$  is the response current,  $t$  is the charge time.

If the applied voltage  $V$  varies with time  $t$  in a linear way, i.e.  $V = V_0 + vt$  ( $V_0$  is the initial voltage;  $v$  is the sweep rate (V/s)), the relationship could be given as:

$$I = C_{dl}v \quad (1.3)$$

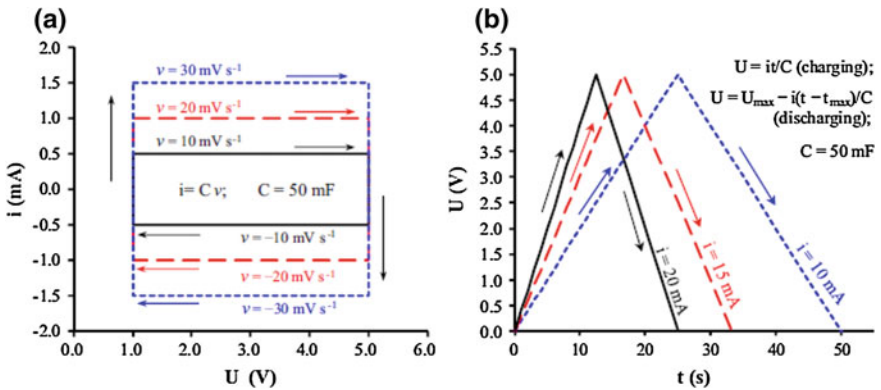
It is found from Eq. (1.3) that the current responses linearly with the sweep rate. This feature translates into a well-defined rectangular current ( $I$ )-voltage ( $V$ ) plot or cyclic voltammogram (CV) curve at different sweep rates (Fig. 1.2a). On the other hand, if a constant current is applied to charge or discharge the capacitor, voltage will increase (charging) or decrease (discharging) with a constant rate as predicted by Eq. (1.3). Thus, a triangular charge/discharge curve is expected (Fig. 1.2b).

The energy stored in such a capacitor is given by [14, 16, 17, 19, 21, 25]:

$$E = \int_0^Q V(q)dQ = \int_0^Q \frac{Q}{C}dQ = \frac{1}{2} \frac{Q^2}{C} = \frac{1}{2} CV^2 \quad (1.4)$$

$$Q = \int_0^{\Delta t} Idt = \int_0^q dq \quad (1.5)$$

where  $V$  is nominal voltage (volts) and  $q$  is the state of charge.



**Fig. 1.2** **a** Cyclic Voltammogram (CV) curves at different sweep rates, and **b** Galvanostatic Charge/Discharge curves at various currents for a 50 mF capacitor [24]. Reprinted with the permission from Elsevier, Copyright 2013



The power is thus described by the equation:

$$P = \frac{E}{t} = \frac{1}{2} \frac{CV^2}{t} \quad (1.6)$$

**Pseudocapacitive Capacitance.** Pseudocapacitive processes are, ideally, two-dimensional (2D) or quasi-two-dimensional. The pseudocapacitive energy storage is based on fast and reversible faradaic redox process in which a monolayer or quasi-monolayer of electrochemical reactive species could be electrosorbed/electrodesorbed with charge transfer [18, 19, 26, 27]. The charge-discharge mechanism involves the transfer of charges between the surface or near surface of the electrode and the electrolyte but without any bulk phase transformation (Fig. 1.1b). The state of charge/discharge ( $q$ ) is a function of the electrode potential with the extent of faradaic charge/discharge ( $Q$ ) passed [19]. The change of charge ( $Q$ ) with respect to the potential gives rise to the derivative,  $dQ/dV$ , corresponds to pseudocapacitance ( $C_\theta$ ) [18]. Pseudocapacitance is faradaic in nature, which is different from the EDL capacitance that is associated with the potential-dependent accumulation of electrostatic charge [18, 19]. Pseudocapacitive processes also differ from the ideal Nernstian processes involved in a battery-type materials where faradaic reactions occur at a constant potential [28].

$$C_\theta \sim \frac{dQ}{dV} \quad (1.7)$$

There are several faradaic processes that can result in pseudocapacitance according to Conway [18, 19]: (i) under-potential deposition (UPD) (two-dimensional, 2D), (ii) surface redox system, and (iii) intercalation system (quasi-2D) (Fig. 1.3).

**Under-potential Deposition.** The deposition of metal ions on a different metal surface to form an adsorbed monolayer, which may occur at a potential less negative than their equilibrium potential for the reduction of this metal ion, is called under-potential deposition (UPD) [29, 30]. A well-known case of UPD is the deposition of Pb on Au, where Pb can deposit onto Au more easily than it deposit onto itself due to stronger Pb–Au interaction than the Pb–Pb interaction in the crystal lattice of pure Pb metal [26, 27, 30]. However, UPD is not limited only to metal deposition, but may also include other adsorbed layer, e.g., H from  $H_3O^+$  or  $H_2O$  deposit on Pt [27, 29, 31, 32].

**Surface Redox System.** Redox processes take place when electroactive species are electrochemically adsorbed onto the surface or near surface of the electrode materials with a concomitant faradaic charge transfer. Redox systems exhibiting pseudocapacitance include the electrochemical oxidation/reduction of transition metal oxides (e.g., ruthenium oxide, manganese oxide) and electrochemical generation of electrically conducting polymer (ECP) (e.g., polyaniline, polypyrrole, and poly-3,4-ethylene dioxythiophene) [14, 18, 21, 33]. The transitional metal oxides ( $MO_2$ ,  $M = Ru$  or  $Mn$ ) can be oxidized and reduced reversibly through

electrochemical protonation ( $H^+$ ) or alkali metal cations ( $C^+=Na^+, K^+, \dots$ ) intercalation, as described below [34, 35]:

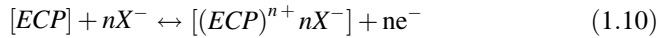


or



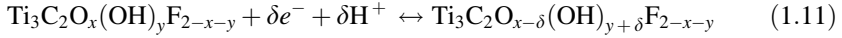
The charge transfer process during charging and discharging does not lead to chemical transformation, but only forms a reversible functionalized molecular layer on the electrode surface. The potential of the electrode is associated with the coverage of the layer and hence dependent on the charges state. This feature is fundamentally different from redox reactions involved in battery-type electrodes, where phase change occurs at a constant potential.

Electrically conducting polymers (ECPs) can store and release charges through redox processes in the  $\pi$ -conjugated polymer chains during electrochemical doping/un-doping processes, as shown below [36–38]:



During oxidation (p-doping) process, the anionic species  $X^-$  from the electrolyte are inserted into the polymer backbone. They are released back into the electrolyte upon reduction process. Similar to a battery-type reaction, the insertion/de-insertion of counter ions takes place in the bulk of the electrode, enabling high values of specific capacitance, but also giving rise to the relatively poor cycling performance resulting from volumetric changes of conducting polymers [39]. Hence, the addition of a moderate amount of carbon allotropes (e.g., carbon black, CNTs or graphene) to improve the mechanical properties of the electrodes is extremely important [33, 40, 41].

**Intercalation Pseudocapacitance.** Intercalation pseudocapacitance arises when the intercalation sorption of electroactive species take place quasi-two-dimensionally accompanied with faradaic charge transfer and without crystallographic phase change. Intercalation systems in pseudocapacitors include the intercalation of  $Li^+$  into hosts such as  $TiS_2$ ,  $MoS_2$ , and  $V_6O_{13}$  or the intercalation of H into Pd and Pd-Ag alloys [14, 19, 26, 27]. More recently, MXenes (of the formula  $M_{n+1}X_nT_x$ , where M is a transitional metal, X is C and/or N, and  $T_x$  denotes surface functionalization), are emerging as unique host materials for intercalation pseudocapacitor [42, 43]. Various ions such as  $Li^+$ ,  $Na^+$ ,  $K^+$ ,  $NH_4^+$ , and  $Al^{3+}$  ions are found to be intercalated into MXenes layers with high volumetric pseudocapacitance [42, 43]. The intercalation/de-intercalation processes, as shown in Eq. (1.11) for two-dimensional titanium carbide ( $Ti_3C_2T_x$ ), accompany with changes in the Ti oxidation state during cycling, ensuring high values of volumetric capacitance [44].



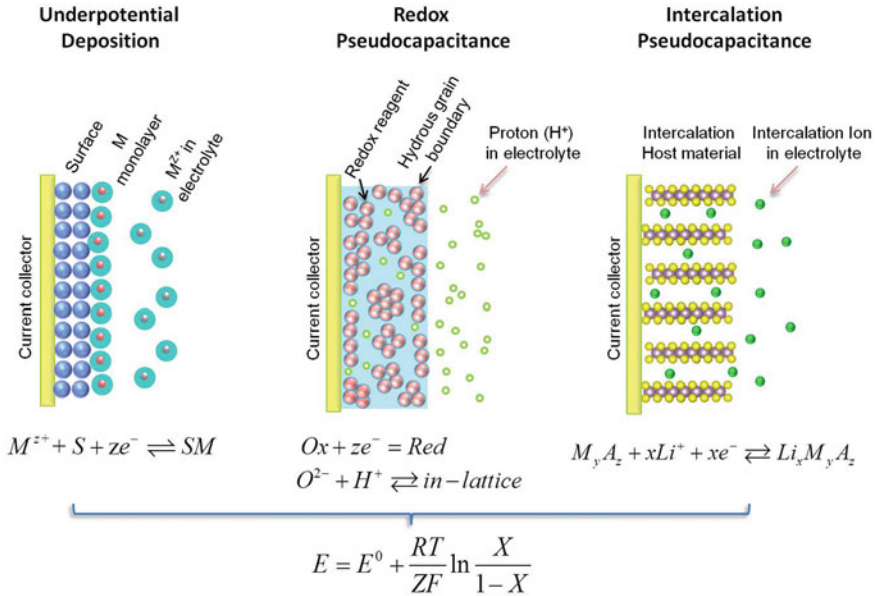
Although these three mechanisms take place based on different faradaic process and in different types of electrode materials, they exhibit similar thermodynamic feature, i.e., logarithmic relationship between electrode potential and the extent of charge/discharge [14, 19, 45] (Fig. 1.3):

$$E = E^0 + \frac{RT}{nF} \ln \frac{X}{1-X} \quad (1.12)$$

where  $E$  is the electrode potential (V),  $R$  is the ideal gas constant ( $8.314 \text{ J mol}^{-1}\text{K}^{-1}$ ),  $T$  is the temperature (K),  $n$  is the number of electrons,  $F$  is the Faraday constant ( $96,485 \text{ C mol}^{-1}$ ), and  $X$  is the occupancy fraction of surface or layer lattice.

If the electrochemical sorption of electroactive species follows an electrochemical Lagmuir isotherm [27, 32]:

$$\frac{X}{1-X} = k \cdot \exp\left(\frac{VF}{RT}\right) \quad (1.13)$$



**Fig. 1.3** Different faradaic processes that give rise to pseudocapacitance. Note  $X$  is two-dimensional site occupancy fraction for UPD,  $[\text{Ox}]/([\text{Ox}] + [\text{Red}])$  for redox systems and occupancy fraction of layer lattice for intercalation systems, respectively

The pseudocapacitance could be defined as [19]:

$$C_{\emptyset} = q^* \cdot \frac{dX}{dV} \quad (1.14)$$

where  $q^*$  is the charge required for completion of monolayer sorption.

Applying Eq. (1.13) into Eq. (1.14) leads to:

$$C_{\emptyset} = \frac{q^* F}{RT} \cdot \frac{k \cdot \exp[VF/RT]}{(1 + k \cdot \exp[VF/RT])^2} = \frac{q^* F}{RT} \cdot X \cdot (1 - X) \quad (1.15)$$

It is found that the pseudocapacitance  $C_{\emptyset}$  is not constant and has a maximum value at  $X = 0.5$ . Pseudocapacitor is similar to the EDL capacitor in the way that the stored charge is proportional to the applied potential. The fundamental difference between them lies in that faradaic charge transfer takes place in a pseudocapacitor. Noted that both battery and pseudocapacitor involve faradaic charge transfer. However, for a pseudocapacitor, the electrode potential associated with the electrosorbed electroactive species is a continuous function of the extent of the conversion of the electroactive material, i.e., the degree of utilization of free sites on the electrode surface or within the 2D or quasi-2D material ( $\Delta G = \Delta G^o + RT \ln(X/(1 - X))$ ); While for most of the battery electrodes, the electrode potential is determined at some singular value by the Gibbs energies of pure, well-defined 3D phases and usually also the composition and/or concentration of the solution ( $\Delta G = -nFE^o$ ) [19, 45, 46]. In addition, higher rate capability is always demonstrated for pseudocapacitor than batteries benefiting from the surface/near-surface reaction nature (Figs. 1.2 and 1.3).

### 1.2.1.2 Kinetic Electrochemical Features of ECs

While thermodynamic aspects of ECs have been introduced above, the practical application of ECs is strongly dependent on their kinetic behaviour. It should be stated that all electrochemical reactions are subjected to polarization effects that would sacrifice working voltage and reversible capacity [14, 19]. Therefore, although electrochemical capacitances could result from various electrochemical processes, they suffer from polarization effects and the ideal complete reversibility is not practical from a kinetic viewpoint. Indeed, there is an internal resistance, known as equivalent series resistance ( $R_{ESR}$ ), for any electric power sources. Here we try to introduce the kinetic features of ECs from the point of  $R_{ESR}$  firstly, and then illustrate electrochemical features of pseudocapacitive via their responses to (i) potentiodynamic sweep (cyclic voltammetry); (ii) constant current (galvanostatic charge/discharge curves), and iii) alternating current (impedance spectroscopy) [14, 19].

### Equivalent Series Resistance ( $R_{ESR}$ )

Just as mentioned above, package electric power sources process intrinsic internal resistance ( $R_{ESR}$ ), which is an important parameter that determines their power performance (Fig. 1.4a).

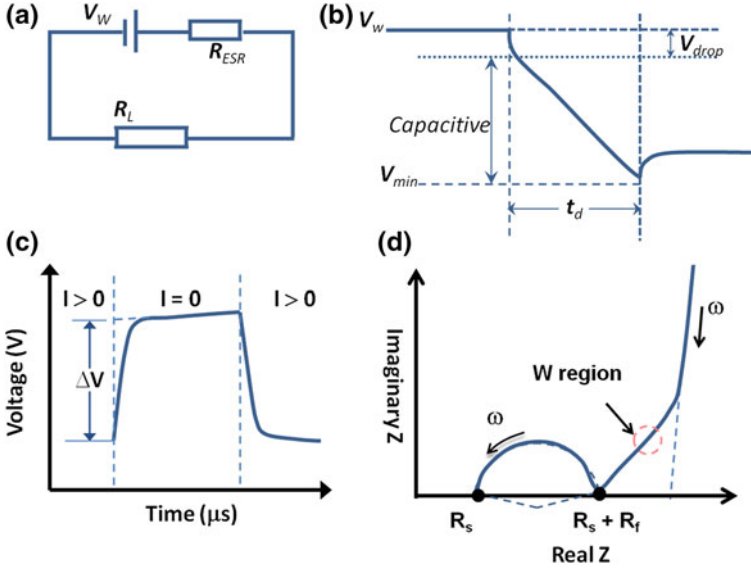
For a power source with working voltage ( $V_w$ ), current ( $I$ ) flow through the circuit with a load ( $R_L$ ) on discharge could be given as [24, 47]:

$$I = \frac{V_w}{(R_L + R_{ESR})} \quad (1.16)$$

Accordingly, there is a resistance component in addition to the capacitive component described in Eqs. (1.2) and (1.3). The resistance component is governed as:

$$V_{drop} = IR_{ESR} \quad (1.17)$$

And then, the Eqs. (1.4) and (1.6) are modified, and new derivations are described as:



**Fig. 1.4** **a** Typical electric circuit that a power source ( $V_w$ ) with a load of ( $R_L$ ) and an equivalent series resistance ( $R_{ESR}$ ). **b** Constant current discharge curves for a EC (where  $V_w$  is working voltage, Capacitive is the voltage drop due to discharge of the capacitor (Eq. 1.2),  $V_{drop}$  is the voltage drop due to  $R_{ESR}$  (Eq. 1.17),  $V_{min}$  is the minimum voltage allowed by power system;  $t_d$  is the discharge time.). **c** Idealized voltage waveform during current interrupt event. **d** Typical Nyquist Plot for a pseudocapacitor

$$E = \int_0^Q V(q)dQ = \int_0^Q \frac{Q}{C} dQ \quad (1.18)$$

$$P = IV = I(V_W - V_{drop}) = I^2 R_L = \left(\frac{V_W}{R_L + R_{ESR}}\right)^2 R_L \quad (1.19)$$

From Eq. (1.19), the maximum power,  $P_{max}$ , could be derived at  $R_L = R_{ESR}$  [48] and given as:

$$P_{max} = \left(\frac{V_W}{R_L + R_{ESR}}\right)^2 R_L = \frac{1}{4} \frac{V_W^2}{R_{ESR}} \quad (1.20)$$

By combining Eqs. (1.6) and (1.20), the shortest discharging time,  $t_{min}$ , can be derived and given as [24]:

$$t_{min} = \frac{1}{2} \frac{C V_W^2}{P_{max}} = 2 C R_{ESR} \quad (1.21)$$

#### Determination of Equivalent Series Resistance ( $R_{ESR}$ )

Several methods can be used to determine  $R_{ESR}$ , such as (i) measuring the  $iR$  drop at the initiation of a constant current discharge, (ii) measuring the bounce back of voltage at the end of a constant current discharge, or (iii) using AC impedance spectroscopy (often at 1000 Hz) [49].

**$iR$  drop.** The  $R_{ESR}$  is usually determined from the galvanostatic discharge tests using  $iR$  drop for practical packed cell in lab. In this case,  $R_{ESR}$  is defined as the voltage change that occurs nearly instantaneously upon the application of current [48]. A change in the form of Eq. (1.17) could define the  $R_{ESR}$  as:

$$R_{ESR} = V_{drop}/I \quad (1.22)$$

This method is somewhat subjective because the data cannot be accurately described by an instantaneous drop followed by a perfectly linear discharge. In practical, the discharge curve is smooth with a gradual transitions. Nevertheless, this method does provide useful information for internal resistance of the cell from a first-order approximation. The results calculated from  $iR$  drop is inversely proportional to cell size [21, 48].

**Current Interrupt Steps.** The  $R_{ESR}$  could also be measured via constant current interrupt steps (<5 s) at a specified voltage. In this case,  $R_{ESR}$  is defined as the voltage change that occurs nearly instantaneously upon application of current [48, 49] (Fig. 1.4c):

$$R_{ESR} = \Delta V / \Delta I \quad (1.23)$$

It should be stated that this method is dependent on the methodology used, including the data sampling rate, electrode geometry, etc. [48]. Special caution should be given for porous electrode-based electrochemical systems, where the overestimation of the ohmic voltage change and the  $R_{ESR}$  of the cell would be expected via the interrupt method.

**Electrochemical Impedance Spectroscopy (EIS).** In EIS testing, a sinusoidal voltage perturbation at a well-defined frequency is applied to the cell with the desired state of charge. The resulting variation in current is recorded which provides information about the electrochemical response of the system over a wide range of frequencies (typically 10 kHz–1 Hz or lower) [48, 50, 51]. By fitting the EIS data, the resistance of a cell, such as solution resistance, electrode properties in terms of ohmic resistance and activation polarization resistance, EDL capacitance, and transport or diffusion properties [52–55], could be therefore characterized (Fig. 1.4d).

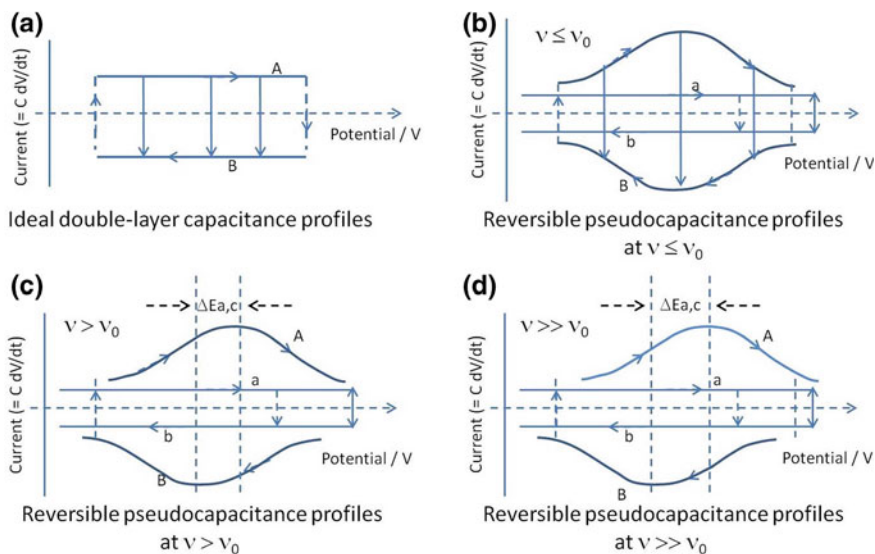
Typical Nyquist plot (Fig. 1.4d) shows a semicircle in the high-frequency region, followed by a Warburg and linear part in the low frequency region. The first crossover point on the Nyquist plot,  $R_s$ , is generally considered as the resistance associated with electrolyte resistance and the external contact resistance.  $R_f$  is the charge transfer resistance resulting from the EDL capacitance on the particle surface of the electrode, and/or the faradaic reactions.  $R_s + R_f$  is the main contributor to  $R_{ESR}$ . It must be emphasized that the interpretation of the EIS data should be based on individual cases, and different experimental configurations will lead to different data interpretation. In the case where pseudocapacitive materials are present, perfect semicircles generally cannot be obtained. Instead, suppressed semicircles in high-frequency region with sloppy linear line in the low-frequency region might be obtained.

## Kinetic Electrochemical Features of Pseudocapacitance

### (a) Potentiodynamic sweep-cyclic voltammetry (CV)

In CV experiments, at various sweep rates ( $v$ , V/s or mV/s), ideally, there is no or small potential difference (or hysteresis) between the anodic and cathodic peaks in fast charge storage devices, and the CV curves are symmetric particularly at slow sweep rates for ideal capacitive system (Figs. 1.5a, b) [14, 19].

**Sweep rate dependence of peak potential.** One typical kinetic feature of pseudocapacitor is the presence of critical sweep rate. That is because, except for air or vacuum dielectric capacitors, all ECs have effective equivalent series resistance ( $R_{ESR}$ ), which result in polarization effect and deviations from ideal capacitive behaviour. The presence of the charge transfer resistance in pseudocapacitors imposes kinetic limitations. If the surface faradaic processes involved for pseudocapacitors are modulated by an increasing sweep rate ( $v$ ), the kinetic reversibility is lost gradually [19]. This is manifested by the peak potential,  $E_p$ , which remains



**Fig. 1.5** CV profiles of ideal double layer capacitor (a) and Reversible pseudocapacitor (b–d) with different sweep rate  $v$ .  $v_o$  is the critical sweep rate [19]. Reprinted with the permission from Ref. [19]. Copyright 1991, The Electrochemical Society

independent of  $v$  until  $v$  reaches critical sweep rate  $v_o$ , and then increase with  $\log v$  [56]. It indicates that there is a critical sweep rate value  $v_o$  from which the kinetic behavior is radically different [56]. For example, the cyclic voltammograms would translate into non-mirror images with the increase in the cathodic and anodic peak voltage separation ( $\Delta E_{a,c}$ ) as  $v > v_o$ , indicating the transition from kinetic reversible process to a kinetic irreversible process (Figs. 1.5c, d) [57, 58]. But the kinetic reversibility could be regained for pseudocapacitor by lowering the sweep rate, since there is no phase change occurs during the charge/discharge processes. The presence of kinetic limitation (characterized by the  $v_o$  value) determines the effective charge/discharge rates or power performance of ECs.

The cyclic voltammograms of EDLCs are always rectangular in shape with no or slight deviation upon the increase of the sweep rate. On the other hand, the CV curves of pseudocapacitors can be rectangular in shape with or without cathodic/anodic peaks (or wide pumps), depending on the type of electrode materials. Wide-broad redox peaks were generally observed for conductive polymers including polyaniline [59], polypyrrole [60] and PEDOT [61], and transition metal oxides (e.g.,  $\text{MoO}_3$  [62],  $\text{V}_2\text{O}_5$  [63],  $\text{T-Nb}_2\text{O}_5$  [64]). Typical pseudocapacitive electrode materials that exhibit nearly ideal rectangular cyclic voltammograms without distinct redox peaks are hydrous  $\text{RuO}_2$  [65, 66] and  $\text{MnO}_2$  [35] in aqueous electrolytes. More recently,  $\text{Ti}_3\text{C}_2\text{T}_x$  Mxene is also found to produce rectangular-shaped CVs in sulfuric acid, originating from the continuous change in the titanium oxidation state during charge/discharge process [42, 44]. These results



demonstrate that reversible faradaic reactions can result in similar electrochemical behavior as those of EDL capacitors. This makes the differentiation between EDL type of mechanism and pseudocapacitive mechanism rather difficult, especially for electrode materials that simultaneously possess both charge storage mechanisms. Nevertheless, efforts are made to roughly estimate the contributions from each of the two surface-controlled charge storage processes. Example will be given later.

**Sweep rate dependence of response current.** Another important and characteristic feature of the kinetic behaviour for pseudocapacitance is the relationship between the response current ( $i$ ) and sweep rate ( $v$ ). In cyclic voltammetry experiments, the total current measured under a potential sweep rate is the sum of the diffusion current ( $i_{diff}$ ) and the current required to charge the double layer at the electrolyte interface/ignite fast faradaic reactions on the exposed electrode surface ( $i_{cap}$ ) [67]. And it could be expressed as:

$$i(V) = i_{cap} + i_{diff} = av^b \quad (1.24)$$

where  $v$  is the sweep rate, and both  $a$  and  $b$  are adjustable parameters [68–71]. The parameter  $b$ -value is determined from the slope of the linear plot of  $\log i$  versus  $\log v$ . There are two well-defined conditions in general:  $b = 0.5$  and  $b = 1$ . The slope  $b = 1$  is representative of a capacitive contribution that arises from surface redox reactions, thus  $i_{cap} = av$ . While the slope  $b = 0.5$  is denoted for semi-infinite diffusion-controlled faradaic process [68–70, 72]. The diffusion current ( $i_{diff}$ ) could be described by the classical Sevcik equation [73]:

$$i_{diff} = nFAC^*D^{1/2}v^{1/2}(\alpha nF/RT)^{1/2}\pi^{1/2}\chi(bt) \quad (1.25)$$

where  $n$  is the electron transfer number,  $F$  is the Faraday constant,  $A$  is the apparent surface area of the electrode materials,  $C^*$  is the concentration of active species,  $D$  is the diffusion coefficient of the rate limiting species,  $\alpha$  is the transfer coefficient,  $R$  is the molar gas constant,  $T$  is the absolute temperature, and the  $\chi(bt)$  functional part is the normalized current for a totally irreversible system as indicated by the cyclic voltammetric response.

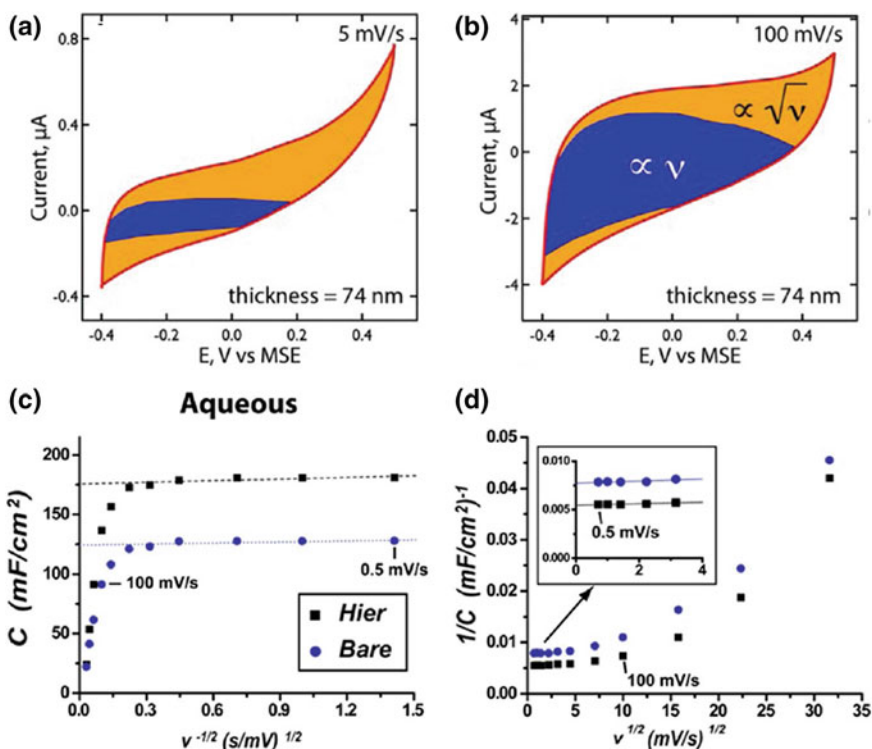
It is derived from Eqs. (1.24) and (1.25) that the current response to sweep-rate varies depending on whether the reaction process involved is a surface mechanism (capacitive) or a diffusion-controlled mechanism. If the reaction process is controlled by surface mechanism, current varies linearly with  $v$  ( $di/dv = \text{constant} = \text{the capacitance}$ ); for faradaic process limited by semi-infinite linear diffusion, the current varies with  $v^{1/2}$  ( $di/dv^{1/2} = \text{constant}$ ) [67, 74]. Taking into account all cases, a general expression for current at a certain potential could be given [67, 74]:

$$i(V) = i_{cap} + i_{diff} = k_1v + k_2v^{1/2} \quad (1.26)$$

or it could be changed as:

$$i(V)/v^{\frac{1}{2}} = k_1 v^{\frac{1}{2}} + k_2 \quad (1.27)$$

The values of  $k_1$  and  $k_2$  could be evaluated from the slop and intercept, respectively, if  $i(V)/v^{1/2}$  plotted versus  $v^{1/2}$  give a straight line. Consequently, it becomes possible to separate the capacitive contribution from diffusion-controlled intercalation processes, and quantify the current or capacitance fraction related to each of these contributions. This technique has been utilized to evaluate the electrochemical performance of nanostructures materials (Fig. 1.6a, b) [68, 75–78]. It is interestingly found that the contribution fraction of each parts is strongly dependent on materials crystalline [78], structure or morphology [75, 79], particle size [68], electrolyte [76] and sweep rate [77].



**Fig. 1.6** CV curves of Au/MnO<sub>2</sub> core-shell nanowires at sweep rates of 5 mV/s (a) and 100 mV/s (b): capacitive current ( $i \propto v$ , blue part) was separated from diffusion current ( $i \propto v^{1/2}$ , yellow part) [75]. Reprinted with the permission of American Chemical Society, copyright 2012 (c) Typical areal capacitance (C) versus  $v^{-1/2}$  plots and (d)  $1/C$  versus  $v^{1/2}$  plots for bare (blue circles) and hierarchical (black squares) MnO<sub>2</sub> nanowire arrays in aqueous LiClO<sub>4</sub> electrolyte [76]. Reprinted with the permission of American Chemical Society, Copyright 2013

**Sweep rate dependence of capacitance.** The variation of voltammetric surface charge  $q^*$  with the sweep rate  $v$  has been described by Trasatti et al. on  $\text{RuO}_2$  electrodes via a linear function [80]:

$$q^* = q_s^* + q_d^* \quad (1.28)$$

The maximum charge density  $q^*$  is considered to consist of two fractions,  $q_s^*$  and  $q_d^*$ , representing the charge related to outer (capacitive contribution) surface and inner (diffusion-controlled contribution) surface. The  $q_s^*$  that corresponds to outer surface could be obtained at infinite potential sweep rate ( $v \rightarrow \infty$ ),

$$q^* \rightarrow q_s^* \quad (1.29)$$

The maximum charge density ( $q_m^*$ ) could be obtained when at the sweep rate ( $v \rightarrow 0$ ),

$$q^* \rightarrow q_m^* \quad (1.30)$$

Particularly,  $q^*$  is expected to be limited by  $v^{-1/2}$  if semi-infinite linear diffusion is involved whereas capacitive contributions are independent of the sweep rate, thus Eq. (1.28) could be expressed as:

$$q^*(v) = q_{v \rightarrow \infty}^* + q_d^* = q_{v \rightarrow \infty}^* + \text{const} \left( v^{-1/2} \right)^* \quad (1.31)$$

from which, a basic amount of  $q_s^*$  could be collected via the extrapolation of linear diagram of  $q^*$  versus  $v^{-1/2}$  to  $v^{-1/2} = 0$  (Fig. 1.6c).

Generally,  $q^*$  decreases as the potential sweep rate increases because of diffusion limitation [80]. Since  $q_s^*$  increases linearly with  $v^{-1/2}$ , it is reasonable to expect that  $1/q^*(v)$  decrease linearly with  $v^{1/2}$ :

$$1/q^*(v) = 1/q_m^* + \text{const} \left( v^{1/2} \right)^* \quad (1.32)$$

where  $q_m^*$  is the maximum total charge. Extrapolation of liner plot of  $1/q^*(v)$  versus  $v^{1/2}$  to  $v^{1/2} = 0$  gives the basic amount of the maximum total charge  $q_m^*$  (Fig. 1.6d).

Consequently, the difference between the total charge ( $q_m^*$ ) and the surface charge ( $q_{v \rightarrow \infty}^*$ ) give the charge associated to diffusion-controlled processes.

$$q_d^* = q_m^* - q_{v \rightarrow \infty}^* \quad (1.33)$$

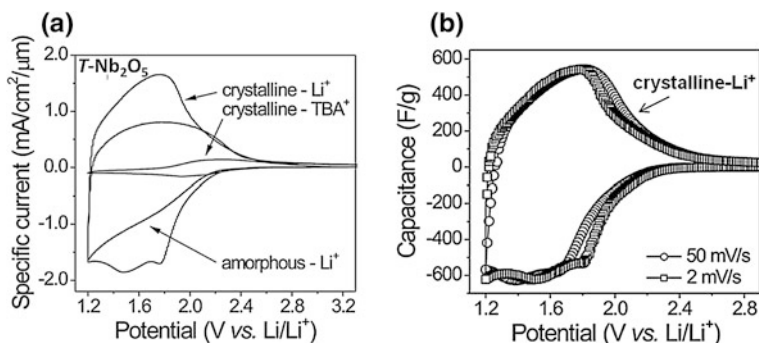
Similarly, the ratio of capacitive contribution and semi-diffusion controlled contribution for the total capacity would be evaluated.

**Sweep rate dependence of double-layer capacitance and Pseudocapacitance.** The separation of capacitive current/charge from diffusion-controlled current/charge has been well addressed in above via cyclic voltammetry. Capacitive charge storage

consists of contributions from both double-layer capacitive and pseudocapacitive effects.

$$C = C_{dl} + C_0 \quad (1.34)$$

Through proper design of experiment, CV can sometimes (not always) be used to differentiate EDL mechanism from fast surface redox reaction, as demonstrated by Dunn, et al. [81]. Mesoporous  $\text{Nb}_2\text{O}_5$  with crystallographically orientated layered nanocrystalline walls shows typical intercalation pseudocapacitance through fast cation intercalation into layered gaps (van der Waal gaps) of  $\text{Nb}_2\text{O}_5$ . When mesoporous  $\text{Nb}_2\text{O}_5$  with crystalline walls was used as the electrode, the use of different electrolyte (and thus different cations) determines different charge storage mechanism. When tetrabutylammonium ( $\text{TBA}^+$ ) perchlorate in propylene carbonate is used as the electrolyte, the total charge storage shown in the CV curve (very small response current) (Fig. 1.7a) is based on EDL mechanism only since the bulky  $\text{TBA}^+$  cations cannot be intercalated into the layered  $\text{Nb}_2\text{O}_5$  quickly; whereas in  $\text{LiClO}_4$  electrolyte, both EDL and intercalation pseudocapacitive processes contribute to the total charge storage (as evidenced by the much larger response current in Fig. 1.7a). The ratio of the EDL capacitance/pseudocapacitance could therefore be estimated from the CV results. A small fraction ( $\sim 10\%$ ) of the total charge storage stems from EDL capacitance while most of the charge is stored through a surface-confined faradaic charge-transfer process. This is further confirmed by broad peaks in the voltages profiles in Fig. 1.7b, which is characteristic of a surface-confined charge-transfer process [81]. It must be emphasized that the method discussed here should be used with great care and it can only provide a rough estimation of the contribution from the EDL process and the surface redox processes. In addition, it is limited to certain types of electrodes only and the method will not work properly if highly porous electrodes containing pores much smaller than the size of the electrolyte ions are present in the system.



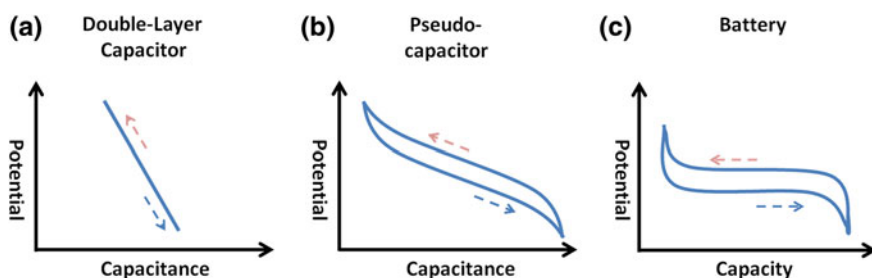
**Fig. 1.7** **a** Cyclic Voltammetry (CV) curves of amorphous and crystalline mesoporous T-Nb<sub>2</sub>O<sub>5</sub> films in Lithium (Li<sup>+</sup>) and tetrabutylammonium (TBA<sup>+</sup>) electrolyte at a sweep rate of 10 mV/s [81]. **b** Potential-dependent capacitance calculated from CV curves at sweep rate of 2 and 50 mV/s. Reprinted with the permission of American Chemical Society, Copyright 2010

### (b) Constant current-charge/discharge curve

As mentioned above, the profile of potential versus capacitance for EDL capacitor is well-defined linear in shape as described by Eq. (1.3) and is illustrated in Fig. 1.8a. For pseudocapacitor, the electrode potential associated with the electro-sorbed species is a continuous logarithmic function of the extent of sorption (Eq. 1.12), which is different from the linear function of that of EDL capacitor. In a constant current charge/discharge process, this translates into smooth charge/discharge profiles with small potential hysteresis (Fig. 1.8b). On contrast, a battery electrode shows a potential plateau without a sloping line in potential versus capacity profile (Fig. 1.8c).

### (c) Alternating current-impedance spectroscopy

EIS is an efficient tool for monitoring changes in ECs and determining their dynamic electrochemical behaviour by applying a sinusoidal voltage perturbation to ECs at a well-defined frequency. The corresponding information regarding the electrochemical response of the system at that frequency is then derived from resulting current response. The equivalent electric circuit diagram is usually used to interpret the experimental data. If the behavior of an EC is purely capacitive, the  $R_{ESR}$  is frequency-independent with the real and imaginary components being out of phase by  $90^\circ$ , and the Nyquist plot is a vertical line with a resistive element  $R$  being connected in series with the capacitor  $C$  [14, 18, 21]. The resistive element represents the resistance from the electrolyte solution and/or from the external contact. However, most practical ECs deviate from purely capacitive behavior because of kinetic limitations, and therefore the equivalent circuit is more complex. The equivalent electric circuit model for EDL capacitor is generally approximated with the EDL capacitance ( $C_{dl}$ ), being in parallel with a resistor  $R_f$ , and an additional resistance ( $R_s$ ) that corresponds to electrolyte resistance and the external contact resistance. For pseudocapacitive system, faradaic resistance  $R_f$  and pseudocapacitance  $C_\theta$  that associates with potential-dependent charge is connected in series, and being in parallel with EDL capacitance ( $C_{dl}$ ) since pseudocapacitance arises from a potential dependent interfacial faradaic reaction. The practical



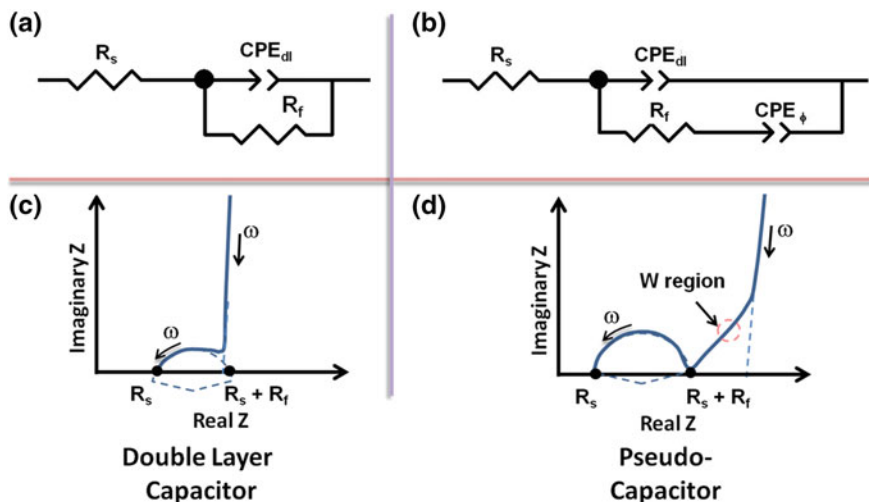
**Fig. 1.8** General electrochemical features of double-layer capacitor (a), pseudocapacitor (b) and battery (c)

impedance results for a solid electrode/electrolyte interface often display a frequency dispersion that cannot be described by simple elements such as capacitor, resistor, inductor or Warburg diffusion. Therefore, a constant phase element (CPE) which allows for a distribution of capacitance values is generally introduced in order to provide much better impedance fittings (Fig. 1.9) [82]. The definition of constant phase element in the equivalent circuit is given as [82, 83]:

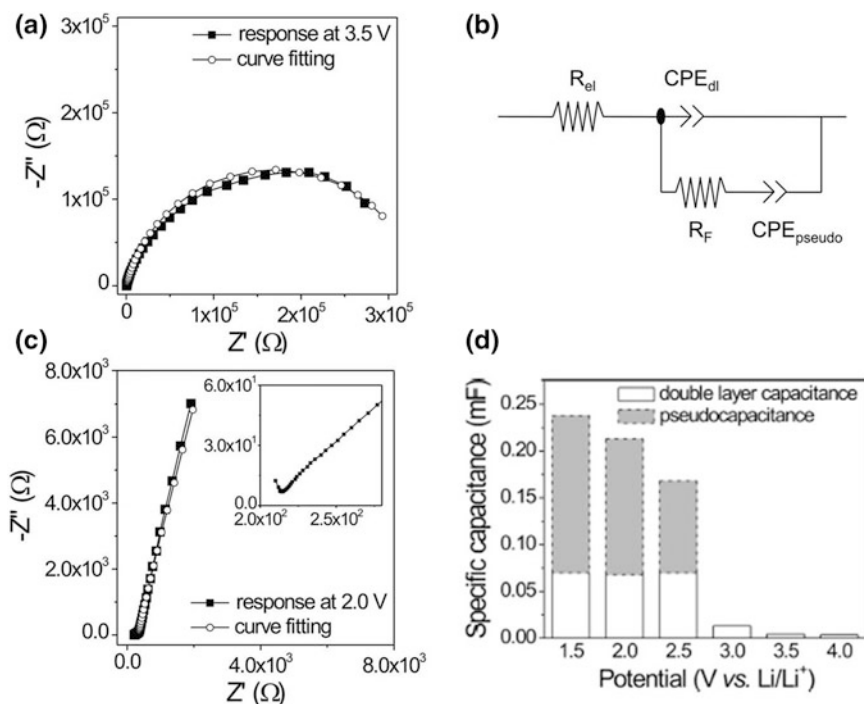
$$Z_{CPE} = \frac{1}{T(j\omega)^\alpha} \quad (1.35)$$

here,  $Z_{CPE}$  is the impedance,  $T$  is a constant in  $F\text{ cm}^{-2}\text{ s}^{\alpha-1}$ ,  $\omega$  is the frequency,  $\alpha$  is an adjustable constant. When  $\alpha = 1$ , the CPE is regarded to represent an ideal capacitor. It would be a resistor for  $\alpha = 0$ , and an inductor for  $\alpha = -1$ . Particularly, the  $\alpha = 0.5$  indicates semi-infinite diffusion.

Based on the equivalent electric circuit diagram (Fig. 1.9), it is apparent that the separation of EDL contribution from pseudocapacitive contribution for certain types of electrodes is possible by fitting the AC impedance result appropriately. An example is shown in Fig. 1.10, where the EDL and pseudocapacitive contributions in  $\text{CeO}_2$  thin film electrodes are distinguished using AC impedance measurement at different applied potentials [79]. For potential above 3 V, very small EDL capacitance was obtained due to the high electronic resistance of ceria when Ce is in its fully oxidized state. At lower potentials, a sizable fraction of  $\text{Ce}^{4+}$  reduces to  $\text{Ce}^{3+}$  and the electronic conductivity increases. The film electrode therefore delivers significant amounts of capacitance. The pseudocapacitive contributions increase



**Fig. 1.9** Equivalent circuits for: **a** double-layer capacitor, and **b** Pseudocapacitor. Corresponding electrochemical impedance spectroscopy results are listed in **c**, **d**, respectively [18]. Reprinted with the permission of Springer, Copyright 2003



**Fig. 1.10** Nyquist plot for KLE-template  $\text{CeO}_2$  at the potential 3.5 V (a) and 2.0 V (b) (vs.  $\text{Li/Li}^+$ ). c Equipment circuit model for impedance data fitting. d Separation of double layer capacitance and pseudocapacitance based on different applied potentials for  $\text{CeO}_2$  films [79]. Reprinted with the permission of American Chemical Society, Copyright 2010

with decreasing voltage while EDL contributions remain almost unchanged for applied potential less than 3 V, suggesting different charge storage mechanisms are involved under different applied potentials [79].

### 1.2.1.3 Symmetric and Asymmetric Supercapacitors

The well-known reciprocal relation between overall capacitance of the device ( $C$ ) and that of two individual electrodes ( $C_1$  and  $C_2$ ) could be given as follows [17, 18]:

$$\frac{1}{C} = \frac{1}{C_1} + \frac{1}{C_2} \quad (1.36)$$

If  $C_1 = C_2$  (symmetric combination, for example, two same non-faradaic electrode work against with each other), the measured  $C$  would be half the value of individual electrode. This type of system is called as “symmetric capacitor” [18]. If the capacitance of the cell is adjusted further via combining mass of two electrodes, a factor of

“4” would introduce. For example, a single carbon electrode (with high surface area  $1000 \text{ m}^2/\text{g}$ ) exhibits the capacitance of  $10 \text{ } \mu\text{F}/\text{cm}^2$ . This gives rise to a specific capacitance of  $100 \text{ F/g}$  for one electrode. For a symmetric capacitor, two electrodes with half the total capacitance (Eq. 1.36) and doubled weight results in an  $25 \text{ F/g}$  active capacitor [17]. The significant differences between single electrode and the complete is of significant importance and should be clarified when an EC is introduced.

If electrode “2” refers to faradaic electrode (or battery-type electrode), corresponding  $C_2$  is essentially infinity. Thus  $C \approx C_1$  is approximated according to Eq. (1.36) because of pseudocapacitance  $C_2 \gg C_1$ , and the full charge stored on  $C_1$  (non-faradaic electrode) is hence available for discharge. This type of system is called as “asymmetric capacitor” [18].

The maximum energy stored in such a capacitor is given by [14, 16, 17, 19, 21, 25]:

$$E = \frac{1}{2} CV_w^2 \quad (1.37)$$

where  $V$  is nominal voltage (volts).

The maximum power is described by the equation:

$$P_{max} = \frac{1}{4} \frac{V_w^2}{R_{ESR}} \quad (1.20)$$

where  $R_{ESR}$  is equivalent series resistance ( $\Omega$ ). For the packed cells, the  $R_{ESR}$  is typically determined via measuring the IR drop, the bounce back of voltage, or using AC impedance spectroscopy [21, 84].

### 1.2.1.4 Summary for Double-Layer Capacitance and Pseudocapacitance

See Table 1.1.

**Table 1.1** Separation of double-layer capacitance and pseudocapacitance

	Double-layer capacitance	Pseudocapacitance or supercapacitor
Mechanism	No-faradaic involved	Faradaic involved
Capacitance-voltage	Capacitance constant (potential-independent)	Capacitance not constant (potential-dependent)
Phase angle-frequency	$90^\circ$ phase angle	Phase angle function of frequency, but some embodiments have transmission-line behaviour
Kinetic aspect	High-power operation	Kinetic limitations for high charge/discharge rates
Reversible	Indefinitely reversible	Highly reversible
Electrode material	Carbon allotropes	Transition metal oxides/hydroxides, conducting polymers, MXenes etc.



### 1.2.2 Lithium-Ion Battery

#### 1.2.2.1 Thermodynamic Aspects of Battery

Similar to ECs, the energy and power features of battery follow directly from the thermodynamic principles for electrochemical reactions, which can be given as [46]:

$$\Delta G = \Delta H - T\Delta S \quad \text{and} \quad \Delta G^\circ = \Delta H^\circ - T\Delta S^\circ \quad (1.38)$$

where  $\Delta G$  is the Gibbs free energy,  $\Delta H$  is the enthalpy,  $\Delta S$  is the entropy and  $T$  is the absolute temperature.

It is noted that  $\Delta G$  represent the net useful energy resulting from a given reaction, and it would be in terms of electrical energy for a battery/cell and expressed as follow:

$$\Delta G = -nFE \quad \text{and} \quad \Delta G^\circ = -nFE^\circ \quad (1.39)$$

where  $n$  is the electron transfer number,  $F$  is the Faraday constant,  $E$  is the cell electromotive force (EMF). The cell EMF is determined at some singular value by the Gibbs energies of pure, well-defined phases and is unique for each redox reaction couple. This is totally different from the continuous logarithmic-dependent electrode potential of ECs.

The free energy for bulk chemical reactions is given according to van't Hoff isotherm [46, 85, 86]:

$$\Delta G = \Delta G^\circ + RT \ln(A_P/A_R) \quad (1.40)$$

Nernst equation for electrochemical reactions could be derived by combining Eqs. (1.39) and (1.40) [46, 85, 86]:

$$E = E^\circ + (RT/nF) \ln(A_R/A_P) \quad (1.41)$$

here,  $R$  is the gas constant,  $T$  is the absolute temperature,  $A_P$  is the activity of products and  $A_R$  is the activity of reactants.

The relationship between the current flow and the extent of reaction could be expressed as follows:

$$I = -nF \frac{m}{MW} / t \quad (1.42)$$

where  $I$  is the current flow,  $n$  is the number of electron involved in the reaction,  $m$  is the weight of active materials,  $MW$  is the molecular weight of active materials, and  $t$  is the time of current flow.

Based on these, the total charge ( $Q$ ) could be given as [85–87]:

$$Q = \int_0^{\Delta t} I dt = \int_o^Q dq \quad (1.43)$$

where  $q$  represents the state of charge.  $Q$  is the cell capacity that depending on  $I$ . In addition, changes in electrode volume, electrode decomposition and electrode-electrolyte chemical reactions result from charge/discharge cycling would cause an irreversible loss of capacity. Therefore, the Coulomb efficiency is one of important metric for a battery/cell, which can be described as follows [85]:

$$\text{Coulom efficiency} = 100 \times Q_{dis}/Q_{ch} \quad (1.44)$$

The densities of stored energy and power are given as:

$$\text{Energy density} = \int_0^{\Delta t} IV(t)dt = \int_o^Q V(q)dq \quad (1.45)$$

$$\text{Power density} = V(q)I(q) \quad (1.46)$$

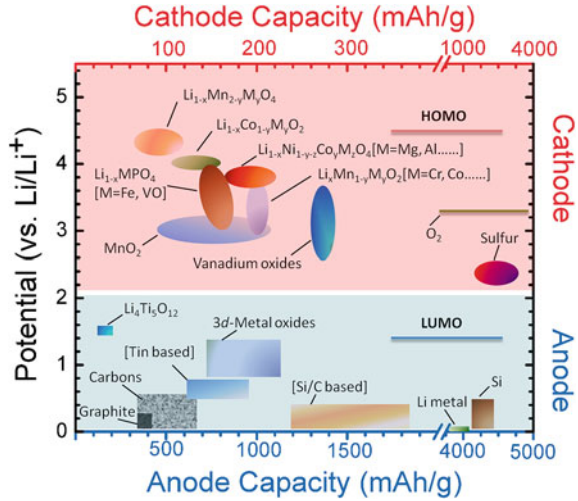
where  $\Delta t$  is the time required for complete discharge at a constant current  $I_{dis} = dq/dt$ . Based on Eqs. (1.43) and (1.45), it is apparent that the stored energy is strongly dependent on the average ( $V(q)$ ) and the capacity ( $Q$ ).

The electrochemical potential difference between anode ( $\mu_a$ ) and cathode ( $\mu_c$ ) gives rise to the open-circuit voltage ( $V_{oc}$ ) of a cell [86]:

$$V_{oc} = (\mu_a - \mu_c)/e \quad (1.47)$$

In practical batteries, the open-circuit voltage is also limited by the “working window” of the electrolyte. The electrolytes for practical rechargeable battery systems are crystalline solid, glass, polymer, or liquid. The working window is determined by the energy gap between the lowest unoccupied molecular orbital (LUMO) and the higher occupied molecular orbital (HOMO) for a liquid electrolyte (Fig. 1.11) or the bottom of the conduction band and top of the valence band for a solid electrolyte [85, 88]. For a thermodynamically stable cell, the electrochemical potentials of anode  $\mu_a$  and cathode  $\mu_c$  of a charged cell should be matched the LUMO and HOMO of the electrolyte for achieving maximum  $V(q)$  of a stable and safe cell. That is because electrolyte would be reduced when the  $\mu_a$  of anode is above its LUMO and would be oxidized when the  $\mu_c$  of cathode is below its HOMO. Alternatively, the solid-electrolyte interphase (SEI) passivation layer that is electronically insulating but permeable to the working ion would form to stabilize a mismatched electrode system [85, 87].

**Fig. 1.11** Voltage and capacity ranges for some cathode and anode materials



### 1.2.2.2 Kinetic Aspects of Battery

During discharge, the voltage drop off (electrode polarization) would occur when current flow across the battery. This results from kinetic limitations of reactions, in which an internal resistance  $R_b$  reduce the output voltage  $V_{dis}$  of a cell relative to the open-circuit voltage  $V_{oc}$  by a polarization  $\eta = I_{dis}R_b$  [46, 85]. The polarization,  $\eta$ , is thus given as:

$$\eta(q, I_{dis}) = V_{oc} - V_{dis} \quad (1.48)$$

Reversely, the presence of  $R_b$  would increase the voltage required to reverse the chemical reaction upon charge by an overpotential  $\eta(q, I_{ch})$  [86]:

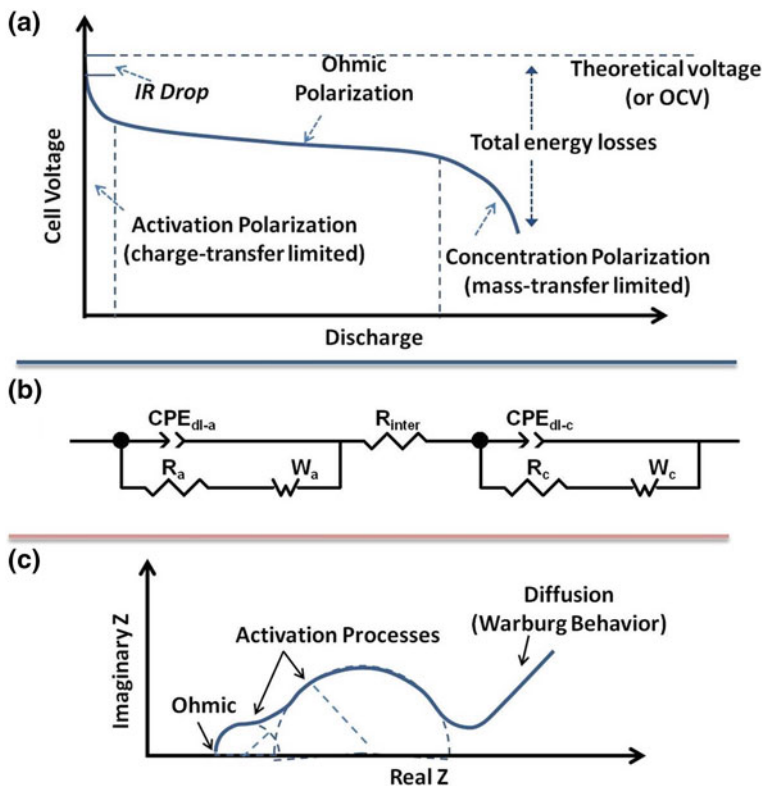
$$V_{ch} = V_{oc} + \eta(q, I_{ch}) \quad (1.49)$$

Generally, there are three different kinetic effects for polarization: (i) activation polarization, (ii) ohmic polarization, and (iii) concentration polarization (Fig. 1.12a) [46, 89, 90].

**Activation polarization** arises from kinetics hindrances of the electrochemical redox (or charge-transfer) reactions taking place at the electrode/electrolyte interfaces of anode and cathode. For a charge-transfer-controlled battery reaction, the current flow  $i$ , could be given as [46]:

$$i = i_0 \exp(\alpha F \eta / RT) - \exp((1 - \alpha) F \eta / RT) \quad (1.50)$$

where  $\eta$  is the polarization,  $\alpha$  is the transfer coefficient.  $i_0 = k_0 FA$  is the exchange current density ( $k_0$  is the reaction rate constant for the electrode reaction, and  $A$  is the activity product of the reactants).



**Fig. 1.12** **a** Typical discharge curve of a battery, showing different types of polarization. **b** Simple battery circuit diagram, **c** Corresponding Nyquist plot for an idealized battery system, where characteristic behaviors of activation, ohmic, and concentration polarizations are distinguished.  $W_a$  and  $W_c$  are the Warburg impedances of diffusion process for anode and cathode, respectively.  $R_a$  and  $R_c$  are the resistances of the anode reactions and cathode reactions.  $R_{inter}$  is the internal resistance of battery.  $CPE_{dl-a}$  and  $CPE_{dl-c}$  are the constant phase elements for anode and cathode, respectively [46]. Reprinted with the permission of American Chemical Society, Copyright 2004

Derived from Eq. (1.50), the activation polarization following the Tafel equation was given as:

$$\eta(q, I_{dis}) = a - b \log(i/i_0) \quad (1.51)$$

**Ohmic polarization** consists of the resistance of individual cell components (electrodes, electrolyte, the conductive additive, binder, current collectors, terminals) and the contact resistance among various individual components. Ohm's Law is obeyed for ohmic resistance  $R$ :

$$\eta(q, I_{dis}) = IR \quad (1.52)$$

**Concentration polarization** results from mass transport limitations during cell operation, in which the availability of the active species at the electrode/electrolyte interface changes and becomes diffusion-limited. The concentration polarization for diffusion-controlled process can be expressed as

$$\eta(q, I_{dis}) = (RT/n) \ln(C/C_0) \quad (1.53)$$

where  $C$  is the concentration at the electrode/electrolyte interface, and  $C_0$  is the concentration in the bulk of the solution.

In reality, the influence of the current rate on the cell voltage is controlled by all three types of polarizations. Similar to that of ECs, EIS is often used to access the kinetic behavior of a battery during the charge/discharge process. It is possible to distinguish different types of polarization by proper fitting of the impedance plot. The equivalent circuit model and the corresponding Nyquist diagram is shown in Fig. 1.12b, c. The activation polarization is often reflected by two semicircles or arcs in Nyquist plot [91, 92]. The first semicircle or arc at higher frequency is associated with the contact resistance between the electrode material and the metallic substrate coupled with a double layer capacitance [91], while the second semicircle or arc at lower frequency is associated with the charge transfer resistance between the electrode materials and the active species from the electrolyte coupled with a CPE element. In anode where there is a SEI layer, the contribution of the SEI resistance will come into the picture as well. Ohmic polarization has no capacitive character and is independent of frequency. It is represented as battery internal resistance  $R_{int}$ . The concentration effect is encapsulated as the Warburg element  $W$ . It reveals typical diffusion-controlled processes in the low frequency featured by  $45^\circ$  Warburg region, which is associated with the diffusion of the active species inside the solid electrode. A good battery cell should have small  $R_{int}$ ,  $R_a$ ,  $R_c$  and short Warburg region.

### 1.2.3 Electrochemical Capacitor Versus Battery

In this section, the properties and differences of electrochemical capacitors and batteries are summarized in terms of electrochemical behavior and thermodynamic behaviour.

#### 1.2.3.1 Thermodynamic Behavior

See Table 1.2.

**Table 1.2** Comparative thermodynamic behavior of electrochemical capacitor and ideal battery [19, 28, 45]

Electrochemical capacitor		Battery
Double layer capacitor	Pseudocapacitor	
Free energies $\Delta G$ of the electroactive materials <b>change continuously</b> with the extent of charge/discharge		Free energies $\Delta G$ of the electroactive phases involved are <b>unique</b> and <b>single-valued</b> during discharge/charge process $\Delta G \cong \text{Constant} = -nFE$
$G = 1/2CV^2$	$\Delta G = \Delta G^\circ + RT \ln(X/(1 - X))$	
Potential varies continuously with <b>time</b>	Potential varies continuously with <b>the state of charge/discharge</b>	Potential on discharge/charge is <b>single-valued</b>
Behavior is <b>capacitative</b>		Behavior is <b>non-capacitative</b>
High degree of <b>reversibility</b>		<b>Irreversibility</b>

### 1.2.3.2 Electrochemical Properties

See Table 1.3.

**Table 1.3** Comparative electrochemical characteristics of electrochemical capacitor and battery [14, 19, 45]

Electrochemical capacitor		Battery
Double layer capacitor	Pseudocapacitor	
<b>Potential</b> is thermodynamically related to the state of charge ( $Q$ ) directly in a continuous manner	<b>Potential</b> is thermodynamically related to the state of charge through $\log[X/1 - X]$ factor in a continuous manner	<b>Electromotive force (EMF)</b> is ideally constant with the degree of charge/discharge, except for nonthermodynamic incidental effects, or phase changes during discharge
<b>Free energies</b> vary with extent of charge field in a continuous manner	<b>Free energies</b> vary with degree of conversion in a continuous manner	<b>Free energies</b> of components are single-valued
<b>Galvanostatic discharge</b> exhibits linear decline of potential with time	<b>Galvanostatic discharge</b> exhibits a “transition” from linear decline of potential to a more or less constant potential	<b>Galvanostatic discharge</b> arises at a more or less constant potential (except for intercalation Li batteries)
The linear modulation of potential exhibits more or less <b>constant</b> charge/discharge current profile (with some dependence on materials)		The linear modulation of potential displays irreversible $i$ versus $V$ profile with <b>non-constant currents</b>
The cyclic voltammetry curves are <b>mirror images</b>	The cyclic voltammetry curves are <b>mirror images until <math>v</math> reaches to <math>v_o</math></b>	The charge/discharge profiles and cyclic voltammetry are <b>not mirror images</b>

**Table 1.4** Overall comparison of electrochemical capacitor and ideal battery [45]. Reprinted with the permission of Springer Sci. Bus. Media, Copyright 1999

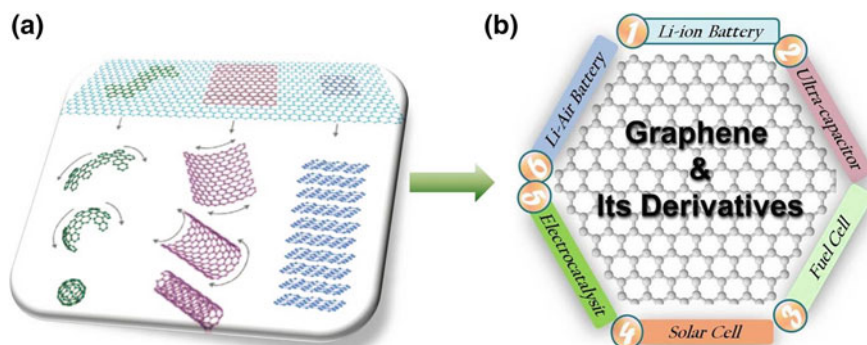
Electrochemical capacitor		Battery
Double layer capacitor	Pseudocapacitor	
<b>Galvanostatic discharge</b> exhibits linear decline of potential with time (good intrinsic stage-of-charge indication)	<b>Galvanostatic discharge</b> exhibits a “transition” from linear decline of potential to a more or less constant potential (relatively good intrinsic stage-of-charge indication)	<b>Galvanostatic discharge</b> arises at a more or less constant potential (poor intrinsic stage-of-charge indication) (except for intercalation Li batteries)
<b>Relatively poor</b> energy density	<b>Moderate</b> energy density	<b>Moderate or good</b> energy density (depending on active materials and battery types)
<b>Good</b> power density	<b>Moderate</b> power density	<b>Moderate or poor</b> power density
<b>Excellent cyclability</b>	<b>Moderate cyclability</b>	<b>Poorer cycle life</b> (due to irreversibility of redox and phase-changes in 3D dimensions)
<b>Internal <math>iR</math> drop</b> (related to <i>high specific area</i> of electrodes and electrolyte and their surface chemistry)		<b>Internal <math>iR</math> drop</b> (due to surface chemistry of <i>electrolyte and active materials</i> )
<b>No or little</b> activation polarization (but C may be Temperature-dependent)		<b>Significant</b> Temperature-dependent activation polarization
<b>Long life time</b> (except for corrosion of current collector, etc.)	<b>Moderate life time</b> (due to degradation of active materials)	<b>Poorer life time</b> (due to degradation and reconstruction of active materials)

### 1.2.3.3 Overall Comparison of Electrochemical Capacitor and Battery Characteristics

See Table 1.4.

## 1.3 Introduction to Graphene

Graphene, a single atomic layer of  $sp^2$ -bonded carbon atoms in hexagonal lattice, has attracted unprecedented interest owing to its intrinsic difference from other forms of carbon allotropes (Fig. 1.13) [93]. It exhibits excellent mechanical [94], electrical [95], thermal [96], and optical properties [97], and is particularly suitable for the implementation in electrochemical applications because of extraordinary electrical conductivity ( $64 \text{ mS cm}^{-1}$ ) [98], large specific surface area (theoretical



**Fig. 1.13** **a** Graphene: the parent of all graphite forms and **b** their applications in Both Energy Conversion and Storage Devices [102]. Reprinted with the permission of WILEY-VCH Verlag GmbH & Co. KGaA, Weinheim, Copyright 2009

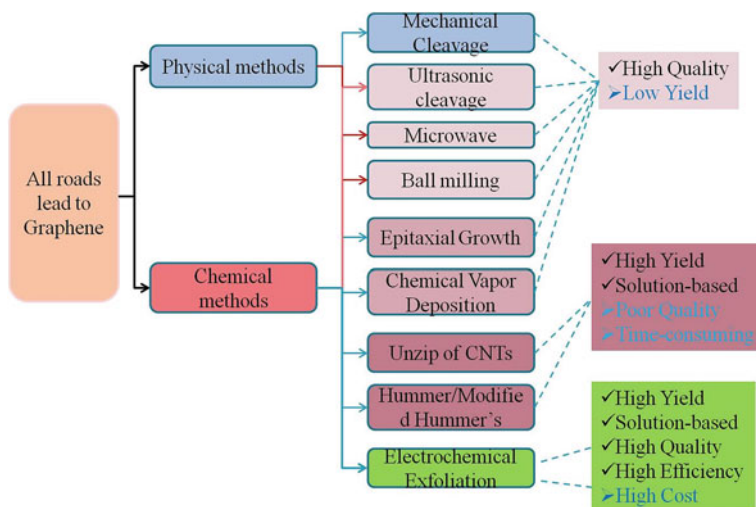
surface area  $\sim 2630 \text{ m}^2 \text{ g}^{-1}$ ) [99], unique heterogeneous electron transfer and charge carrier rates, and good electrochemical stability [100]. Graphene/Graphene-based composites have been used as effective counter electrodes for dye-sensitized solar cells, photo-catalysts for water splitting, electrocatalysts for oxygen reduction/hydrogen evolution in fuel cells, high-performance electrodes in super-capacitors, ions ( $\text{Li}^+$ ,  $\text{Na}^+$ ,  $\text{Al}^{3+}$ , etc.) batteries, lithium-sulfur batteries and lithium- $\text{O}_2$  batteries [101]. The synthesis of graphene in both high quality and quantity in a green and economical way is therefore highly desirable.

### 1.3.1 Various Approaches Leading to Graphene Oxide/Graphene

Since the first fabrication of single-sheet graphene through micromechanical cleavage of bulk graphite was reported [103], a number of methods have been proposed for generating graphene with high quality and low cost, which can be classified into two categories: bottom-up approach and top-down approach (Fig. 1.14) [104]. Bottom approaches, based on the catalytic decomposition of hydrocarbon gases, can provide large sized graphene with high crystal nature via epitaxial growth [105] or Chemical Vapour Deposition [106] although their high cost and low production. Top-down approaches, consisting of the intercalation of additional elements between graphite layers to form graphite intercalation compound (GIC), and then followed by the exfoliation of GIC either by physical, chemical or electrochemical methods, have received intense interest due to their scalability and low production cost [107–110].

Chemical exfoliation of graphene based on Brodie, Staudenmaier and Hummers methods, which involves the oxidation of graphite with strong acids and oxidants, and subsequent chemical or thermal reduction, is particularly favorable due to





**Fig. 1.14** All roads lead to Graphene or Graphene oxide (GO)

easy-processing and scalability [107]. Unfortunately, the use of strong acids and oxidants severely damages the  $sp^2$ -bonded of graphene and deteriorates its performance in various applications even though these damages could be recovered partially by subsequent reduction process [108].

Ultrasonic cleavage was also used to prepare graphene [109, 111]. However, the success of ultrasonic cleavage is strongly dependent on the proper choice of solvents and surfactants as well as the sonication frequency amplitude and time, which thus impedes its practical applications [110]. Graphene sheets can also be generated by unrolling carbon nanotubes (CNTs) via simultaneous intercalation of  $\text{NH}_3$ -solvated  $\text{Li}^+$  into interlayer space of MWCNTs [112], or use strong oxidizing agents  $\text{KMnO}_4$  to cut MWCNTs along the longitudinal direction [113].

Microwave-assisted heating technique was also adopted for the synthesis of water-soluble graphene due to the strong microwave absorption ability of graphitic materials [114]. Recently, electrochemical exfoliation of graphite and HOPG has been reported to be an effective way to prepare graphene and attracted increasing attentions [115–117].

### 1.3.2 Graphene for Soft Energy Storage Devices

The electrochemistry of graphene has been investigated intensively with respect to surface chemistry and structure, heterogeneous charge transfer rate constants on redox species, electrochemical operating window, and electrocatalysis of molecules recently [118, 119]. Particularly, the sharp proliferation of portable,

ultrathin/lightweight and wearable electronics, such as roll-up displays, touch screens, implantable medical devices, conformable health-monitoring electronic skin, wearable sensors and active radio-frequency identification tags (RFID), have promoted increasing demand for new power sources with high energy/power density, low cost, environmentally-friendly, as well as ultrathin, lightweight and flexible features [120–123]. One key challenge for soft energy storage devices lies in the development of deformable and high energy density electrodes with multiple merits via selecting and designing both current collector and electrode active materials [121, 123]. Soft electrodes are generally made from various functional organic and/or inorganic materials building on flexible conductive substrates without binders and conductive additives. Various soft electrodes have been prepared from paper-like carbonaceous electrode support, such as carbon nanotubes network (CNTs) [33, 124], graphene paper [120, 122], carbon cloth [125, 126], and other conductive paper (e.g., cellulose, textile, etc.) [123, 127]. Among them, electrodes based on CNTs network and/or graphene paper supports have attracted more attentions because of lightweight, good electric conductivity [95], large surface area [99], and good physical/chemical stability [100]. Graphene foam (GF), a 3-D interconnected network of chemical vapour deposition-grown graphene, has proven to be effective scaffold for soft energy storage devices [122]. Various soft electrodes based on GF, including GF/Fe<sub>3</sub>O<sub>4</sub> [128], GF/LiFePO<sub>4</sub> [122, 129] and GF/MnO<sub>2</sub> [130], have been prepared and exhibit enhanced electrochemical performance.

Although significant process has been made until now, the synthesis of high-quality graphene via an economic and environmentally-friendly way remains extremely challengeable. In addition, the exploring of graphene-based composites for their practical applications in flexible energy storage devices including supercapacitors and rechargeable batteries is highly-desirable and meaningful. These issues and challenges were addressed to some extent in this thesis. Briefly, in Chap. 2, a novel electrochemical exfoliation method that is green, efficient and economic was proposed for the gram-scaled synthesis of high quality graphene. The underlying mechanism was elucidated, the synthesis conditions were optimized, and the electrochemical performance of resultant samples was evaluated. Chap. 3 is focused on the design of flexible graphene foam (GF)/Fe<sub>3</sub>O<sub>4</sub> hybrid electrode for lithium-ion battery via atomic layer deposition approach. In Chap. 4, a novel carbon-based hybrid structure, named GF/carbon nanotubes (CNTs) hybrid films, was designed via a facile chemical vapor deposition (CVD) approach. This hybrid structure extends the 2D plane of Graphene into 3D directions without sacrificing electric conductivity and mechanical integrity. These features makes GF/CNTs hybrid films to be ideal electrode supports for deposition of large amounts of electrochemically active materials per unit area. To demonstrate the concept, asymmetric supercapacitors that are flexible was successfully fabricated based on GF/CNT supports. In Chap. 5, a new concept was proposed for designing flexible Nickel/Iron battery based on GF/CNTs hybrid films. The assembled prototypes display enhanced electrochemical performance and bridge the gap between supercapacitors and batteries, demonstrating great practical significance.

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## Chapter 2

# Electrochemical Exfoliation Synthesis of Graphene

The synthesis of graphene in both high quality and quantity *via* economic ways is highly desirable and meaningful for practical applications. Here a facile, environmentally-friendly and cost-effective multiple electrochemical exfoliation approach has been developed for the synthesis of high quality graphene flakes with high yield by using graphite rod from spent zinc-carbon/pencil core as carbon source. Various protonic acid (i.e.  $\text{H}_2\text{SO}_4$ ,  $\text{H}_3\text{PO}_4$  or  $\text{H}_2\text{C}_2\text{O}_4$ ) aqueous solution were chosen as electrolyte. The unique cell configuration enables multiple exfoliation process to improve both the quality and yield of graphene sheets. After nitrogen doping, the exfoliated graphene flakes process good electrocatalytic activity, stability and toxicity tolerance for alkaline solution-based oxygen reduction reaction.

## 2.1 Introduction

Since the first fabrication of single-sheet graphene through micromechanical cleavage of bulk graphite was reported [1], numbers of methods have been developed for generating graphene with high quality and low cost. Micromechanical cleavage [1], chemical vapor deposition (CVD) [2, 3] and epitaxial growth [4] produce graphene with high crystal quality but they are impractical for commercial applications due to low production rate and relatively high cost. Chemical exfoliation of graphene based on Brodie, Staudenmaier and Hummers methods, which involves the oxidation of graphite with oxidants and strong acids, and the subsequent chemical or thermal reduction, is advantageous in terms of low cost and controllable solution-processing [5]. However, this method employs some hazardous chemicals (e.g.,  $\text{H}_2\text{SO}_4$ - $\text{KMnO}_4$ , hydrazine) which are environmentally harmful and the production process is time-consuming [6]. Recently, electrochemical exfoliation of various carbon precursors, including graphite rods, carbon papers or HOPG, has been demonstrated to be an effective approach for generating graphene. Using

graphite rods as electrodes and ionic-liquid/water solution as electrolyte, Ionic liquid functionalized graphene sheets have been prepared *via* a one-step electrochemical approach [7]. Lu et al. [8] performed a detailed study and proposed a mechanism for the electrochemical exfoliation of graphite in ionic liquid solution, which involves (i) anodic oxidation of water, (ii) hydroxylation or oxidation of graphite edge planes, (iii) intercalation by ionic liquid anions between graphite layers, forming the graphite-intercalation-compounds (GICs), and (iv) oxidative cleavage and precipitation of the GICs. Inspired by the electrochemical reactions between graphite anode and organic carbonates in lithium ion batteries, Wang et al. [9] successfully prepared graphene flakes with few-layer *via* electrochemical exfoliation of graphite in propylene carbonate (electrolyte). The solvation nature of the bulky organic ions or molecules facilitate the intercalation process and the expansion of graphene layers. However, the organic compounds are sensitive to moisture and oxygen and the reactions always take a long reaction time. All these impede their practical applications. In the past few decades metal chlorides, strong protonic acids and other inorganic reagents have been the most promising “invaders” for graphite intercalation [10]. The expansion of graphite sheets in these intercalated compounds was realized by violent releasing of gases via fast heating. Very recently electric power has been used to drive the expansion and exfoliation of sulfate-intercalated graphite. In an electrochemical cell using protonic acid aqueous solution as electrolyte Su et al. [11] applied a relatively high (10 V) voltage to graphite anode for the synthesis of graphene sheets. Among many different electrolytes examined, including HBr, HCl, HNO<sub>3</sub>, and H<sub>2</sub>SO<sub>4</sub>, only H<sub>2</sub>SO<sub>4</sub> exhibits ideal exfoliation efficiency from natural graphite flake or highly oriented pyrolytic graphite. In Su’s paper the anode (graphite) and cathode (Pt) were placed parallel with a separation of a few cm away. Similarly almost all the reported electrochemical cells for graphite exfoliation are in the parallel configuration.

Herein an improved synthesis of high-quality graphene is demonstrated in a vertical cell configuration *via* multiple electrochemical exfoliation of graphite rod [12]. Unlike previous reports, the unique cell configuration adopted here enables multiple exfoliation processes to improve both the quality and yield of graphene sheets. The mechanism of multiple electrochemical exfoliation of spent graphite rod was discussed in detail, the experiment conditions were optimized, and the structure and electrocatalytic activity of the resultant sample were investigated.

## 2.2 Experiment and Characterization

### 2.2.1 Material Synthesis

*Synthesis of Graphene Flakes.* Graphene flakes were prepared *via* multiple electrochemical exfoliation (MEE) approach. Briefly, graphite rod from spent Zinc-Carbon dry cells was utilized as positive electrode and the carbon source.

The anode (graphite rod) and cathode (platinum wire) were placed at the bottom and top of the electrochemical cell, respectively, with protonic acid (e.g.  $\text{H}_2\text{SO}_4$ ,  $\text{H}_3\text{PO}_4$  or  $\text{H}_2\text{C}_2\text{O}_4$ ) aqueous solution as electrolyte. The electrochemical exfoliation process was ignited upon the application of a certain voltage across the electrodes. The water soluble graphene flakes were ultrasonicated, washed, dried and collected. Control experiments were also conducted *via* conventional (parallel) electrochemical configuration.

*Synthesis of Nitrogen-doped Graphene Flakes.* The as-prepared graphene flakes were annealed at 800 °C for 1 h under the flow of  $\text{Ar}/\text{NH}_3$  (95/5, v/v, 400 sccm), to achieve the N-doped graphene.

### 2.2.2 Material Characterization

*Structure and Morphology Characterization.* The morphology was investigated *via* Scanning Electron Microscopy (SEM), Transmission Electron Microscopy (TEM, JEM-2010, 200 kV), Optical Microscopy and Atomic Force Microscopy (AFM, Nanoscope V, diDimension). Fourier transform infrared spectroscopy (FTIR) (Perkin Elmer 2000 FTIR spectrometer), Thermogravimetric Analysis (TGA) and X-ray photoelectron spectroscopy (XPS) [VG ESCALAB 250 spectrometer (Thermo Electron, Altrincham, U.K.), using an  $\text{Al } K\alpha$  X-ray source (1486 eV)] were used to shed more light on chemical composition information.

*Electrochemical Performance Evaluation.* Rotating disk electrode (RDE) and Cyclic voltammetry (CV) measurements were conducted in a standard three-electrode system (platinum foil-counter electrode,  $\text{Ag}/\text{AgCl}$  electrode-the reference electrode, Graphene-working electrode). The working electrode was prepared as follows [13]: (i) 10 mg of N-doped graphene was ultrasonically dispersed into 1 ml of 2-propanol containing Nafion solution (5 wt%, dupont); (ii) 10  $\mu\text{l}$  of the catalyst ink was coated on the glassy carbon disk (5 mm in diameter) and dried at 80 °C for 15 min. As-prepared graphene, Pt-loaded carbon catalyst (Pt/C 20% on Vulcan XC-72R, E-TEK division, PeMEAS Fuel Cell Technology) with the same amount, and the bare glassy carbon electrode were tested for comparison. Methanol toxicity test was conducted at a constant potential  $-0.5$  V (vs.  $\text{Ag}/\text{AgCl}$ ). The voltammetric stability tests were performed in  $\text{O}_2$ -saturated 0.1 M KOH within the potential window of  $-1.0$ – $0.2$  V (vs.  $\text{Ag}/\text{AgCl}$ ) for 20,000 cycles. The sweep rate is 100 mV/s. All measurements were carried out at room temperature. All potentials presented in the graphs and in the discussion were calibrated with reference to the reversible hydrogen electrode (RHE), which is independent of pH value. The number of electron transferred ( $n$ ) was calculated based on Koutecky-Levich equation.

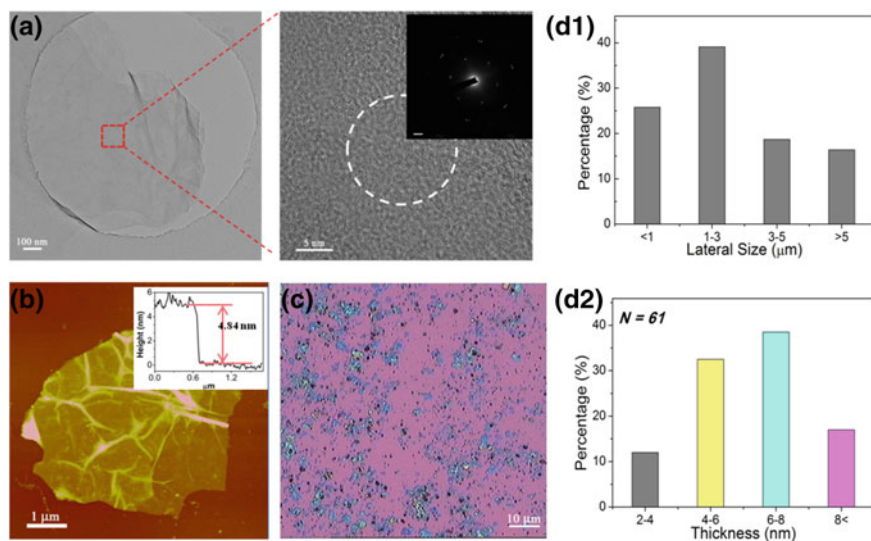
## 2.3 Results and Discussions

### 2.3.1 The Synthesis of Graphene Flakes

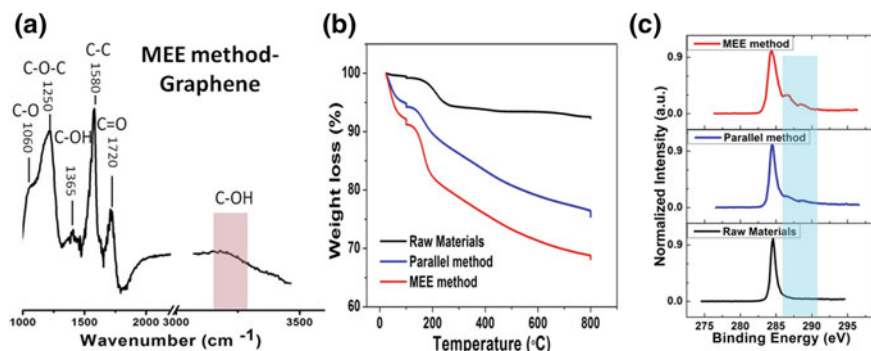
Different from conventional parallel two-electrode electrochemical cell, in our design graphite rod obtained from spent Zn–C primary battery (anode) and platinum wire (cathode) were placed vertically at the bottom and top of the electrochemical cell, respectively. The graphite rod was surrounded with a plastic tube and only the top surface of it was exposed to the electrolyte solution. A constant current of 0.1A was applied across the two electrodes. The potential of 6–8 V could drive the anions into the intercalation space and make the exfoliation to proceed. Comparative experiment was also conducted *via* conventional method. An apparent colour change for the aqueous electrolyte solution from transparent to dark was observed in vertical cell after only few minutes. This response time is much shorter than that of conventional method, indicating the exfoliation process in the vertical configuration is more efficient. In the same reaction time period, significantly larger quantity of graphene sheets were collected, benefiting from the multiple electrochemical exfoliation feature in our design. More details about the underlying mechanism will be discussed later.

The morphological and structural properties of the resultant samples were investigated by TEM, AFM and Optical microscopy. TEM and optical images reveal that the as-prepared products consist of a large amount of exfoliated graphene with lateral size ranging from 1 to few  $\mu\text{m}$  (Fig. 2.1a, c and d). The exfoliated graphene flakes with thickness of 4.84 nm are identified (Fig. 2.1b). Based on the statistical AFM mapping of exfoliated graphene flakes, approximately 32% of the graphene flakes have thicknesses in the range of 4–6 nm while nearly 80% of them are located in the thickness range of 4–8 nm (Fig. 2.1d). In addition, the total yield of graphene flakes is nearly  $\sim 50\%$ , which is two folds of that of the control design.

FT-IR, XPS, and Thermogravimetric analysis (TGA) were employed to shed more light on the element information of the resultant samples. The presence of various functional groups including C–O (at  $1060\text{ cm}^{-1}$ ), C–O–C ( $1250\text{ cm}^{-1}$ ), C=O/COO (at  $1690\text{--}1710\text{ cm}^{-1}$ ), and COO–H/CO–H ( $1365\text{ cm}^{-1}$ ) [14] was observed (Fig. 2.2a). These functional groups can be eliminated by heating. The weight loss at  $\sim 100\text{ }^{\circ}\text{C}$  in TGA (Fig. 2.2b) is due to the vaporization of adsorbed moisture or water. There is a major weight loss that starts at  $\sim 150\text{ }^{\circ}\text{C}$  and continues up to  $800\text{ }^{\circ}\text{C}$ , which certainly results from the decomposition of functional groups. More significant loss for “MEE” graphene than “SEE” one (30% wt. vs. 20% wt.) indicates there are less functional groups on the “SEE” sample [15]. The presence of oxygen functional groups is further verified by XPS C1 s spectra

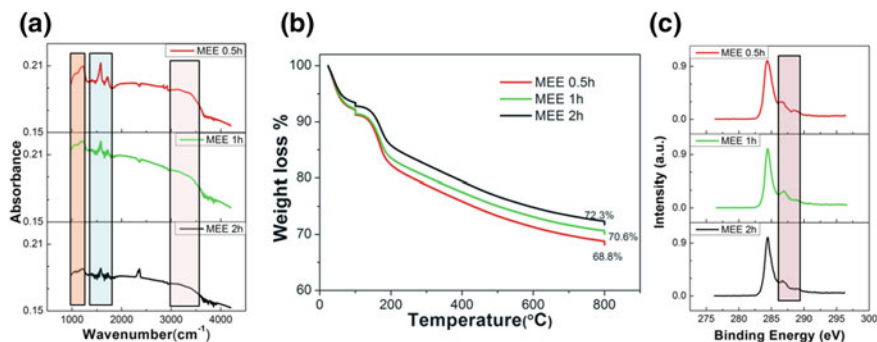


**Fig. 2.1** **a** TEM image and corresponding selected area electron diffraction pattern of the multiple electrochemical exfoliation (MEE) graphene flakes. **b** AFM image of exfoliated graphene flakes spin-coated onto a SiO<sub>2</sub> (285 nm)/Si substrate. The thickness is  $\sim 4.84$  nm, corresponding to 10–15 layers. **c** The low-magnification optical microscopy image of the MEE graphene flakes on SiO<sub>2</sub>/Si substrate. **d** Lateral size and thickness distribution histograms of the MEE graphene sheets, as estimated from corresponding AFM images. The graphene flakes are mainly distributed in the range of 2–8 nm thickness ( $\sim 80\%$ ) with lateral size about 1–5  $\mu\text{m}$ . Figure reproduced from Ref. [12]



**Fig. 2.2** **a** FTIR spectrum, **b** TGA plots and XPS C1 s spectra **c** for raw materials, parallel configuration graphene flakes and MEE graphene flakes

(Fig. 2.2c). In which, the peaks at 286, 287 and 289 eV in XPS C1 s spectra (blue area), which are assigned to C–O, C=O and carboxyl groups, respectively, were identified. This corroborates the significant oxidation of MEE graphene [16].



**Fig. 2.3** FT-IR spectra **a**, TGA curves **b** and XPS C1 s spectra **c** of MEE GO prepared with different reaction time

The electrolysis time is found to be important for controlling the quality of graphene, including oxidization state, thickness/lateral size distribution and production efficiency. Specially, the FTIR intensity of typical functional groups peaks, such as C–O (at  $1060\text{ cm}^{-1}$ ) and C–O–C ( $1250\text{ cm}^{-1}$ ), C=O stretch in carboxylic acid ( $1690\text{--}1710\text{ cm}^{-1}$ ), and COO–H/CO–H ( $1365\text{ cm}^{-1}$ ) remarkably decrease with the increase of exfoliation time (Fig. 2.3a). This is attributed to the remove of function groups upon heating with prolonging the reaction time [17]. This phenomenon is further confirmed by TGA results, in which slightly decrease in the total weight loss are observed (Fig. 2.3b), i.e. 31.2%, 29.4% and 27.7% for MEE 0.5 h, MEE 1 h and MEE 2 h, respectively. Particularly, a remarkable decrease in hydroxyl content (C–O,  $286.6\text{--}286.8\text{ eV}$ ) was observed from MEE 0.5 to MEE 2 h (Fig. 2.3c).

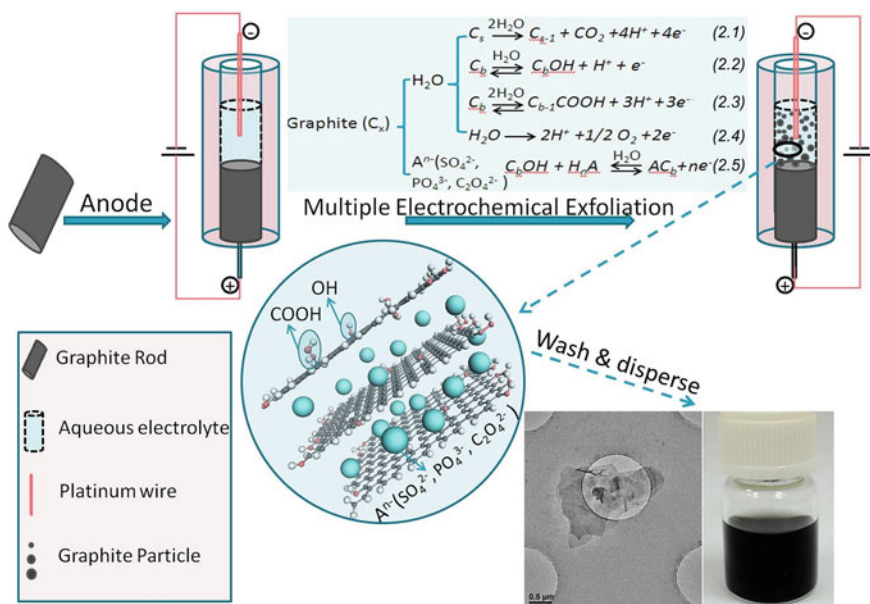
Electrolyte plays an important in efficient electrochemical exfoliation of graphene precursors. Various aqueous protonic acids including phosphoric acid, oxalic acid, sulfuric acid, acetic acid and formic acid were explored. These acids with bulky anions, such as phosphoric acid, sulfuric acid, and oxalic acid were proven to be effective in the exfoliation of spent graphite rod. The diverse choices of aqueous electrolyte provide us with more freedom to adjust the oxidization states of exfoliated graphene and reduce the production cost further. Oxalic acid solution is of particular interest due to: (i) the exfoliation process is faster; (ii) the oxalic acid exfoliated graphene exhibit better solubility in DI water, and (iii) the post-treatment is much easier. Poor performance have been observed for formic acid and acetic acid. This probably results from the weak anion salvation and weak expansion of graphite sheets upon the intercalation of  $\text{HCOO}^-$  or  $\text{H}_3\text{CCOO}^-$ , due to the their smaller size [18].

Previously reports indicated that the successful electrochemical exfoliation of graphite was strongly dependent on the graphite structure, and hence exfoliation

was observable only on high quality crystalline graphite such as HOPG, natural graphite flakes or paper [19, 20]. In our design, there is no special requirement on the quality and morphology of graphite source. Recycled graphite rod obtained from spent Zn–C primary batteries and pencil core could be equally well exfoliated without the need of special pre-treatment or cleaning. This design would no doubt pave the way for the commercialization of graphene, and also open up a wide opportunity for recycling of spent graphite in future.

### 2.3.2 The Mechanism for Electrochemical Exfoliation

Upon a high potential ( $\sim 6\text{--}8\text{ V}$ ) is applied across the two electrodes, the electrolyte anions such as  $\text{OH}^-$ ,  $\text{HSO}_4^-$  and  $\text{SO}_4^{2-}$  and their solvated complexes (in the case of dilute  $\text{H}_2\text{SO}_4$  being used as the electrolyte) are driven to graphite anode (Fig. 2.4). Electrochemical oxidation reactions (Eqs. 2.1–2.4) including the anodic



**Fig. 2.4** Schematics of multiple electrochemical exfoliation (MEE) process. The digital photograph of the dispersed exfoliated graphene sheets in DMF solution, and the corresponding typical TEM images are shown. The mechanism of electrochemical exfoliation that consisting of anodic oxidation of graphite (Eqs. 2.1–2.3) and water (Eq. 2.4), and the intercalation of anions into graphite rod ( $\text{C}_s$ —surface of graphite rod,  $\text{C}_b$ —bulk of graphite rod) (Eq. 2.5), is illustrated. Schematic of graphite intercalation compound (GIC) with both hydroxyl and carboxyl groups formed is shown. Figure reproduced from Ref. [12]



oxidation, hydroxylation and carboxylation of graphite (as well as water oxidation), were triggered by the current flow accompanying with the remove of the electrons from anode (Fig. 2.4). These processes take place initially at the surface, grain boundary or structural defect sites, generating  $\bullet\text{OH}$ ,  $\bullet\text{COC}$ ,  $\text{CO}\bullet$ , and  $\text{COO}\bullet$  functional groups on the graphite surface. During these processes,  $\text{CO}_2$  and  $\text{O}_2$  can be produced as the electrolysis products (Eqs. 2.1 and 2.4) [21, 22]. The release of gaseous bubbles was obviously observed during the electrochemical process, which became vigorous with increasing exfoliation time, as if water boiled. The anodic corrosion/etching as well as the violent gas release open up the edge sheets of the graphite rod and facilitate the intercalation of bulky anions (as well as their solvated moieties) into the graphite layers, forming graphite-intercalation-compounds (GIC) ( $\text{C} + \text{A}^- \rightarrow \text{CA} + \text{e}^-$ ) (Eq. 2.5). The intercalation and the hydrolysis of the intercalated complex ( $\text{CA} + \text{H}_2\text{O} \rightarrow \text{COH} + \text{H}^+ + \text{e}^-$ ) [18, 23] lead to the expansion of graphene sheets and the cleavage/exfoliation of functional graphene sheets. Here, a mixture of GIC and graphite oxide is obtained. The exfoliated particles can be pushed up by the gas bubbles if they are small in size or light in weight. Or they would sink if the exfoliated particles are large and heavy. Nevertheless the precipitating big GIC particles can continue the electrochemical exfoliation when they have electric contact with anode. Multiple exfoliation process would proceed until smaller graphene sheets form and suspend in the solution. Therefore, the exfoliated graphene sheets produced in vertical design are thinner and better distributed in layer numbers.

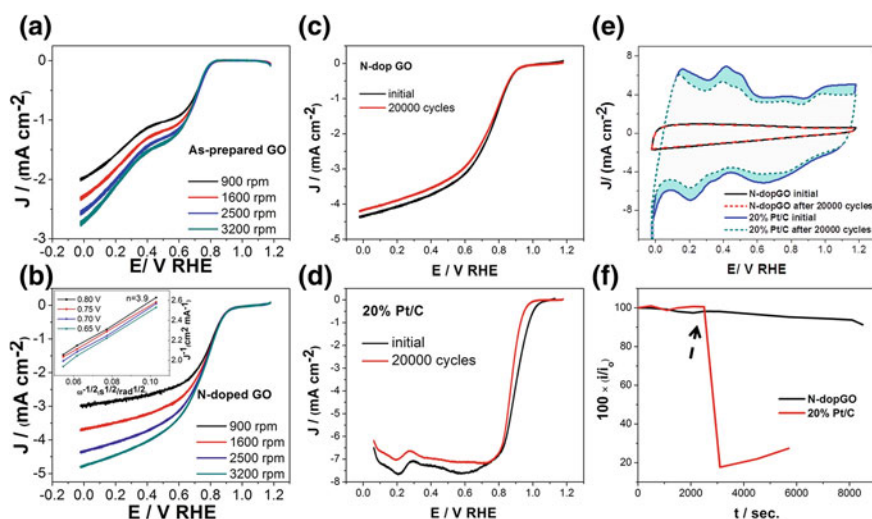
### 2.3.3 *Electrochemical Performance of Resulted Graphene Flakes*

The graphene flakes were used as electrocatalysts for oxygen reduction reaction (ORR). To optimize their electrocatalytic performance further, nitrogen-doping was performed *via* annealing as-prepared MEE-Graphene in  $\text{Ar}/\text{NH}_3$  atmosphere. The appearance of  $\text{N}1\text{ s}$  peaks and a sharp decrease in the intensity of  $\text{O}1\text{ s}$  peaks in XPS spectra corroborate the incorporation of N, and the reduction/remove of functional groups. The calculated N/C atomic ratio is 5.4 atomic %, similar to the values of N-doped graphene [24, 25]. The high resolution XPS  $\text{N}1\text{ s}$  spectrum reveals the presence of pyridinic N (398.2 eV), pyrrolic N (400.5 eV), quantum N (401.1 eV) and N-oxides of pyridinic N (402.1 eV). These nitrogen-doped active sites are of particular interest for improving ORR electrocatalytic performance of carbon materials [24, 25].

The ORR catalytic activities of the MEE graphene before and after N-doped were investigated using rotating disk electrode (RDE) measurements in  $\text{O}_2$ -saturated 0.1 M KOH electrolyte (Fig. 2.5). A clear two-step process with

onset potentials at 0.82 V and 0.40 V, respectively, has been identified for the as-prepared MEE graphene, consisting well with previous reports on pure CNT [26] and graphene [27] (Fig. 2.5a). On the other hand the N-doped graphene electrode exhibits a well-defined, one-step process, suggesting a four-electron pathway for ORR on N-doped graphene (Fig. 2.5b). Furthermore, a much more positive ORR onset potential (0.92 V, vs. RHE) and higher cathodic currents are identified, corroborating the enhanced ORR catalytic performance [28]. The increase in electrocatalytic sites during N-doping process and the reduction of graphene are responsible for the enhanced ORR activities. Moreover, the corresponding Koutecky-Levich plots at different potential exhibit good linearity, and their slopes were nearly the same over the potential range of 0.65–0.80 V, indicating the first-order reaction kinetics with almost constant electron-transfer numbers for ORR over a wide electrode potential (inset in Fig. 2.5b) [29]. The electron-transfer number  $n$  was calculated to be 3.9 according to the slopes of Koutecky-Levich plots, suggesting that nearly four-electron transfer process taken place in this potential range.

The stability tests were conducted in order to confirm the feasibility of MEE N-doped graphene for ORR application. There is only slightly decrease in limiting current, and the onset potential remains the same (Fig. 2.5c). The good catalytic stability was further confirmed by the overlap of CV curves before and after 20,000



**Fig. 2.5** ORR curves for as-prepared graphene **a** and N-doped graphene **b** in O<sub>2</sub>-saturated 0.1 M KOH solution. The inset in **b** shows corresponding Koutecky-Levich plots derived from the ORR measurements. Polarization curves of N-doped G **c** and 20% Pt/C catalysts **d**, before and after 20,000 potential cycles. (Sweep rate, 100 mV/s; rotating rate, 2500 rpm.) **e** Cyclic Voltammerty curves of N-doped GO and 20% Pt/C catalysts before and after 20,000 cycles. **f** Current ( $i$ )-time (t) chronoamperometric responses to methanol. The arrow indicates the addition of 2% (weight ratio) methanol. Figure reproduced from Ref. [12]

cycling (Fig. 2.5e). Unlike N-doped graphene electrode, negative shifts in onset potential, reduction in limiting current as well as loss of surface area of CV curves were observed for 20% Pt/C electrode (Fig. 2.5d and e).

The N-doped graphene was further subjected to test the poisoning effect in the presence of methanol. As illustrated in Fig. 2.5f, the current response decreases sharply upon the addition of 2 wt% methanol for 20% Pt/C electrode. In contrast, the N-doped graphene electrode displays a strong and stable amperometric response, indicating a high selectivity due to the much lower ORR potential than that required for oxidization of methanol molecules [27, 30].

## 2.4 Conclusion

In conclusion, a simple, green and cost effective multiple electrochemical exfoliation approach has been proposed for synthesizing graphene in high quality and quantity. The mechanism of multiple electrochemical exfoliation of graphite was elucidated in detail. The experiment conditions are optimized. The nitrogen-doped graphene sheets have been demonstrated to deliver good electrocatalytic activity, stability and toxicity tolerance for alkaline electrolyte-based oxygen reduction reaction. Our present findings pave the way for scaled-up preparation, and further commercialization of graphene in a low cost and environmentally friendly way.

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## Chapter 3

# High-Performance Graphene Foam/ $\text{Fe}_3\text{O}_4$ Hybrid Electrode for Lithium Ion Battery

The development of deformable electrodes with good electrochemical performance in addition to ultrathin, lightweight and flexible, is one key challenge in flexible electrochemical energy storage devices. Graphene foam (GF), is a three-dimensional (3D) interconnected network of high-quality chemical vapour deposition-grown graphene. It possesses high porosity, good electric conductivity and mechanical integrity, and is a good scaffold for flexible electrodes. In this chapter, thin, lightweight, and flexible  $\text{Fe}_3\text{O}_4$ /GF electrode has been designed based on the 3D interconnected current collector via a bottom up approach assisted by atomic layer deposition. The 3D interconnect feature of GF provides a highly conductive pathway for ions and electrons. Benefiting from the unique design, the electrode delivers high reversible capacity and fast charge/discharge capability.

### 3.1 Introduction

The prosperity of hybrid electric vehicles (HEV), portable electronics and micro-electro-mechanical systems (MEMS) has promoted increasing demand for high-performance lithium ion batteries (LIB) [1, 2]. The achievements are strongly dependent on scrupulous selection of active materials and unique nanostructures design that ensuring fast pathway for electron/ions diffusion.  $\text{Fe}_3\text{O}_4$  has been demonstrated to be an attractive anode material due to high theoretical energy capacity, low cost, low toxicity, and ease of fabrication [3, 4]. However,  $\text{Fe}_3\text{O}_4$  always suffers from poor cyclability caused by drastic volume expansion during  $\text{Li}^+$  ion intercalation/de-intercalation process [4]. Particularly, the loss of electrical connection of  $\text{Fe}_3\text{O}_4$  from current collectors resulting from high volume changes during continuous charge–discharge process has been reported, which significantly limits its practical application [5]. Many approaches have been proposed to address this challenge, such as fabricating  $\text{Fe}_3\text{O}_4$  nanomaterials into optimized nanostructure

and shapes [6–9] or embed the active materials in a cushioning medium including conductive medium [10–15] or other stable metal oxides [16, 17].

Building nanostructures is considered as an effective strategy to improve the electrochemical performance of the LIB electrode benefiting from several advantages over their bulk counterparts [6, 15, 18–20]. (i) The nanostructure processes a short transport path for Li<sup>+</sup> diffusion. (ii) The well electric/mechanical contact at electrode/electrolyte interface ensures facile charge transport. (iii) The nanostructure could accommodate the large volume expansion during charge/discharge process, and maintain the structural integrity of the electrode. Indeed various nanostructures including solid/hollow nanoparticle [21, 22], nanotube [7], nanowire [23], porous nanosheet [24], and nanowall [25], have been designed to improve the performance of iron oxide-based electrodes. In addition, through combining with other conductive additives, such as metal nanostructures [10], polymers [26], carbon materials [12, 13, 15] and other stable materials [17], the electric conductivity of iron oxide-based electrode could be further optimized via reducing the diffusion length. Particularly, the hybridization of Fe<sub>3</sub>O<sub>4</sub> with carbon allotropes including porous carbon, carbon nanotubes and graphene, provides great opportunity in improving the performance of Fe<sub>3</sub>O<sub>4</sub> as the LIB electrodes [11, 24, 27].

Although intense efforts have been made, the improvement in electrochemical performance of Fe<sub>3</sub>O<sub>4</sub> LIB electrode is still marginal. The fabrication of Fe<sub>3</sub>O<sub>4</sub> based electrodes with good rate performance and long cycle life is still challengeable but highly desirable. In this work, GF/Fe<sub>3</sub>O<sub>4</sub> hybrid electrode was prepared via a novel and facile bottom up approach. The unique hybrid electrode delivers several characteristics: (i) good electric contact and facile electron/ions transportation [28, 29]; (ii) good mechanical contact and integrity ensures long cycle time; (iii) adjustable and large active material loading; (iv) lightweight, flexible features ensures that the GF/Fe<sub>3</sub>O<sub>4</sub> hybrid electrode used directly without the employing of binder or other conducting additive. Benefiting from this unique design, the GF/Fe<sub>3</sub>O<sub>4</sub> hybrid electrode demonstrates good cycling performance (up to 500 cycles) and fast charge/discharge feature (10 C) [30].

## 3.2 Experiment and Characterization

### 3.2.1 Materials Synthesis

*Synthesis of graphene foams.* The 3D graphene foams were prepared via chemical vapour deposition [28, 31].

*Synthesis of ZnO.* Prior to ALD deposition, GF was treated with oxygen plasma (March PX-250 plasma etching system). The diethyl zinc (DEZ, 99.99%, Sigma Aldrich) and H<sub>2</sub>O were adopted as the Zn and O precursors for the deposition of ZnO (Beneq TFS 200 system) at 200 °C. The thickness was controlled by the deposition cycles. Samples with thickness of 10, 30, and 50 nm, were prepared in this work.

*Formation of  $\text{Fe}_3\text{O}_4$  nanostructure.* The GF/ $\text{Fe}_3\text{O}_4$  electrode is achieved via (i) bathing ZnO-coated GF into a mixture of  $\text{FeCl}_3$  (30 mM) and glucose solution (30 mM) for 24 h, and followed with (ii) annealing in Ar atmosphere at 400 °C for 2 h.

### 3.2.2 Material Characterization

*Structure and Morphology Characterization.* The morphology of the samples were characterized with JEOL JSM 6700F field emission scanning electron microscopy (SEM) and JEOL JEM-2010 transmission electron microscopy (TEM). The element chemical information is collected via X-ray photoelectron spectroscopy (XPS) [VG ESCALAB 220i-XL system, monochromatic Al K $\alpha$ 1 source (1486.6 eV)] and Thermogravimetric analysis (TGA) (TGA Q500, Thermal Analysis Instruments, Burlington, MA).

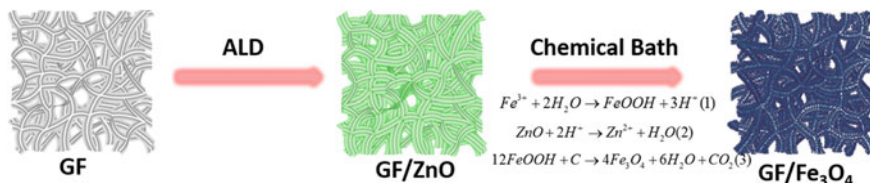
*Electrochemical Performance Evaluation.* Electrochemical performance was evaluated on CR2032-coin-type cells using the free-standing GF/ $\text{Fe}_3\text{O}_4$  as working electrode and lithium foil as the counter electrode. The electrolyte was 1 M  $\text{LiPF}_6$  in a mixture organic solvent consisting of ethylene carbonate (EC) and diethyl carbonate (DEC) (1:1 v/v). The assembled cells were assembled and aged in the glove box prior to the electrochemical measurements. Galvanostatical discharge/charge testing were performed over the voltage range of 0.01–3.0 V (vs.  $\text{Li}^+/\text{Li}$ ) using a NEWARE cell tester. The cyclic voltammetry (CV) and electrochemical impedance spectroscopy (EIS) were carried out using a CHI 660D workstation (CHI instrument Co. Shanghai).

## 3.3 Results and Discussions

### 3.3.1 The Synthesis of GF/ $\text{Fe}_3\text{O}_4$ Hybrid Films

Three steps are involved for the synthesis of the GF/ $\text{Fe}_3\text{O}_4$  nanostructure electrodes (Fig. 3.1). Firstly, self-supported graphene foam was achieved via (i) catalytic decomposition of  $\text{CH}_4$  on Ni foam, and (ii) the etching away of Ni backbone (Fig. 3.1a) [28]. Secondly, ALD-deposited ZnO coated onto the graphene foam, forming a thin layer (Fig. 3.1b). ALD is a thin film deposition technique that lead to uniform and conformal films with precise thickness control via self-limiting surface reactions [32, 33]. GF was treated by oxygen plasma prior to ALD to introduce hydroxyl bonds on the surface, and ensure the conformal coating of ZnO [34, 35]. Thirdly, ZnO was converted into  $\text{FeOOH}$  via bathing GF/ZnO into the mixed solution of  $\text{FeCl}_3$  solution with glucose. The bicontinuous/mesoporous GF/ $\text{Fe}_3\text{O}_4$  was then obtained after annealed in Ar atmosphere (Fig. 3.1c). The glucose is



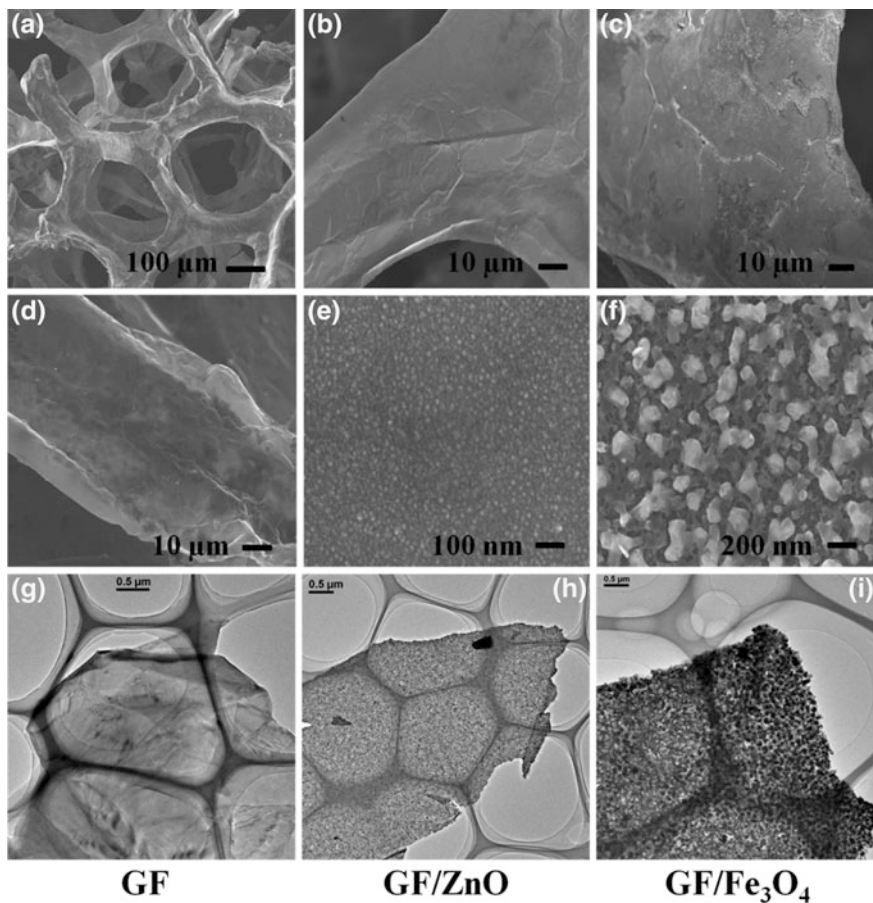


**Fig. 3.1** Schematic illustration of the indirect ALD approach. Figure reproduced from Ref. [30]

converted into amorphous carbon that surrounding around the Fe<sub>3</sub>O<sub>4</sub> nanoparticles accompanying with pyrolysis process [15]. The indirect ALD approach for the synthesis of GF/Fe<sub>3</sub>O<sub>4</sub> in this work is superior over the direct ALD coating method in terms of high growth rate, large active materials loading, and flexible/low requirements for temperature and ozone atmosphere [36, 37]. More importantly, different from the compact thin film formed in traditional ALD approach, unique bicontinuous/mesoporous-nanostructure could be generated, which is particularly favorable for the fast charge/discharge electrode.

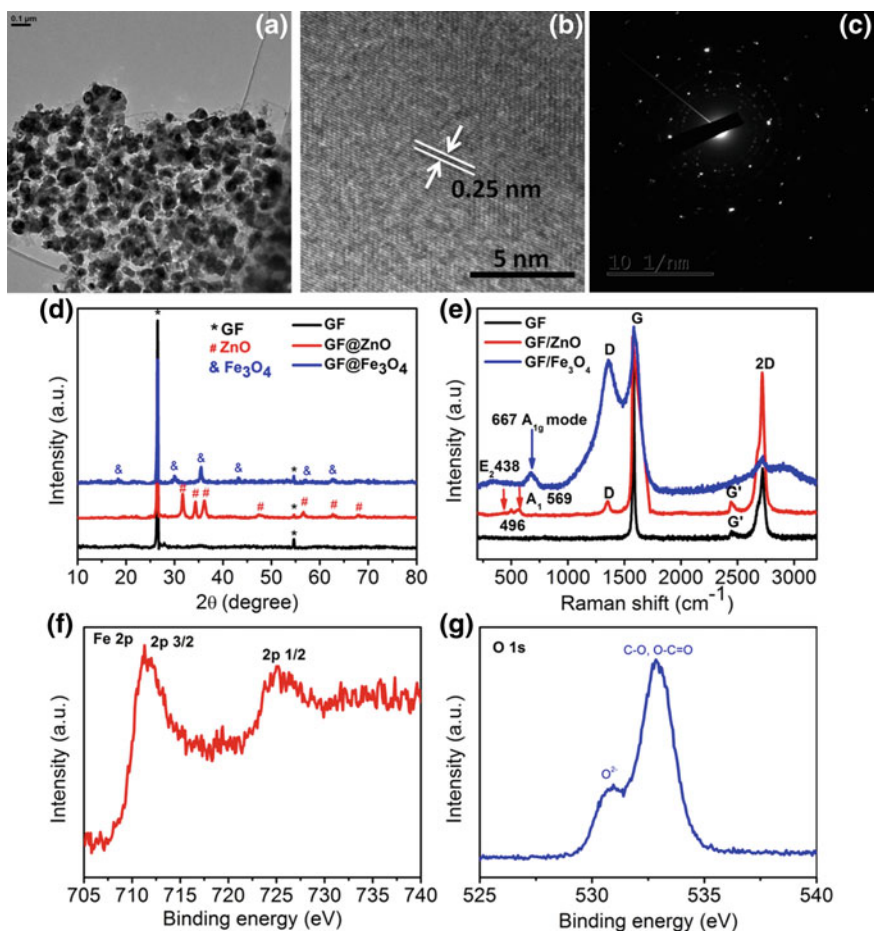
The morphology of the GF/Fe<sub>3</sub>O<sub>4</sub> hybrid structure is characterized via SEM and TEM. GF inherits the 3D structure of the Ni foam backbone well, with porous feature (Fig. 3.2a, d). GF is ultrathin and lightweight, and its thickness or the areal density (0.1–0.8 mg cm<sup>-1</sup>) could be tuned via controlling the carbon source amount and growth time. There is no obvious change in the morphology of graphene foam after ZnO coating, corroborating the conformal coating of ZnO (Fig. 3.2b). More details about the tiny particle of ZnO could be found in Fig. 3.2e and h. The uniform coating of ZnO is the key prerequisite for the good coverage of Fe<sub>3</sub>O<sub>4</sub> on GF. By adjusting the deposition amount of ZnO, the mass loading of the Fe<sub>3</sub>O<sub>4</sub> can be easily controlled. The graphene foam surface becomes rough, covered by small particles, after the replacement reaction of ZnO into Fe<sub>3</sub>O<sub>4</sub> (Fig. 3.2f and i). The formation of bicontinuous/mesoporous nanostructure with Fe<sub>3</sub>O<sub>4</sub> nanocrystallites interconnected with each other was clearly observed (Fig. 3.3a). The HRTEM image (Fig. 3.3b) and corresponding SAED image (Fig. 3.3c) reveal that the nanoparticle is single crystalline with an average diameter of 30 nm. The lattice fringe distance of 0.25 nm, corresponding to the (311) plane of Fe<sub>3</sub>O<sub>4</sub>, is also identified.

To learn more about the structure and composition of the GF/Fe<sub>3</sub>O<sub>4</sub> electrodes, X-ray diffraction (XRD), Raman spectroscopy and X-ray photoelectron spectroscopy (XPS) measurements were conducted. Two typical diffraction peaks at 26.5 and 54.6° are observed for GF, corresponding to the (002) and (004) reflection planes of graphitic carbon (JCPDS card 75-1621), respectively (Fig. 3.3d) [38]. More diffraction peaks appear for GF/ZnO composites, result from the hexagonal structure of ZnO (JCPDS card 36-1451). The high deposition temperature ensures that ALD ZnO is crystalline. After the replacement of ZnO with Fe<sub>3</sub>O<sub>4</sub>, the characteristic peaks of ZnO disappear accompanying with the appearance of the typical peaks of magnetite Fe<sub>3</sub>O<sub>4</sub> (JCPDS, card 19-0629) (Fig. 3.3d). In Raman spectra (Fig. 3.3e), three typical peaks of graphene, centering at 1580 cm<sup>-1</sup> (G), 2550 cm<sup>-1</sup> (G'), and 2720 cm<sup>-1</sup> (2D) are identified [28, 31, 38]. The absence of



**Fig. 3.2** SEM images of GF (a, d), GF/ZnO (b, e) and GF/Fe<sub>3</sub>O<sub>4</sub> (c, f). TEM images of GF (g), GF/ZnO (h), and GF/Fe<sub>3</sub>O<sub>4</sub> (i). Figure reproduced from Ref. [30]

the defect-related D band at  $1350\text{ cm}^{-1}$  corroborates the high quality of the GF. The Raman intensity of the 2D band is much smaller than the 2D band, indicating that the GF is multilayer [31, 38]. These features make GF to be promising scaffold for electrodes. Three more Raman peaks appear at  $438$ ,  $496$ , and  $569\text{ cm}^{-1}$  after the ZnO deposition, corresponding to ZnO E<sub>2</sub> and A<sub>1</sub> phonons, respectively [39]. Some defects were introduced after the ZnO deposition, accompanying with the appearance of the D band. The typical Raman modes of Fe<sub>3</sub>O<sub>4</sub> can be clearly identified at  $667\text{ cm}^{-1}$  for GF/Fe<sub>3</sub>O<sub>4</sub> composite, corresponds to the A<sub>1g</sub> mode (Fig. 3.3e) [11]. In addition, an enhanced D band and a broadened but decreased 2D band are observed. The former is attributed to the introduction of more defects, while the latter may originates from the amorphous carbon layer that surrounding around Fe<sub>3</sub>O<sub>4</sub> surface [40]. Corresponding XPS results were illustrated in Fig. 3.3f and g. Two typical



**Fig. 3.3** HRTEM image of GF/Fe<sub>3</sub>O<sub>4</sub> (a), an individual Fe<sub>3</sub>O<sub>4</sub> nanoparticle (b) and SAED patterns of GF/Fe<sub>3</sub>O<sub>4</sub> (c). **d** X-ray diffraction patterns and **e** Raman spectra of the GF, GF/ZnO and GF/Fe<sub>3</sub>O<sub>4</sub> nanostructures. XPS of the Fe 2p states (**f**) and the O 1s state (**g**) of Fe<sub>3</sub>O<sub>4</sub>

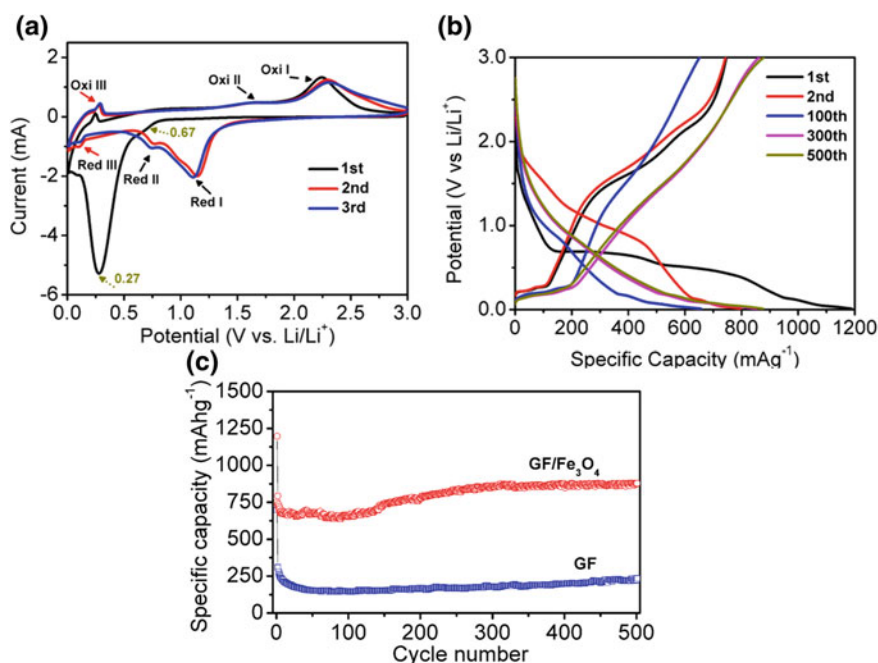
characteristics of Fe<sub>3</sub>O<sub>4</sub> located at 710.9 and 724.2 eV that are corresponding to the Fe 2p<sub>3/2</sub> and 2p<sub>1/2</sub> states, respectively, are found [41]. There is no satellite peak detected, corroborating the final product is Fe<sub>3</sub>O<sub>4</sub> rather than Fe<sub>2</sub>O<sub>3</sub> [41].

### 3.3.2 Electrochemical Performance of GF/Fe<sub>3</sub>O<sub>4</sub>

Cyclic voltammetry (CV) and galvanostatic charge/discharge curves were collected to evaluate the electrochemical property of the GF/Fe<sub>3</sub>O<sub>4</sub> electrodes systematically. There are two well defined reduction peaks located at 0.67 and 0.27 V in the 1st

discharge process (Fig. 3.4a), corresponding to the structure transition ( $\text{Fe}_3\text{O}_4 + x\text{Li}^+ + xe^- \rightarrow \text{Li}_x\text{Fe}_3\text{O}_4$ ) and the further reduction of  $\text{Li}_x\text{Fe}_3\text{O}_4$  to  $\text{Fe}(0)$  by conversion reaction [ $\text{Li}_x\text{Fe}_3\text{O}_4 + (8-x)\text{Li}^+ + (8-x)e^- \rightarrow 4\text{Li}_2\text{O} + 3\text{Fe}$ ] [8, 42, 43]. Note that these two cathodic peaks positively shifted to 1.1 and 0.75 V, with the anodic peaks located at 1.6 and 2.3 V, respectively, for the subsequent cycles. These two redox pairs were attributed to the reversible reduction/oxidation ( $\text{Fe}_3\text{O}_4 \leftrightarrow \text{Fe}$ ) reactions during lithiation/delithiation process [42, 43].

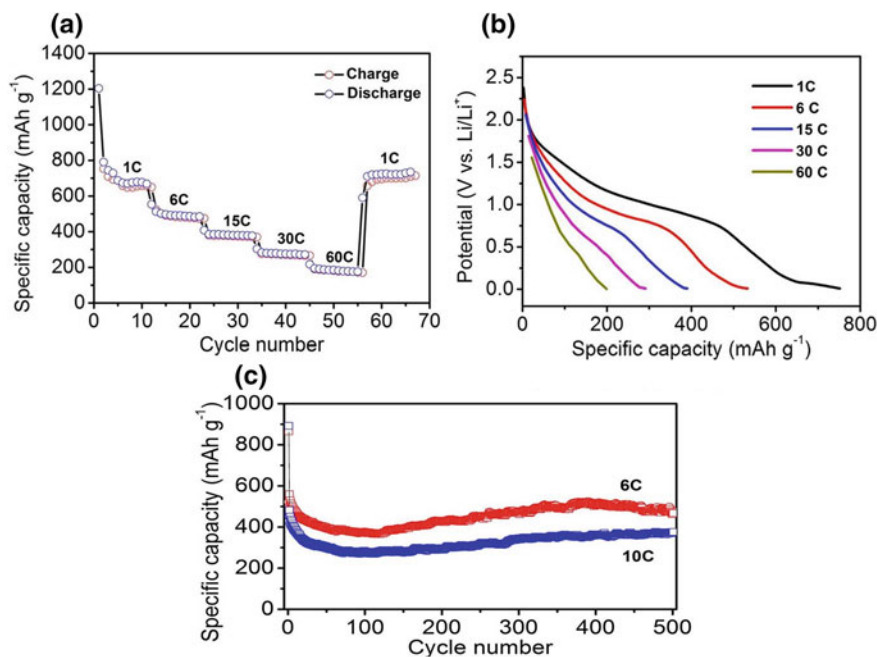
Apart from the reaction peaks for  $\text{Fe}_3\text{O}_4$ , one more redox pair is found at 0.1 V (cathodic) and 0.27 V (anodic), indicating that GF taken part in electrochemical reactions [29, 44]. This redox pair exhibits lower peaks' intensity than those of  $\text{Fe}_3\text{O}_4$ . This is probably because of the high loading of  $\text{Fe}_3\text{O}_4$  (80% of weight percentage) as also confirmed by the TGA result. The 2nd and 3rd CV curves almost overlap with each other, suggesting the good reversibility of GF/ $\text{Fe}_3\text{O}_4$  electrode. There are two voltage plateaus located at 0.4 and 0.65 V in the 1st discharge curve (Fig. 3.4b), corresponding to irreversible reactions induced by the formation of SEI. They disappear since the 2nd cycle, consisting well with the CV curves. The GF/ $\text{Fe}_3\text{O}_4$  hybrid electrode has demonstrated a high initial capacity of  $1192 \text{ mAh g}^{-1}$  in the 1st cycle and a lower capacity of  $785 \text{ mAh g}^{-1}$  in the 2nd cycle, giving rise to a columbic efficiency of 66%. The irreversible reactions



**Fig. 3.4** **a** Cyclic voltammetry (CV) curves, and **b** discharge/charge profiles of the GF/ $\text{Fe}_3\text{O}_4$  electrode. **c** Cycling profiles of the GF and GF/ $\text{Fe}_3\text{O}_4$  electrodes at 1C rate. Figure reproduced from Ref. [30]

involved in the formation of the SEI layer account for the 34% capacity loss [13, 15, 27]. The discharge/charge measurements were carried out up to 500 cycles to evaluate the cycle performance. After deep cycling to 300 and 500 cycles, the plateaus of the discharge–charge profiles are not so evident as in the initial stage (Fig. 3.4b), which are in agreement with the previous reports [43, 45]. The good cyclic performance is revealed in Fig. 3.4c. The capacity decreases slightly for the initial 100 cycles, and then increases gradually. The hybrid electrode could deliver a capacity of 870 mAh/g up to 500 charge/discharge cycles, which is better than that of previous reports [11, 12, 43]. In summary, the electrode displays relatively stable performance and high capacity retention (Fig. 3.4c). On the other hand, pure  $\text{Fe}_3\text{O}_4$  electrode always displays much shorter cycle life (<100 cycles) even at a much smaller charge/discharge rate (i.e., 0.5 C).

Galvanostatic discharge/charge measurements were conducted at various C rates to evaluate the rate performance of GF/ $\text{Fe}_3\text{O}_4$ . The specific capacity decreases with increasing C rates (Fig. 3.5a and b). A specific capacity of 190 mAh  $\text{g}^{-1}$  was achieved at 60 C, suggesting that the full charge could complete in one minutes. The GF/ $\text{Fe}_3\text{O}_4$  hybrid electrode still delivers a high capacity of 800 mAh  $\text{g}^{-1}$  even



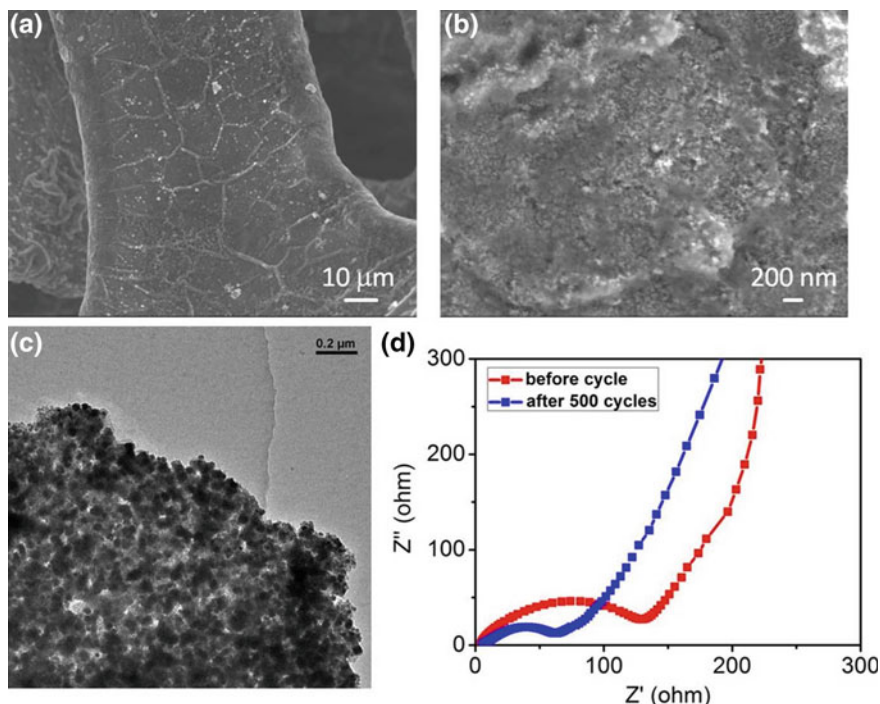
**Fig. 3.5** Rate capability of the GF/ $\text{Fe}_3\text{O}_4$  LIB electrode. **a** Specific capacity of the GF/ $\text{Fe}_3\text{O}_4$  electrode under different discharge/charge rates. **b** Discharge profiles of the GF/ $\text{Fe}_3\text{O}_4$  electrode at different current rates. **c** Cycling profiles of the GF/ $\text{Fe}_3\text{O}_4$  electrodes at 6 and 10 C rates. Figure reproduced from Ref. [30]



when the C rate reduces back to 1 C, corroborating the high stability and good reversibility. The retained capacities of  $\sim 400$  and  $300 \text{ mAh g}^{-1}$  could be identified at 6 and 10 C charge/discharge rates, respectively, till 500 cycles (Fig. 3.5c).

### 3.3.3 Underlying Mechanism for the Enhanced Electrochemical Performance

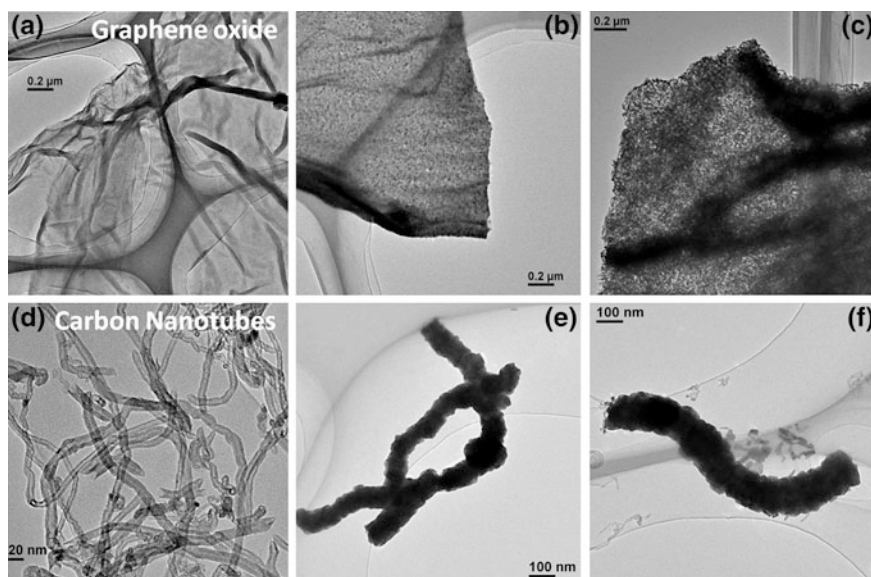
In order to reveal the underlying mechanism for the enhanced electrochemical performance, the composite electrodes were characterized after 500 charge/discharge cycles at 1 C (Fig. 3.6). Despite somewhat pulverization, the  $\text{Fe}_3\text{O}_4$  layer still keeps good electric and mechanical contact with GF, and the individual  $\text{Fe}_3\text{O}_4$  nanocrystallites can still be well maintained (Fig. 3.6a–c). Corresponding electrochemical impedance spectroscopy (EIS) results (Fig. 3.6d) reveal an evidently decrease in the charge transfer resistance of  $\text{GF}/\text{Fe}_3\text{O}_4$  after cycling, which is partly attributed to the reduction of  $\text{Fe}_3\text{O}_4$  into Fe during the irreversible reactions.



**Fig. 3.6** SEM images under low magnification (a), high magnification (b) and TEM image (c) of  $\text{GF}/\text{Fe}_3\text{O}_4$  after 500 cycles at 1 C. **d** Electrochemical impedance spectroscopy results for  $\text{GF}/\text{Fe}_3\text{O}_4$  before and after 500 cycles at 1 C

Note that the specific capacity increases with prolonged cycling gradually. Similar trend has been observed for many other metal oxide-based electrodes previously [46–49]. However there is no consensus on the reason until now. There are three possibilities that may take responsible for it: (i) more active sites would be released for lithium storage resulting from the pulverization of the electrode, and thus result in the increase in capacity. (ii) Fe nanoparticles would be generated resulting from the irreversible reactions (SEI formation). The formation of metallic Fe will improve the overall conductivity of the electrode, as evidenced by the EIS results (Fig. 3.6d) [38]. Therefore, the specific capacity would increase benefiting from the enhanced charge-transfer kinetics. (iii) The organic/gel-like SEI layer would form on the electrode surface [12, 46, 49]. It could improve the mechanical cohesion of the active materials without hindering the ion transfer and provide excess lithium ion storage sites by a so-called “pseudo-capacitive-type” behavior, especially in the low potential region.

The good performance of the GF/ $\text{Fe}_3\text{O}_4$  electrodes is attributed to the unique mesoscale structure design that takes advantages of both high electrical conductivity and good structural stability. More importantly, this ALD approach for  $\text{Fe}_3\text{O}_4$  is general and is suitable for other carbon substrates (Fig. 3.7). As mentioned above, the deposition of ZnO is determinant via affecting the homogeneity and mass loading of the resulting active materials. It is foreseeable that, the method we reported here is possible to scale up and push the iron oxide-based LIB electrodes into real applications, given the compatibility with reduced graphene oxide/CNTs, and industry-scale ALD. Note that the total loading amount of the active materials



**Fig. 3.7** TEM images for graphene oxide (a–c) and carbon nanotubes (d–f): **a** GO, **b** GO/ZnO and **c** GO/ $\text{Fe}_3\text{O}_4$ , **d** CNTs, **e** CNTs/ZnO and **f** CNTs/ $\text{Fe}_3\text{O}_4$ . Figure reproduced from Ref. [30]

is not high in our work, which also retards the practical application. This issue could be addressed by stacking the as fabricated GF supported active material electrodes together to form a multilayer film [30].

### 3.4 Conclusion

In conclusion, a novel approach to prepare bicontinuous-mesoporous  $\text{Fe}_3\text{O}_4$  nanostructures on 3D GF has been demonstrated. Benefiting from the rational design and the unique mesoscale structure, a high capacity of  $785 \text{ mAh g}^{-1}$  (1 C) could be collected and maintained up to 500 cycles. Even at the high rate of 60 C, the electrode could deliver a capacity of  $190 \text{ mAh g}^{-1}$ . The good electrochemical performance is attributed to the tightly grafting of  $\text{Fe}_3\text{O}_4$  onto GF that benefits from the uniform ALD coating of ZnO. Particularly, this fabrication method is general and suitable for many other conductive substrates.

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## Chapter 4

# Graphene Foam (GF)/Carbon Nanotubes (CNTs) Hybrid Film-Based High-Performance Flexible Asymmetric Supercapacitors

In Chap. 3, graphene foam (GF) has been described to be an attractive scaffold for flexible electrodes. However, bearing in mind that high active material loading with good electric/mechanical contact in electrodes is critically important for high-performance flexible devices, the relatively low active material loading results from insufficient surface area of GF limits the practical applications of GF as efficient electrode support for flexible and lightweight energy storage devices. In order to further increase active material loading, a facile approach was developed for fabricating a novel 3D electrode support consisting of graphene foam (GF) with covalently bonded carbon nanotubes (CNTs) in this chapter. This hybrid structure extends the 2D plane of Graphene into 3D directions without sacrificing electric conductivity and mechanical integrity. The asymmetric supercapacitors (ASCs) based on the unique GF/CNTs hybrid films deliver high energy/power density and good cycling stability in addition to good mechanical flexibility.

### 4.1 Introduction

Carbon is a fascinating material that exists in various structural forms by different hybridization ways of atomic orbitals ( $sp^2$  and  $sp^3$ ). There are many different kinds of low-dimensional carbon allotropes, such as zero-dimensional fullerenes, one-dimensional carbon nanotubes and two-dimensional graphene, in addition to bulk phases of carbon (graphite, diamond) [1, 2]. The diversity of microstructures and bonding types ensures versatility in properties and applications for various carbon allotropes [3, 4]. The hybrid structures of different carbon materials would no doubt further extend the diversity of carbon-based micro-/macrostructures, with integrated properties inheriting from the each constituent structure. Indeed hybrid

structures such as CNTs/fullerenes [5], CNTs/carbon film [6], graphene/CNTs [7–10], and graphene/fullerenes [11], have displayed improved physical/chemical performance over their single component, benefiting from the synergistic effects. These hybrid structures have found wide applications in sensors, drug delivery, nanoelectronics, and energy storage and conversion [12–18]. Theoretical calculation [19, 20] predicated that covalently bonded carbon nanotubes and graphene could lead to superior properties in three dimensions without sacrificing inherited properties in the planar and axial directions. Such hybrid structures would be of particular interest for many applications, especially for implementation in microelectronics and microelectrochemical devices because of good electrical conductivity [21], large specific surface area [22], unique heterogeneous electron transfer and charge carrier rates, and good electrochemical stability [23].

Many approaches, including solution-based processes [9, 12, 24], microwave irradiation [25], and chemical vapor deposition [4, 7, 26–28], have been attempted to prepare high-quality graphene/CNTs hybrid electrodes. You et al. [24] and Yu and Dai [29] synthesized Graphene/CNTs hybrid films with improved electrochemical performance as supercapacitor electrodes via simple liquid phase mechanical mixing approach. However, these kinds of hybrid films exhibit poor electric/mechanic connection between CNTs and graphene, which limits their application in fast charge/discharge power devices. The synthesis of high-quality graphene/CNTs hybrid materials with strong bonding connection among them is therefore highly desirable. *In situ* growth by chemical vapor deposition has been proved to be an effective approach to achieve this. For example, graphene/CNTs hybrid films with good flexibility and electrical conductivity have been synthesized via vertically growing CNTs arrays on catalyst-patterned graphene films [8]. Recently, Zhu and coworkers [26] have demonstrated the covalently-bonded graphene/CNTs hybrid films. Similar results were also reported via the CVD growth of CNTs on nickel-supported graphene [30]. Noted that CNTs are grown only on the graphene surfaces where the catalyst particles are deposited by e-beam evaporation or dip-coating in the above-mentioned studies. The insufficient surface area of these graphene/CNTs hybrid films makes them challenging to achieve high mass loading of electroactive materials per unit area. Therefore, it is highly desirable to design graphene/CNTs hybrid films with strongly electric/mechanical connected and large quantity of CNTs that could substantially extend the porous architecture and enlarge the surface area.

Herein, a unique 3D architecture that consists of carbon nanotubes (CNTs) and graphene foam (GF) has been designed, aiming to increase the amount of CNTs and the subsequent mass loading of electroactive materials while maintaining the good electric/mechanic contact between CNTs and graphene. The catalytic chemical vapor deposition is chosen for the growth of CNTs onto GF. A hydrothermal method is adopted to deposit catalysts onto GF to improve the subsequent loading of CNTs substantially. Asymmetric supercapacitors (ASCs) based on GF/CNTs/MnO<sub>2</sub> positive electrode and GF/CNTs/Ppy negative electrode have been fabricated and demonstrated good electrochemical performance.

## 4.2 Experiment

### 4.2.1 Material Synthesis and Device Fabrication

*Synthesis of Graphene Foam (GF).* Chemical vapor deposition was chosen for the growth of GF on nickel foam [31].

*Synthesis of Graphene Foam (GF)/Carbon nanotubes (CNTs) Hybrid Films.* GF serves as the template for the subsequent growth of CNTs. A hydrothermal method is adopted for the deposition of the NiCo catalyst. The CNT growth is carried out at 750 °C. The gas flow rate of C<sub>2</sub>H<sub>4</sub>, H<sub>2</sub> and Ar is 20, 40 and 100 sccm, respectively.

*Synthesis of GF/CNTs/MnO<sub>2</sub> Hybrid Films.* MnO<sub>2</sub> nanosheets is prepared via hydrothermal method [32]. The samples are denoted as GF/CNTs/MnO<sub>2</sub>-n, where n is the loading amount of MnO<sub>2</sub> (mg/cm<sup>2</sup>).

*Synthesis of GF/CNTs/Polypyrrole (Ppy) Hybrid Films.* A chemical polymerization method is adopted for the synthesis of the GF/CNTs/Ppy hybrid films [33]. The samples are referred as GF/CNTs/Ppy-m. m is the amount of pyrrole monomer (μl) used during the synthesis.

*Assemble of GF/CNTs/MnO<sub>2</sub>//GF/CNTs/Polypyrrole (Ppy) Asymmetric Supercapacitors (ASCs).* ASCs were assembled using an electrolyte-soaked (0.5 M Na<sub>2</sub>SO<sub>4</sub>) separator sandwiched between a piece of GF/CNTs/MnO<sub>2</sub> (1 × 4 cm<sup>2</sup>) and a piece of GF/CNTs/Ppy (1 × 4 cm<sup>2</sup>). The ASC devices are denoted as ASC-n, where n is the loading amount of MnO<sub>2</sub> (mg/cm<sup>2</sup>).

### 4.2.2 Material Characterization

*Structure and Morphology Characterization.* Field-emission scanning electron microscopy (FESEM, JEM-6700F, 10.0 kV), Transmission electron microscopy (TEM, JEM-2010, 200 kV), Raman spectroscopy (Renishaw, 532 nm excitation laser).

*Electrochemical Performance Evaluation.* Cyclic voltammetry (CV) curves, Galvanostatic charge/discharge profiles, and electrochemical impedance spectroscopy (EIS, 100 kHz–0.01 Hz) were collected using CHI 760D workstation. Three-electrode system (working electrode: GF/CNTs/MnO<sub>2</sub> or GF/CNTs/Ppy; reference electrode: saturated Ag/AgCl; Counter electrode: Pt plate) was chosen for individual electrodes' testing. The EIS results are fitted via the software Z-View. Two-electrode system is adopted for the ASCs' testing.

The areal capacitance of the individual electrode is calculated from the corresponding CV curves:

$$C = \frac{1}{s \nu \Delta V} \int_{V_0}^{V_0 + \Delta V} IdV$$

where  $I(A)$  is the response current,  $v$  is the scan rate (V/s),  $s$  is the apparent surface area ( $\text{cm}^2$ ),  $V_o$  is the lower potential limit, and  $\Delta V$  is potential window (V).

The areal capacitance ( $C_s$ ,  $\text{F}/\text{cm}^2$ ) and specific capacitance ( $C_m$ ,  $\text{F}/\text{g}$ ) of ASCs are calculated from corresponding charge/discharge curves:

$$C_s = 4 \frac{I}{s} \frac{dt}{dV} \quad \text{or} \quad C_m = 4 \frac{I}{m} \frac{dt}{dV}$$

The equation:  $C_- V_- = C_+ V_+$ , is used for the charge match between two electrodes. The energy density (E) and power density (P) are calculated according to the equations [18]:

$$E = CV_{\max}^2 / 8$$

$$P = V_{\max}^2 / (4m R_{\text{ESR}})$$

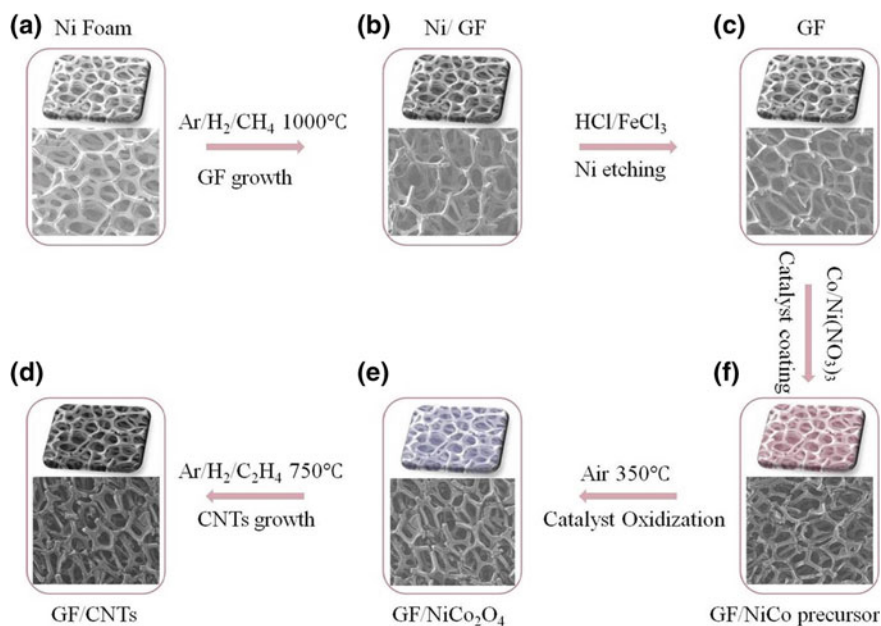
$$R_{\text{ESR}} = V_{\text{drop}} / (2I)$$

where  $V_{\max}$  is the maximum voltage of the ASC,  $R_{\text{ESR}}$  is the equivalent series resistances.

## 4.3 Results and Discussions

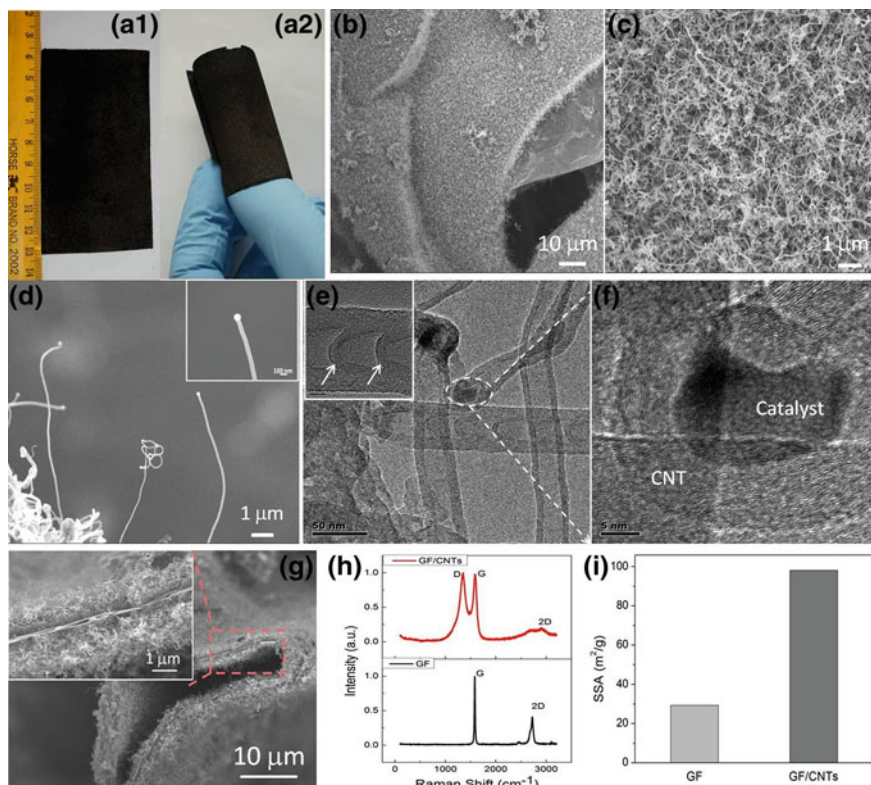
### 4.3.1 Fabrication of GF/CNTs Hybrid Films

Figure 4.1 schematically illustrates the synthesis procedure of the GF/CNTs hybrid film. Three steps are involved: (i) GF is deposited on nickel foam via catalytic decomposing of  $\text{CH}_4$  at  $1000^\circ\text{C}$  (Fig. 4.1a, b). Self-supported GF with intact 3D microstructure is collected via etching nickel substrate (Fig. 4.1c). The areal density of GF could be controlled easily via adjusting growth conditions. (ii) The uniform coating of NiCo-catalyst precursor on GF is achieved via a facile hydrothermal process (Fig. 4.1d). The high loading of NiCo catalysts ensures the large quantity growth of CNTs subsequently, and hence the large surface-to-volume ratio of the GF/CNTs hybrid film. Little defects are introduced, suggesting that the high quality of GF could be well maintained during hydrothermal method process. (iii) GF/NiCo-precursor is converted to GF/ $\text{NiCo}_2\text{O}_4$  by heated in air at  $350^\circ\text{C}$  prior to the growth of CNTs (Fig. 4.1e). This could effectively prevent NiCo catalyst particles from agglomeration at high temperatures, and provide more catalytic sites for the growth of CNTs. The  $\text{NiCo}_2\text{O}_4$  nanoneedles are then reduced to form well dispersed catalyst islands in the presence of  $\text{H}_2$ , and further catalyze the decomposition of  $\text{C}_2\text{H}_4$  to form 3D GF/CNTs framework (Fig. 4.1f). During the synthesis process, apparent color change could be detected, while the macroscopic 3D framework is well preserved.



**Fig. 4.1** Illustration of the growth procedure of GF/CNTs hybrid films

Large sized GF/CNTs hybrid film with good flexibility were prepared based on the above approach (Fig. 4.2a1–a2). The well-defined interconnected network structure of GF/CNTs hybrid film, with a layer of entangled CNTs that surrounding around graphene tightly is detected in Fig. 4.2b and c. The multi-walled CNTs, displays about 15–20 walls, 20–25 nm in diameter and a few hundred nanometers to several micrometers in length (Fig. 4.2d, e, f). A bamboo-like structure with complete knots (indicated by the white arrow) is clearly observed from the inset in Fig. 4.2e, because of the growth of a complete inner graphene layer prior to contraction of the catalyst particle [34, 35]. SEM image (Fig. 4.2d) and TEM images (Fig. 4.2e, f) reveal that most of catalyst particles located at the top of CNTs, corroborating a tip-growth mechanism for the CNTs growth [36]. This feature also further verifies the excellent electric/mechanical interconnection between GF and CNTs. Moreover, there are CNTs on the outer and inner surfaces of GF backbones (Fig. 4.2g). This provides large surface-to-volume ratio for the subsequent electroactive materials deposition. The absence of the D peak at  $1350\text{ cm}^{-1}$  in the spectrum of GF corroborates the high quality of GF (Fig. 4.2h) [37]. A sharp D peak appears after CNTs growth, resulting from the generation of defects during growth process. The introduce of defects was also verified via the corresponding SAED patterns [38]. Nevertheless, GF/CNTs hybrid film exhibits a sheet resistance of  $191\ \Omega/\text{sq}$  ( $178\ \text{S/m}$ ), which is much smaller than that of pure GF ( $352\ \Omega/\text{sq}$ ,  $101\ \text{S/m}$ ), corroborating the good electrical conductivity of GF/CNTs hybrid film. As expected, the 3D architecture of GF is well extended by the densely grown CNTs.



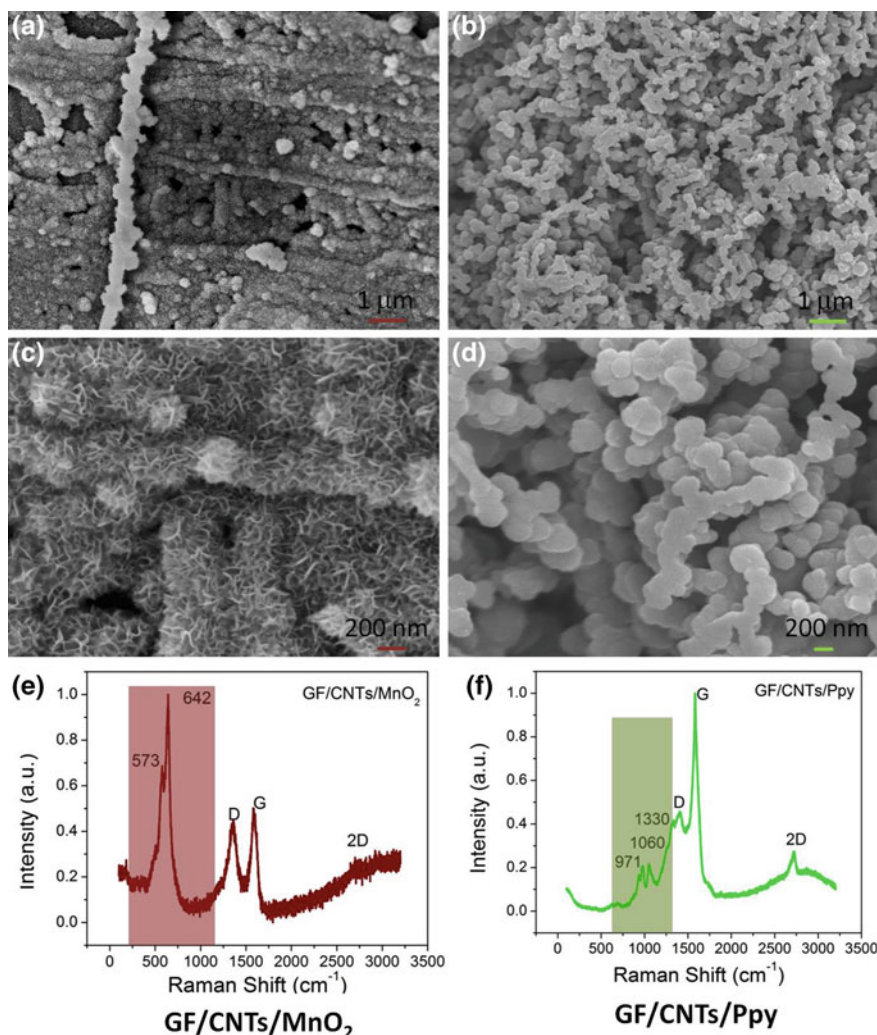
**Fig. 4.2** a1–a2 Representative photograph of the film. b–d Typical FESEM images. e, f TEM images. g Cross-sectional images. h Raman spectra. i Comparative specific surface area (SSA). Inset of (d) suggests the tip-growth mechanism for CNTs. The bamboo-like structure is identified in the inset of (e). The uniform growth of CNTs on both *outer* and *inner* surfaces of GF branches is illustrated in inset of (g). Figure reproduced from Ref. [32]

The GF/CNTs hybrid film exhibits significant increase in surface area (98 m<sup>2</sup>/g vs. 30 m<sup>2</sup>/g for GF) (Fig. 4.2i) [37]. It should be stressed that, the GF/CNTs hybrid films with different CNTs mass loading could be easily prepared by adjusting the growth conditions, offering the possibility to further optimize this kind of hybrid film.

### 4.3.2 Fabrication of GF/CNTs/MnO<sub>2</sub> and GF/CNTs/Ppy Hybrid Films

Figure 4.3a and c reveal the nanostructure of the GF/CNTs/MnO<sub>2</sub> hybrid film, where CNTs are uniformly surrounded by flower-like MnO<sub>2</sub> nanosheets, forming





**Fig. 4.3** Representative FESEM images of GF/CNTs/MnO<sub>2</sub> (a, c) and GF/CNTs/Ppy (b, d). Raman spectra of GF/CNTs/MnO<sub>2</sub> (e) and (f) GF/CNTs/Ppy

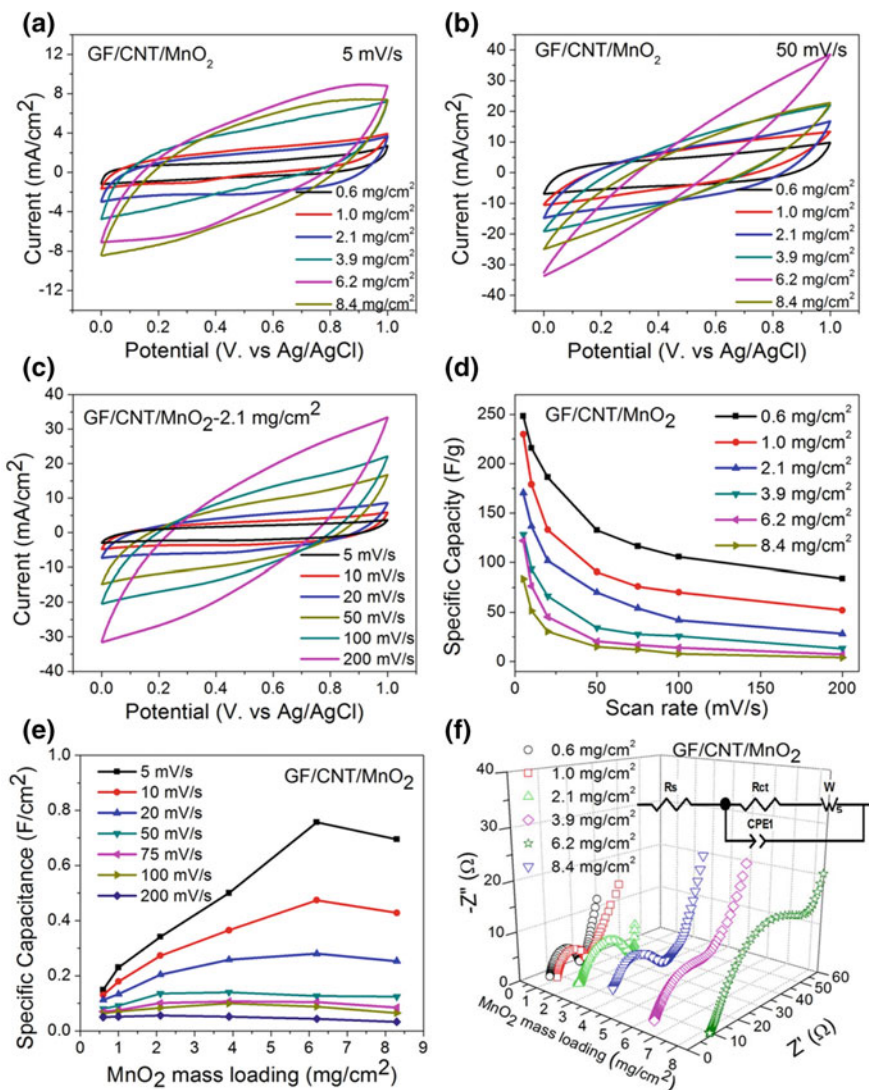
unique CNTs (core)-MnO<sub>2</sub> (shell) nanostructure. A highly porous network was assembled by the flower-like MnO<sub>2</sub> nanosheets with thickness of a few nanometers (Fig. 4.3a, c). The successful deposition of MnO<sub>2</sub> is further verified by the appearance of typical MnO<sub>2</sub> Raman peaks at 568 cm<sup>-1</sup>, 640 cm<sup>-1</sup> as well as the decrease in intensity of G peak (Fig. 4.3e) [39]. This hybrid electrode design provides better current collector/active materials contact, and ensures large accessible surface area and fast mass transfer for electrolyte. It is also found that the introduction of CNTs in the GF is crucial to achieve high loading of active

materials. For example, the areal density of  $\text{MnO}_2$  of GF/CNTs/ $\text{MnO}_2$  film is  $6.2 \text{ mg/cm}^2$  (at 0.6 mM manganese source), which is 6 folds of that of GF/ $\text{MnO}_2$  film. The relatively high and adjustable mass loading of electroactive  $\text{MnO}_2$  on GF/CNTs hybrid film offers the opportunity to optimize the electrochemical performance of the assembled ASC devices further.

Conducting polymers/graphene composites have been investigated intensively as promising electrode materials for supercapacitors [40, 41]. GF/CNTs/Polypyrrole (Ppy) hybrid film was prepared, and used as the negative electrode to match with the GF/CNTs/ $\text{MnO}_2$  hybrid film positive electrode here. The in situ chemical polymerization is chosen for achieving the conformal coating of Ppy on GF/CNTs film (Fig. 4.3b, d) [33]. Corresponding Raman spectrum corroborates the synthesis of Ppy with characteristic peaks at 971, 1060 and  $1330 \text{ cm}^{-1}$  (Fig. 4.3f). A series of samples with different polypyrrole loading amounts were prepared to optimize the electrochemical performance of GF/CNTs/Ppy hybrid film.

### 4.3.3 *Electrochemical Performance of GF/CNTs/ $\text{MnO}_2$ and GF/CNTs/Ppy Hybrid Electrodes*

The electrochemical performance of individual electrode is investigated in a three-electrode system. The electrolyte is 0.5 M  $\text{Na}_2\text{SO}_4$  aqueous solution. The self-supported hybrid film is used as the working electrode directly because of its good electric conductivity and mechanical integrated structure. To investigate the contribution of  $\text{MnO}_2$  to the capacitance in the hybrid electrode and optimize the mass loading of  $\text{MnO}_2$ , a series of CV curves are collected at different sweep rates (Fig. 4.4a, b). The current response increases with the increase in  $\text{MnO}_2$  mass loading density from 0.6 to  $6.2 \text{ mg/cm}^2$ , indicating an increase in the total capacitance [42]. However, the total capacitance decreases when the mass loading density of  $\text{MnO}_2$  further increases to  $8.4 \text{ mg/cm}^2$ . The areal capacitance vs. mass density plots in Fig. 4.4e further support the presence of optimal mass loading density. In which the GF/CNTs/ $\text{MnO}_2$ -8.4 sample displays a lower areal capacitance compared to the sample GF/CNTs/ $\text{MnO}_2$ -6.2, especially at low sweep rates. Electrochemical impedance spectroscopy (EIS) measurements were conducted to understand the inferior performance of GF/CNTs/ $\text{MnO}_2$ -8.4  $\text{mg/cm}^2$  (Fig. 4.4f). The impedance data is fitted with an equivalent electrical circuit consisting of the electrolyte resistance ( $R_s$ ), charge transfer resistance (or polarization resistance,  $R_{ct}$ ), Warburg element (W) and constant phase element (CPE) (inset in Fig. 4.4f) [43, 44]. The charge transfer resistance ( $R_{ct}$ ) is found to increase with the increase of mass loading density. There are two factors accounting for this trend: (i) the poor intrinsic electrical conductivity of  $\text{MnO}_2$ , and (ii) the increase in the thickness of  $\text{MnO}_2$  layer that impedes the ion diffusion and migration process. Interestingly,  $R_{ct}$  increases slightly

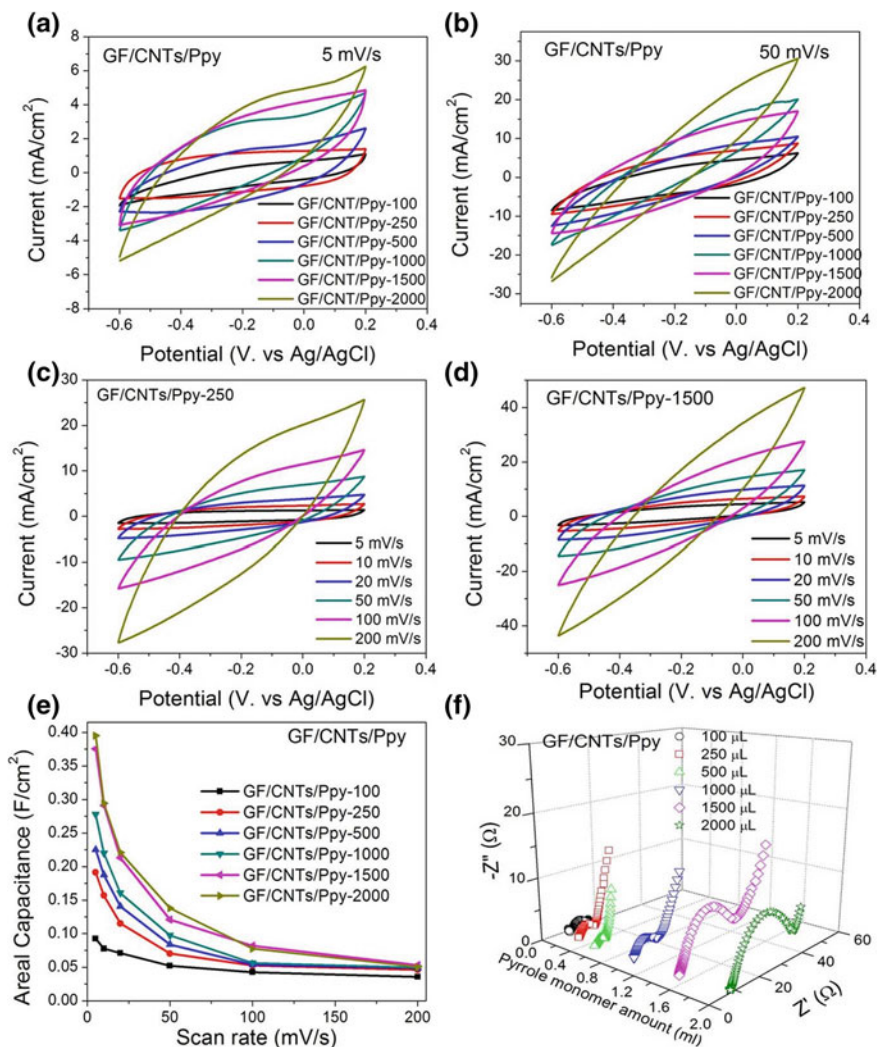


**Fig. 4.4** CV curves of GF/CNTs/MnO<sub>2</sub> hybrid films with different loading of MnO<sub>2</sub> (from 0.6 to 8.4 mg/cm<sup>2</sup>) at the sweep rate of 5 mV/s (a) and 50 mV/s (b). c Rate-dependent CV curves of GF/CNTs/MnO<sub>2</sub>-2.1 hybrid film. d Specific capacitance versus sweep rate for GF/CNTs/MnO<sub>2</sub> hybrid films with different loading of MnO<sub>2</sub>. e Areal capacitance versus mass loading for GF/CNTs/MnO<sub>2</sub> hybrid films at different sweep rates. f Corresponding Nyquist plots of GF/CNTs/MnO<sub>2</sub> hybrid films. An equivalent electrical circuit consisting of the electrolyte resistance (R<sub>s</sub>), interface charge transfer resistance (R<sub>ct</sub>), Warburg element (W) and constant phase element (CPE), is illustrated in the inset of (f). Figure reproduced from Ref. [32]

with the increase of  $\text{MnO}_2$  mass loading from 0.6 to 6.2  $\text{mg}/\text{cm}^2$ , but jumps sharply from 31.6  $\Omega$  (for GF/CNTs/ $\text{MnO}_2$ -6.2) to 56.2  $\Omega$  (for GF/CNTs/ $\text{MnO}_2$ -8.4). This phenomenon excludes the effect of factor i) to some extent, and the factor ii) takes the main responsibility for the sharp increase in  $R_{\text{ct}}$  when the thickness of  $\text{MnO}_2$  layer is close to the diffusion length of  $\text{Na}^+$  at these sweep rates [45]. Typically, the ion diffusion length in GF/CNTs/ $\text{MnO}_2$  hybrid films decreases as the sweep rate increases, thus giving rise to the decrease in the optimal mass loading density. For example, the optimal mass loading density at 75 mV/s is 3.9  $\text{mg}/\text{cm}^2$  whereas it is 2.1  $\text{mg}/\text{cm}^2$  at 200 mV/s.

A series of rate-dependent CV curves of GF/CNTs/ $\text{MnO}_2$ -2.1 hybrid film are plotted to investigate the effect of sweep rates on electrochemical performance (Fig. 4.4c). The CV curves deviate from a rectangular shape of ideal double-layer capacitors, resulting from the relatively large resistance and overpotential [42]. The specific capacitance and areal capacitance of the GF/CNTs/ $\text{MnO}_2$  hybrid films are calculated and plotted (Fig. 4.4d, e). The high specific capacitance of 215 F/g (Fig. 4.4d), which corresponds to 130  $\text{mF}/\text{cm}^2$  (Fig. 4.4e), is obtained for sample GF/CNTs/ $\text{MnO}_2$ -0.6 at a sweep rate of 10 mV/s. The value is higher than those of  $\text{MnO}_2$ -based electrodes in previous reports, such as 62  $\text{mF}/\text{cm}^2$  at 5  $\text{mA}/\text{cm}^2$  for PEDOT/ $\text{MnO}_2$  [46], 70  $\text{mF}/\text{cm}^2$  at 2  $\text{mA}/\text{cm}^2$  for  $\text{TiO}_2/\text{MnO}_2$  [47], 64  $\text{mF}/\text{cm}^2$  at 0.08  $\text{mA}/\text{cm}^2$  for  $\text{SnO}_2/\text{MnO}_2$  [48], 41  $\text{mF}/\text{cm}^2$  at 0.12  $\text{mA}/\text{cm}^2$  for  $\text{TiN}/\text{MnO}_2$  coaxial arrays [49], 105  $\text{mF}/\text{cm}^2$  at 0.06  $\text{mA}/\text{cm}^2$  for  $\text{WO}_{3-x}/\text{Au}/\text{MnO}_2$  nanowire [50] and comparable to that of hydrogenated  $\text{ZnO}/\text{MnO}_2/\text{Carbon cloth}$  (138.7  $\text{mF}/\text{cm}^2$  at 1  $\text{mA}/\text{cm}^2$ ) [51]. A high capacitance of 106 F/g (63  $\text{mF}/\text{cm}^2$ ) could be retained, even at a high sweep rate of 100 mV/s. Moreover, the GF/CNTs/ $\text{MnO}_2$  hybrid film displays good cycling performance with nearly overlapped CV curves after 5000 cycles.

Similar to GF/CNTs/ $\text{MnO}_2$  hybrid films, the current responses in the CV curves of GF/CNTs/Ppy hybrid films increase when more Ppy were deposited, resulting from the increased amount of active materials that contribute to the total capacitance (Fig. 4.5a, b). Typical CV curves deviate from an ideal rectangular shape, especially with high Ppy loading and at high sweep rates (Fig. 4.5c, d). Interestingly the difference in the areal capacitance for GF/CNTs/Ppy hybrid films is smaller particularly at high sweep rates (Fig. 4.5e), due to the reduced ion diffusion length and increased  $R_{\text{ct}}$ , as discussed for the case of GF/CNTs/ $\text{MnO}_2$  hybrid films. The EIS results of GF/CNTs/Ppy hybrid films (Fig. 4.5f) shows slight decrease initially, and followed with the increase in  $R_{\text{ct}}$  when Ppy loading increase gradually. The theoretic calculation indicates that the resistance of CNTs network usually comes from CNT/CNT junctions [52]. The slight decrease in  $R_{\text{ct}}$  is probably resulting from the uniform coating of Ppy onto the GF/CNTs film that improves the electric conductivity between CNT/CNT junctions [53]. However, further increasing the Ppy loading blocks the ion diffusion and migration process eventually, giving rise to the increase of  $R_{\text{ct}}$  from 10.7  $\Omega$  for GF/CNTs/Ppy-1000 to 28.6  $\Omega$  for GF/CNTs/Ppy-2000.



**Fig. 4.5** Comparative CV curves of GF/CNTs/Ppy hybrid films at sweep rates of **a** 5 mV/s and **b** 50 mV/s. CV curves of **c** GF/CNTs/Ppy-250 and **d** GF/CNTs/Ppy-1500 measured at different sweep rates. **e** The plot of Areal capacitance versus sweep rate and Nyquist plot (**f**) of GF/CNTs/Ppy hybrid films

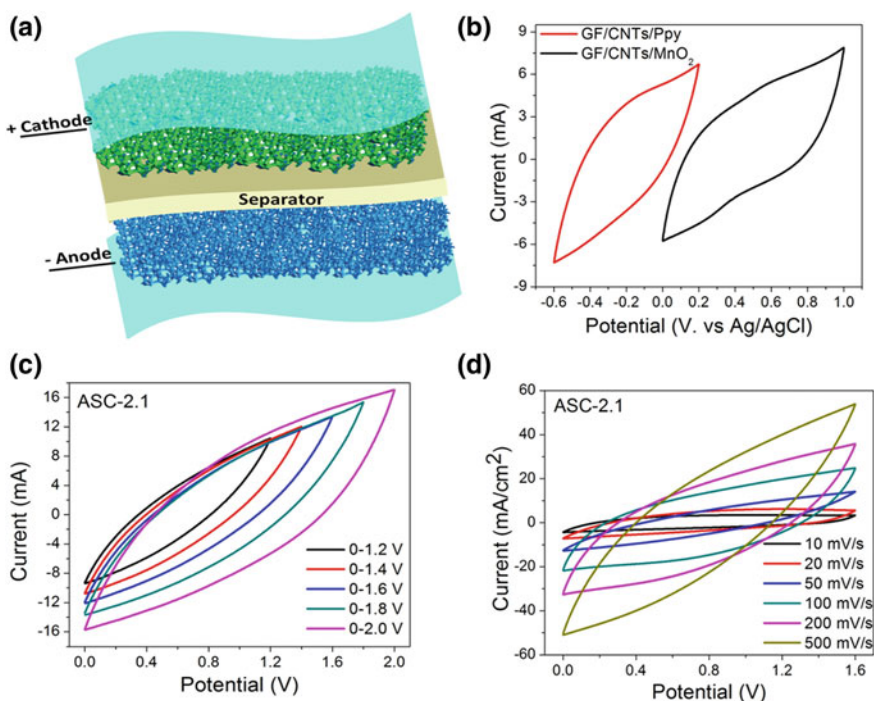
#### 4.3.4 Electrochemical Performance of GF/CNTs/MnO<sub>2</sub>//GF/CNTs/Ppy ASCs

The charge balance between positive electrode and negative electrode is crucial to maximize the energy density of ASCs [54]. Based on the results above, two couples of electrodes that exhibiting close total amount of charge in a wide range of sweep



rates, were chosen for the fabrication of ASC-0.6 and ASC-2.1, respectively. The weight ratio of positive electrode ( $\text{MnO}_2$ ) and negative electrode (Ppy) is 1.2:1 for ASC-0.6 and 1.3:1 for ASC-2, respectively.

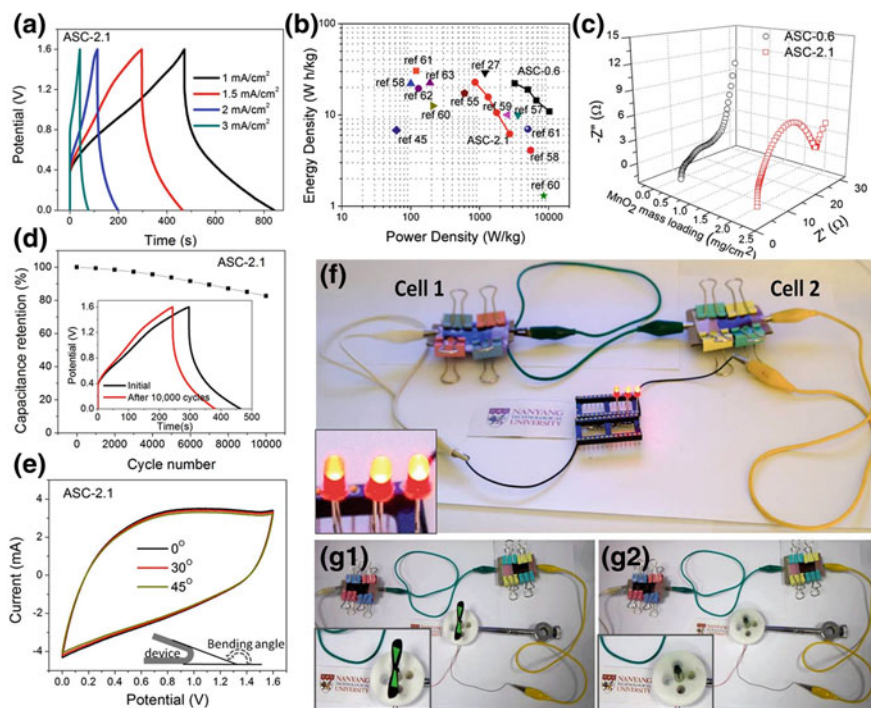
The ASC device, consisting of an electrolyte-soaked separator sandwiched by positive and negative electrodes, is illustrated schematically in Fig. 4.6a. Two pieces of poly(ethylene terephthalate) (PET) sheets were used as the flexible substrates. Considering the working window of GF/CNTs/ $\text{MnO}_2$  and GF/CNTs/Ppy hybrid films are 0–1.0 V and  $-0.6$ – $0.2$  V, respectively (Fig. 4.6b), the ASC device is expected to work stably over a voltage window of 0–1.6 V. Figure 4.6c illustrates the CV curves with different working windows. Note that the maximal voltage window of 1.6 V exceeds the theoretical decomposition voltage of water (1.23 V), resulting from the high overpotential of hydrogen evolution on the GF/CNTs/Ppy hybrid electrode. CV curves of ASC-2.1 were plotted in Fig. 4.6d. The assembled full cell exhibits quasi-rectangular CV curves at low sweep rates, agreeing with a



**Fig. 4.6** **a** Schematic illustration of an ASC that consists of GF/CNTs/ $\text{MnO}_2$  positive electrode, electrolyte-soaked separator and GF/CNTs/Ppy negative electrode. **b** CV curves of GF/CNTs/ $\text{MnO}_2$  and GF/CNTs/Ppy half cells in 0.5 M  $\text{Na}_2\text{SO}_4$  solution at a sweep rate of 20 mV/s. **c** CV curves of ASC-2.1 measured with different potential windows (at 50 mV/s). CV curves of ASC-2.1 **(d)** measured between 0 and 1.6 V with sweep rates ranging from 10 to 500 mV/s. Figure reproduced from Ref. [32]

good capacitive behavior [55]. The CV curves remain symmetrical even at a high sweep rate of 500 mV/s, corroborating the good reversibility of electrochemical processes.

Figure 4.7a illustrates the typical galvanostatic charge/discharge curves of the fabricated full cell. The charge-discharge curves deviate from the linear voltage-time relation, suggesting pseudo-capacitive behavior involved in the hybrid electrodes [56]. The ASC-2.1 exhibits a Coulombic efficiency of 74-85%, while the value for ASC-0.6 is above 95% at the current density of 1–3 mA/cm<sup>2</sup>. There are two possibilities that may contribute to the relatively low Coulombic efficiency: (i) ASC-2.1 exhibits large resistance with high mass loading; and ii) some unavoidable electrolysis of water take place because of the high working voltage. The Ragone plots of the ASCs, showing energy and power density of the devices, are shown in Fig. 4.7b. ASC-2.1 exhibits a maximum energy density of 22.8 Wh/kg at 860 W/kg and a high power density of 2.7 kW/kg at 6.2 Wh/kg. ASC-0.6 delivers better rate performance, with a maximum energy density of 22.2 Wh/kg at



**Fig. 4.7** **a** Galvanostatic charge/discharge curves of ASC-2.1 at different current densities. **b** Ragone plot of the ASCs and some other reported devices. **c** Nyquist plots for ASC-2.1 and ASC-0.6. **d** Cycling performance of ASC-2.1 at a current density of 1.5 mA/cm<sup>2</sup> for 10,000 cycles. Inset of **d** shows the charge/discharge curves for the 1st and 10,000th cycles. **e** CV curves of ASC-2.1 at different bending angles. Optical images show two ASCs connected in series powering **f** LEDs and **g** a small rotation motor. Figure reproduced from Ref. [32]

a power density of 3.2 kW/kg. Even at a high power density of 10.3 kW/kg, ASC-0.6 still displays an energy density of 10.9 Wh/kg. This is superior to that of many other  $\text{MnO}_2$ -based symmetric or asymmetric supercapacitors [45, 55, 57–63], as given in the same plot for comparison. The fast charge transport and lower resistance of ASC-0.6 may account for its superior rate performance over ASC-2.1, as revealed by the EIS results in Fig. 4.7c. In which, a typical diffusion-controlled Warburg capacitive behavior with a diagonal line in the low frequency region and small depressed semicircle in the high frequency region [43, 44], have been observed. The series resistance of the devices is estimated to be 17.7  $\Omega$  ( $R_s$ , 1.6  $\Omega$ ;  $R_{ct}$ , 16.1  $\Omega$ ) for ASC-0.6 and 26.4  $\Omega$  for ASC-2.1 ( $R_s$ , 6.4  $\Omega$ ;  $R_{ct}$ , 20.0  $\Omega$ ). The relatively small values of the serial resistances also corroborate the compact fabrication that ensures fast charge transfer in the cell. The overall volumetric and gravimetric energy and power densities were calculated based on the packaged cell configuration. The ASC-2.1 and ASC-0.6 deliver a maximum volumetric energy density of 8.7 and 2.7 Wh/L, respectively, based on the fully packaged cell. The value is quite satisfactory, and higher than reported  $\text{MnO}_2$ -based ASCs [63] and Ni(OH)<sub>2</sub>-based ASCs [64]. In addition, decent volumetric power densities of 1.2 kW/L for ASC-0.6 and 1.0 kW/L for ASC-2.1 have been delivered. The ASCs also display good cycling stability. Specially, high capacitance retentions of 90.2% for ASC-0.6 and 83.5% for ASC-2.1 (Fig. 4.7d) were reported, even after 10,000 charge/discharge cycles, which are comparable with or better than those of previously reported ASCs [65–67].

The development of multifunctional flexible electronics promotes increasing demands for power sources that are lightweight and flexible in addition to good electrochemical performance. To explore the practical application of our ASCs as flexible power source, the assembled cell was mechanically bended during the CV measurements (Fig. 4.7e). Under different bending angles, perfectly overlapped CV curves and similar specific capacitance are reported. This suggests that the device could be bent to a large extent without degrading the performance, benefiting from the flexible feature and good integrity of the hybrid electrodes. By connecting two pieces of packaged cells in series, output voltage window of 3.2 V was achieved. The ASC could power three red LEDs (1.8 V, 20 mA, 5 mm diameter) after charging for only 30 s (Fig. 4.7f) or even drive a small rotation motor (3 V, 0.45 W) with charging for only a few seconds (Fig. 4.7g).

### 4.3.5 Underlying Mechanism for Enhanced Electrochemical Performance

The performance of the ASCs designed in this work is quite satisfactory, especially considering the relatively high and tunable loading density of electroactive materials. The unique design of the 3D interconnected nanostructure of the flexible electrodes may account for the enhanced performance. Specifically, the densely grown CNTs extend the 3D architecture of GF to offer a large surface-to-volume



ratio that allows high active materials loading, and also provides good electric/mechanical contact within the hybrid films. Serving as current collector and mechanical supports, the GF/CNTs hybrid films ensures short diffusion length for ions, facile transfer pathways for electrons, and good integrity for active materials. Moreover, relative large mass fraction of electroactive materials is achieved, benefiting from the lightweight and highly porous feature of the GF/CNTs film and the additive-free design of the electrodes. Such electrodes would surely lead to a high energy density of real ASCs in practice, and show apparent advantages over those conventionally prepared with additives (e.g., carbon black and binder) and planar or 3D metallic current collectors. Additionally, the proper selection of positive/negative electrode materials as well as the well charge balance between the two electrodes also contribute to the good performance of ASCs [32].

## 4.4 Conclusion

In conclusion, novel GF/CNTs hybrid films with unique 3D architecture and large surface-to-volume ratio, and are flexible and lightweight were prepared. Using the hybrid films as electrode supports for the deposition of pseudo-capacitive materials, lightweight and flexible asymmetric supercapacitors (ASCs) have been fabricated. The good performance in terms of energy/power densities, cycling stability and flexibility have been demonstrated by the ASCs. This is attributed to the unique 3D nanostructure of the integrated electrodes, which allows high loading of electroactive materials and ensures facile charge transport. Such ASCs would be promising high-performance power source for flexible electronics.

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## Chapter 5

# Graphene Foam/Carbon Nanotubes Hybrid Film Based Flexible Alkaline Rechargeable Ni/Fe Battery

The proliferation of wearable and portable electronics requires high-performance power sources that are lightweight, ultrathin, flexible and low cost in addition to high performance features. Here, a new type of flexible Ni/Fe cell is designed and fabricated by employing  $\text{Ni}(\text{OH})_2$  nanosheets and porous  $\text{Fe}_2\text{O}_3$  nanorods grown on lightweight and flexible graphene foam (GF)/carbon nanotubes (CNTs) hybrid films as electrodes. The assembled f-Ni/Fe cells are able to deliver high energy/power densities (100.7 Wh/kg at 287 W/kg and 70.9 Wh/kg at 1.4 kW/kg) and outstanding cycling stability (retention 89.1% after 1000 charge/discharge cycles). Benefiting from the use of ultra-light and thin GF/CNTs hybrid films as current collectors, the f-Ni/Fe cell can exhibit a volumetric energy density of 16.6 Wh/l (based on the total volume of full cell). This value is comparable to that of thin film battery and better than that of typical commercial supercapacitors. Moreover, the f-Ni/Fe cells can retain the electrochemical performance with repeated bendings. These features endow f-Ni/Fe cells highly promising candidates for next generation flexible energy storage systems.

## 5.1 Introduction

The sharp proliferation of portable electronics and electrical vehicles requires high-performance power sources that process high energy density and power density and with lightweight, ultrathin, flexible, cost-effective and environmental friendly characteristics [1–3]. Among various energy storage devices, aqueous rechargeable batteries have attracted much attentions because of high ionic conductivity, environmental issues, good safety and low cost [4–7]. Many types of aqueous rechargeable batteries including aqueous alkali-ion ( $\text{Li}^+$ ,  $\text{Na}^+$ ,  $\text{K}^+$ ) batteries [8, 9], aqueous metal-ion batteries ( $\text{Al}^{3+}$ ,  $\text{Zn}^{2+}$ ) [10, 11] and aqueous nickel/metal (zinc, cadmium, cobalt and iron) batteries, have been explored [5, 6, 12, 13]. Different from the reversible intercalation/de-intercalation chemistry for aqueous alkali-ion

batteries and metal-ion batteries, the nickel/metal battery are mainly based on Faradaic reactions that involve one or multi-electron reactions on electrode materials [5]. Numerous electrochemical redox couples have been explored for alkaline rechargeable nickel/metal batteries, such as nickel/cadmium [6, 7], nickel/zinc [14], nickel/cobalt [5] and nickel/iron [12, 13]. Among these, aqueous Ni/Fe batteries are particularly favorable because (i) both Ni and Fe active materials are insoluble in alkaline solution, and has no requirement for the separator (in contrast with Ni/Zn and Ag/Zn batteries) [15, 16]; (ii) both Ni and Fe are earth-abundant elements and exhibit low toxic or corrosive effect [13, 15, 16]. Nickel-iron battery, which was invented in 1899–1902, has been well developed [15, 16]. More recently, the century-old nickel-iron battery was revisited and re-discovered to explore its potential application for modern energy supply systems. In contrast with traditional Ni/Fe batteries, hybrid materials based on novel inorganic nanoparticles (or rods) and carbon allotropes (carbon fibers [12], carbon nanotubes and graphene [13]) are now used as electrode materials, which indeed have improved the rate performance and energy density of Ni/Fe cells. Nevertheless, in the recent demonstrated high-performance Ni/Fe batteries [13], the active materials are in powder form and carbon black and binders are still required. These additives, together with the heavy Ni foam current collector, will lower the gravimetric specific capacity of the full cells. To push the performance particularly in flexible electronic devices, it is highly desirable to design novel electrode architecture that is binder-free, bendable and durable in long-term cycling.

In Chap. 4, graphene foam/carbon nanotubes (GF/CNTs) hybrid films were prepared and demonstrated to be excellent electrode supports due to their highly conductive, and large surface-to-volume ratio features [17]. They are ideal for depositing nanometer sized active materials without binders or carbon additives towards flexible and high-performance power sources. Herein, aqueous rechargeable Ni/Fe batteries are constructed by direct growth of  $\text{Ni}(\text{OH})_2$  nanosheets (cathode material) and mesoporous  $\text{Fe}_2\text{O}_3$  nanroods (anode material) on the GF/CNTs hybrid films. These novel flexible Ni/Fe cells deliver superior energy and power densities stemming from the nanosized feature of active materials and the hierarchical structure of the electrodes. Stable capacities on repeated bending and long-term (up to 1000) cycling are also demonstrated.

## 5.2 Experiment

### 5.2.1 Materials Synthesis

*Synthesis of Graphene Foam (GF)/Carbon nanotubes (CNTs) hybrid film.* The GF/CNTs hybrid films were synthesized via a modified recipe [18].

*Synthesis of GF/CNTs/ $\text{Ni}(\text{OH})_2$  hybrid film.*  $\text{Ni}(\text{OH})_2$  nanosheets were electrochemical deposited on GF/CNTs hybrid film directly in 0.1 M  $\text{Ni}(\text{NO}_3)_2$  aqueous

solution at a sweep rate of 100 mV/s with working windows at  $-1.2-0$  V (vs. SCE). The mass loading of  $\text{Ni}(\text{OH})_2$  was controlled via adjusting the number of cyclic voltammmetry from 50 to 200. The samples are denoted as GF/CNTs/ $\text{Ni}(\text{OH})_2$ -n, where n is the areal mass density of  $\text{Ni}(\text{OH})_2$  (unit of  $\text{mg}/\text{cm}^2$ ).

*Synthesis of GF/CNTs/ $\text{Fe}_2\text{O}_3$  hybrid film.* A simple hydrothermal method is used for the synthesis of GF/CNTs/ $\text{Fe}_2\text{O}_3$  hybrid film. Briefly, a piece of GF/CNTs film was immersed into a mixture solution of  $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$  (Merck AR, >99.0%) (monomer amount at 1.5, 3 and 6 mM), DI water (50 mL) and 15 mmol urea (AR, >99.0%), followed by the addition of 5 mL of 30% HCl. The mixture was then transferred into a Teflon-lined autoclave and heated at 150 °C for 15 h. The as-prepared precursor was washed with DI water and annealed at 550 °C for 1.5 h in Ar to obtain GF/CNTs/ $\text{Fe}_2\text{O}_3$  hybrid films. The samples are denoted as GF/CNTs/ $\text{Fe}_2\text{O}_3$ -n, where n is mass loading amount of  $\text{Fe}_2\text{O}_3$  ( $\text{mg}/\text{cm}^2$ ).

*Assemble of GF/CNTs/ $\text{Ni}(\text{OH})_2$ -GF/CNTs/ $\text{Fe}_2\text{O}_3$  rechargeable batteries (F-Ni/Fe batteries).* Flexible Ni/Fe batteries with high performance were assembled using a piece of GF/CNTs/ $\text{Ni}(\text{OH})_2$  ( $1 \times 4 \text{ cm}^2$ ) and a piece of GF/CNTs/ $\text{Fe}_2\text{O}_3$  ( $1 \times 4 \text{ cm}^2$ ), with an electrolyte-soaked (6 M KOH) separator in between.

## 5.2.2 Materials Characterization

*Structure and Morphology Characterization.* Field-emission Scanning Electron Microscopy (FESEM, JEM-6700F, 10.0 kV), Transmission Electron Mmicroscopy (TEM, JEM-2010, 200 kV), X-ray diffraction (XRD, Bruker D-8 Avance), X-ray photoelectron spectroscopy (XPS) on a VG ESCALAB 250 spectrometer (Thermo Electron, Altrincham, UK) [Al  $K\alpha$  X-ray source (1486 eV)] and the  $\text{N}_2$  adsorption/desorption [ASAP2020 volumetric adsorption analyzer (Micromeritics, USA)] were used to characterize the samples.

*Electrochemical Performance Evaluation.* Cyclic voltammmetry (CV) curves, Galvanostatic charge/discharge curves and electrochemical impedance spectroscopy (EIS, 100 kHz–0.01 Hz) were collected using CHI 760D workstation. The three-electrode system is chosen for individual electrode testing.

*Calculations.* The specific capacity ( $C^*$ , mAh/g) of positive or negative electrode in **three-electrode** configuration are calculated according to the equation:

$$C^* = \frac{I}{m} \Delta t$$

where I is the discharging current, m is the mass of the individual electrodes,  $\Delta t$  is the discharge time.



The specific capacity ( $C^*$ , mAh/g) of f-Ni/Fe cells in **two-electrode** configuration are calculated according to the equation:

$$C^* = \frac{I}{M} \Delta t$$

where  $I$  is the discharging current,  $M$  is the total mass of the two electrodes,  $\Delta t$  is the discharge time.

The equation:  $C_- V_- = C_+ V_+$ , is used for the charge match between two electrodes. The energy density ( $E$ ) and power density ( $P$ ) are calculated according to the equations below:

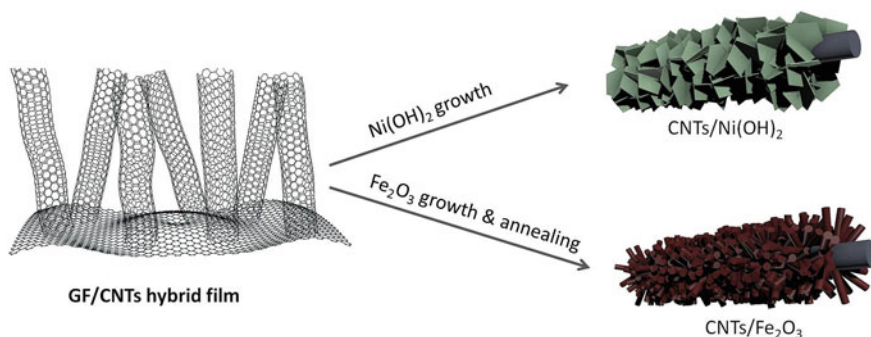
$$E = \int IV dt/dm$$

$$P = E/\Delta t$$

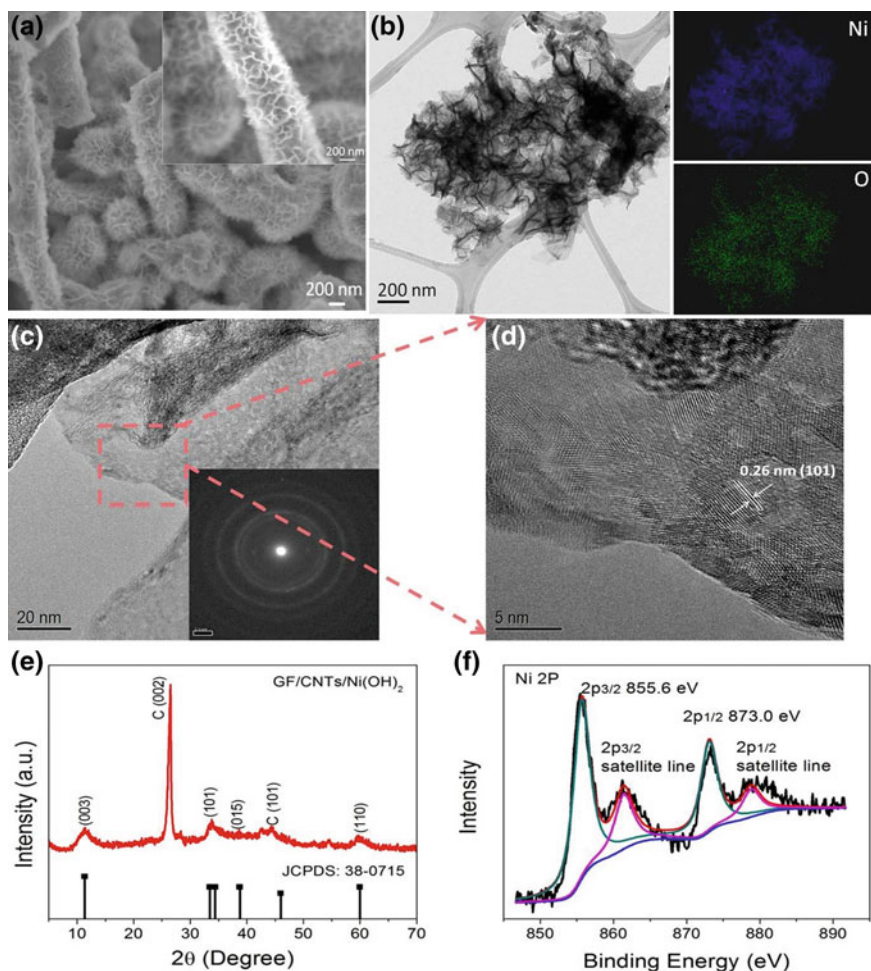
### 5.3 Results and Discussions

#### 5.3.1 The Synthesis of GF/CNTs/Ni(OH)<sub>2</sub> and GF/CNTs/Fe<sub>2</sub>O<sub>3</sub>

In situ electrochemical deposition method was employed for the synthesis of GF/CNTs/Ni(OH)<sub>2</sub> hybrid electrodes. This method is advantageous due to: (i) it can produces thin nanosheet structure of Ni(OH)<sub>2</sub> active material; and (ii) it also allows a fine tuning of mass loading of Ni(OH)<sub>2</sub> via modulating the concentrations of electrolyte and deposition time (Fig. 5.1) [19, 20]. The flower-like Ni(OH)<sub>2</sub> nano-sheets surround the CNTs uniformly with outer diameters ranging from 150 to 300 nm (depending on the mass loading amount) (Fig. 5.2a). The mass loading



**Fig. 5.1** Schematic illustration of the synthesis of GF/CNTs-based electrodes. Figure reproduced from Ref. [41]

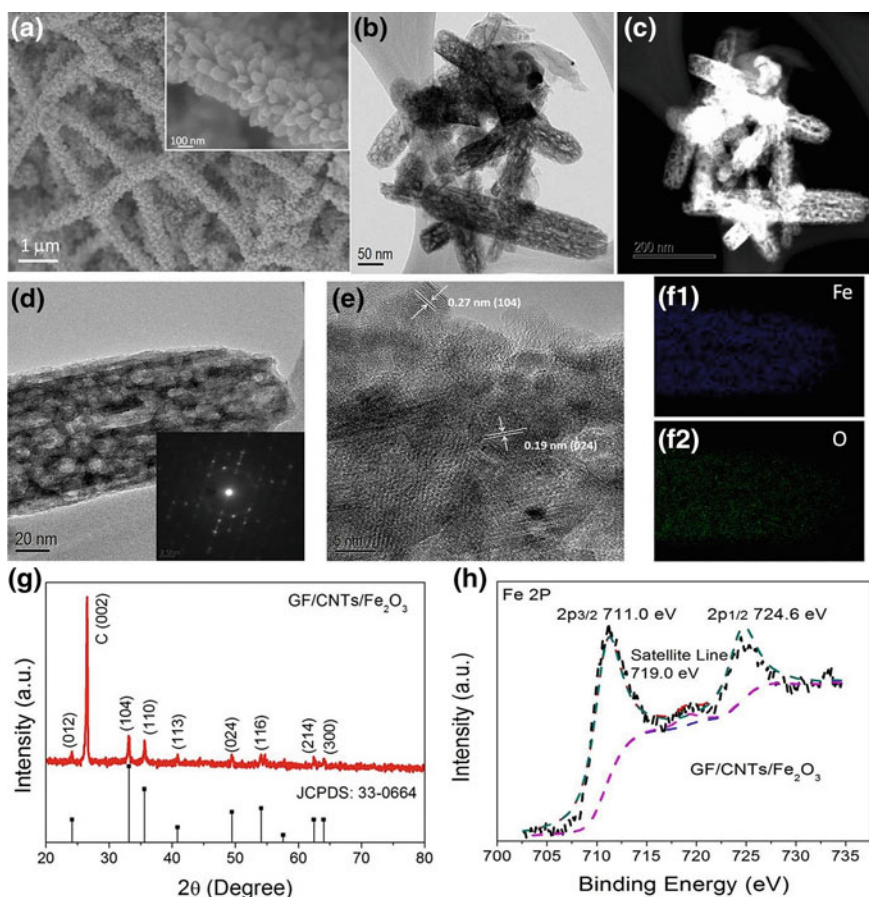


**Fig. 5.2** Characterization of the GF/CNTs/Ni(OH)<sub>2</sub> hybrid film. **a** Typical FESEM image (inset is magnified SEM image) and **b** Low-magnification TEM image of the hybrid film and corresponding element mappings of Ni and O. **c** TEM image (inset is selected area electron diffraction (SAED) pattern) and correspond HRTEM image (**d**). **e** XRD pattern and **f** XPS spectra

density of Ni(OH)<sub>2</sub> is adjustable and well-controlled. More details about the nano-sheet feature of Ni(OH)<sub>2</sub> can be found in TEM images (Fig. 5.2b, c). The element mapping images verify the uniform distribution of O and Ni (Fig. 5.2b). The well-defined SAED pattern (inset in Fig. 5.2c) corroborates that the Ni(OH)<sub>2</sub> nano-sheets are polycrystalline. Well-resolved lattice fringes of 0.26 nm was observed (Fig. 5.2d), corresponding to the (101) plane of  $\alpha$ -Ni(OH)<sub>2</sub> (JCPDS #38-0715). X-ray diffraction (XRD) results further confirm the formation of rhombohedral  $\alpha$ -Ni(OH)<sub>2</sub>. All the peaks could be indexed to rhombohedral  $\alpha$ -Ni(OH)<sub>2</sub> except the crystalline peaks at 26.4° and 44.3° that result from GF/CNTs

substrate (Fig. 5.2e). X-ray photoelectron spectroscopy (XPS) analysis was conducted to shed more light on composition and oxidation stage of  $\text{Ni}(\text{OH})_2$ . Two typical peaks centered at 855.6 and 873.0 eV were observed (Fig. 5.2f), corresponding to  $\text{Ni } 2p_{3/2}$  and  $\text{Ni } 2p_{1/2}$  of  $\text{Ni}(\text{OH})_2$ , respectively [21]. Meanwhile, two satellite lines associated with  $\text{Ni } 2p$  are also identified.

GF/CNTs/ $\text{Fe}_2\text{O}_3$  hybrid electrodes were prepared via a facile hydrothermal reaction of  $\text{FeOOH}$  nanorods followed by thermal annealing (Fig. 5.1). Representative SEM images (Fig. 5.3a) reveal the well-defined interconnected network structure of GF/CNTs/ $\text{Fe}_2\text{O}_3$ , in which the columnar  $\text{Fe}_2\text{O}_3$  nanorods coated around CNTs uniformly with outer diameter ranging from 200 to 300 nm.

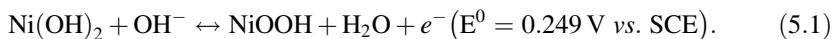


**Fig. 5.3** Characterization of the GF/CNTs/ $\text{Fe}_2\text{O}_3$  hybrid film. **a** Typical FESEM image (inset is magnified SEM image) and **b** Low-magnification bright-field TEM image and **c** dark field TEM image of the hybrid film. **d** TEM image (inset is selected area electron diffraction (SAED) pattern), corresponding HRTEM image (**e**), and **f1–f2** corresponding element mappings of Fe and O. **g** XRD pattern and **h** XPS spectrum

TEM images (Fig. 5.3b, c) clearly identify the mesoporous nanorod structure of  $\text{Fe}_2\text{O}_3$  with diameter in the range of 50–150 nm and length ranging from 50 to 500 nm. This feature was further verified by the magnified TEM image in Fig. 5.3d, where the pore size is around 5–10 nm. The specific surface area of the GF/CNTs/ $\text{Fe}_2\text{O}_3$  hybrid film is around  $68 \text{ m}^2/\text{g}$ . This value is comparable with rGO/ $\text{Fe}_2\text{O}_3$  composites [22] and higher than that of mesoporous  $\text{Fe}_2\text{O}_3$  [23]. The good crystallinity nature of  $\text{Fe}_2\text{O}_3$  nanorods is manifested by the clear SAED pattern (inset of Fig. 5.3d). The well-defined lattice fringes with distances of 0.19 and 0.27 nm (Figs. 5.3e) correspond to the d-spacing of (024) and (104) planes, respectively. The homogeneous distribution of both Fe and O corroborates the uniform coating of  $\text{Fe}_2\text{O}_3$  (Fig. 5.3f1, f2). The characteristic peaks in XRD can be well indexed as tetragonal  $\alpha\text{-Fe}_2\text{O}_3$  (JCPDS 33-0664) [24]. XPS result (Fig. 5.3h) exhibits typical Fe 2p spectrum of  $\text{Fe}_2\text{O}_3$  with two peaks centered at 711.0 and 724.6 eV, corresponding to Fe 2p<sub>3/2</sub> and Fe 2p<sub>1/2</sub>, respectively [25]. The presence of satellite line of the main Fe 2p<sub>3/2</sub> located at 719.0 eV further verifies the  $\text{Fe}_2\text{O}_3$  phase rather than  $\text{Fe}_3\text{O}_4$ .

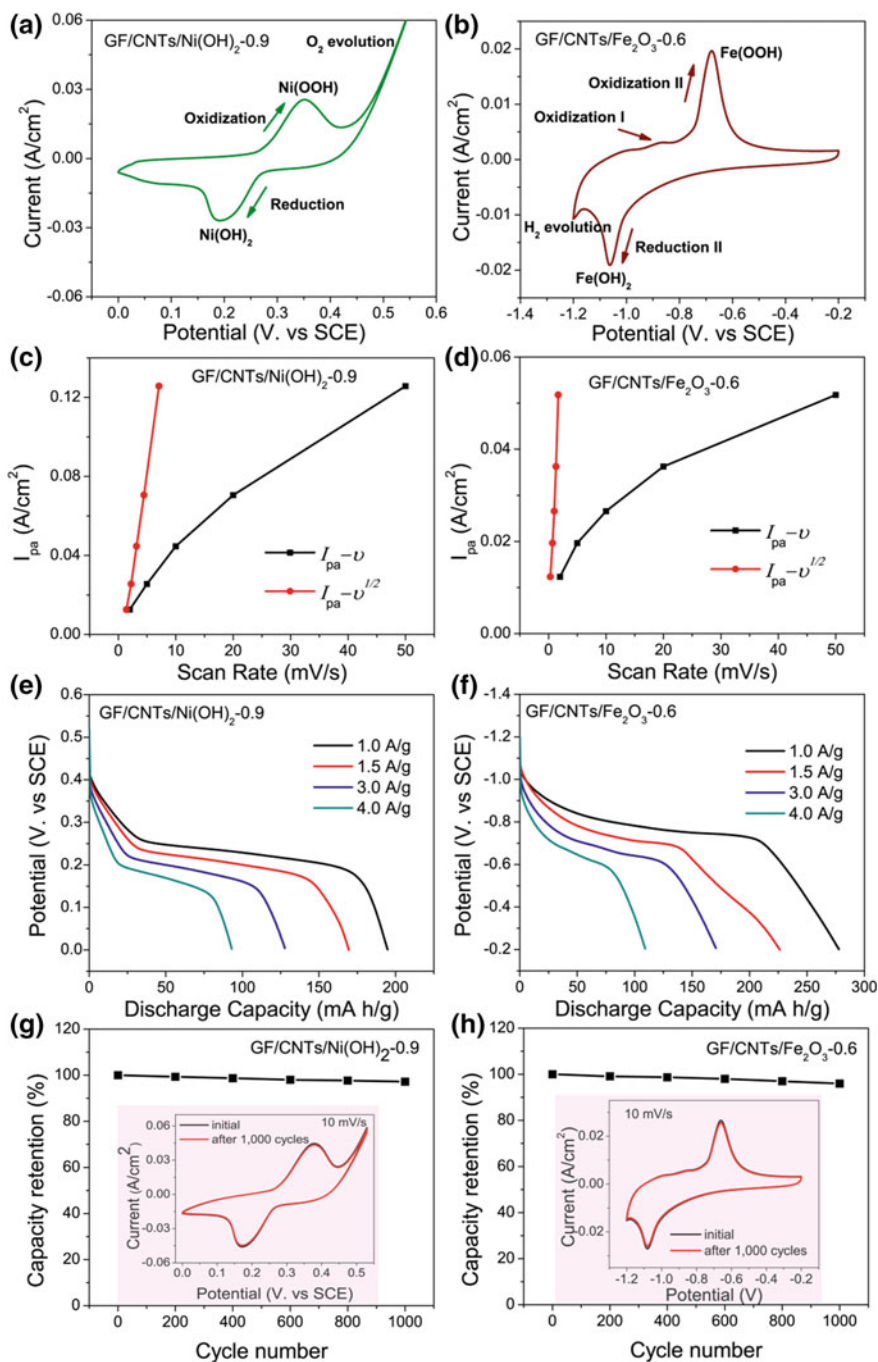
### 5.3.2 Electrochemical Performance of GF/CNTs/ $\text{Ni}(\text{OH})_2$ and GF/CNTs/ $\text{Fe}_2\text{O}_3$

The electrochemical properties of both GF/CNTs/ $\text{Ni}(\text{OH})_2$  cathode and GF/CNTs/ $\text{Fe}_2\text{O}_3$  anode were investigated in a three-electrode configuration containing 6 M KOH solution. Hereby, our discussion start with the charge-matching electrodes, viz., GF/CNTs/ $\text{Ni}(\text{OH})_2$ -0.9 cathode and GF/CNTs/ $\text{Fe}_2\text{O}_3$ -0.6 anode (0.9 and 0.6 denote the areal mass densities of the corresponding active materials in unit of  $\text{mg}/\text{cm}^2$ ). Typical cyclic voltammetry (CV) curves of GF/CNTs/ $\text{Ni}(\text{OH})_2$ -0.9 and GF/CNTs/ $\text{Fe}_2\text{O}_3$ -0.6 are shown in Figs. 5.4a, b. Well-defined redox peaks locating at 0.36 (anodic)/0.21 V(cathodic) (vs. SCE) are identified in typical cyclic voltammetry (CV) curves of GF/CNTs/ $\text{Ni}(\text{OH})_2$ -0.9 (Fig. 5.4a). This corresponds to the reversible reaction as follows [7, 12, 26]:



Two oxidization peaks around  $-0.89$  and  $-0.71$  V in the anodic scan are observed for the GF/CNTs/ $\text{Fe}_2\text{O}_3$  electrode (Fig. 5.4b). They are attributed to the formation of  $\text{Fe}(\text{OH})_2$  (with the oxidization from  $\text{Fe}^0$  to  $\text{Fe}^{2+}$ ) and  $\text{FeOOH}$  (with the oxidization from  $\text{Fe}^{2+}$  to  $\text{Fe}^{3+}$ ), respectively. One well-defined reduction peak at around 1.05 V is found in the cathodic curve, which is assigned to the reduction from  $\text{Fe}^{3+}$  to  $\text{Fe}^{2+}$ . Another cathodic peak (corresponding to the reduction of  $\text{Fe}^{2+}$  to  $\text{Fe}^0$ ) is missed, probably due to the distortion caused by the  $\text{H}_2$  evolution.

The redox peaks are found to be sweep rate dependent with the peak position separation,  $\Delta E_{a,c}$ , increases with increasing sweep rate [27, 28]. The increase in the

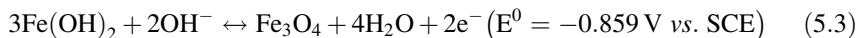
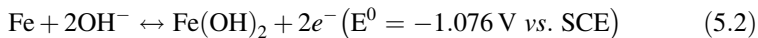




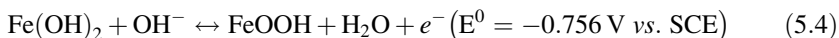
◀**Fig. 5.4** Electrochemical characterizations of the hybrid film electrodes. *Left column* GF/CNTs/Ni(OH)<sub>2</sub>-0.9 cathode. *Right column* GF/CNTs/Fe<sub>2</sub>O<sub>3</sub>-0.6 anode. **a, b** Cyclic voltammetry curves at a sweep rate of 5 mV/s. **c, d** Variation of anodic peak current ( $I_{pa}$ ) with sweep rate. **e, f** Galvanostatic discharge curves at various current densities. **g, h** Cycling performance. Insets are the corresponding CV curves after 1000 cycles. Figure reproduced from Ref. [41]

charge diffusion polarization within the pseudoactive material upon the increase of sweep rate accounts for this [29]. The peak current ( $I_{pa}$ ) is plotted as a function of sweep rate ( $v$ ) and  $v^{1/2}$  to gain insight into the kinetic information of the involved redox reactions (Figs. 5.4c, d). The linear  $I_{pa}$  versus  $v^{1/2}$  plots have been derived. On the other hand, the  $I_{pa}$  versus  $v$  plots display a non-linear behavior. Generally,  $I_{pa}$  versus  $v^{1/2}$  plot shows linear relationship regardless of the sweep rate for a kinetically uncomplicated redox reaction in semi-infinite diffusion controlled CV, and the  $I_{pa}$  versus  $v$  plots is expected to be linear for an adsorption process [30–35]. Therefore, the oxidation processes involved here are diffusion limited, agreeing well with previous reported results about LiFePO<sub>4</sub> [33].

Figures 5.4e, f illustrate the typical discharge curves of Ni(OH)<sub>2</sub> electrode and Fe<sub>2</sub>O<sub>3</sub>, respectively, upon various discharge current densities. A well-defined plateau at around 0.25 V was observed for Ni(OH)<sub>2</sub> electrode, consisting well with Eq. (5.1). The oxidation reactions of iron anode in alkaline electrolytes could be described as [7, 15, 36–39]:



or/and



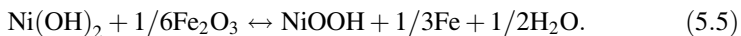
The well-defined plateau around -0.77 V (vs. SCE) can be assigned to the reaction (5.4). The plateau corresponding to reaction (5.2) is not evident in either CV or discharge curves, which suggests that the anodic process is dominated by reaction (5.4). Possibly reaction (5.2) takes place synchronously with the hydrogen evolution during the cathodic scan when the H<sub>2</sub> evolution occurs at a more positive potential.

The gravimetric capacitance of GF/CNTs/Ni(OH)<sub>2</sub> electrode (Fig. 5.4e) and GF/CNTs/Fe<sub>2</sub>O<sub>3</sub> electrode (Fig. 5.4f) were calculated from the corresponding galvanostatic discharge curves. The GF/CNTs/Ni(OH)<sub>2</sub>-0.9 and GF/CNTs/Fe<sub>2</sub>O<sub>3</sub>-0.6 deliver a gravimetric capacity of 195 and 278 mAh/g, respectively, at 1 A/g. The gravimetric capacities retain at 93 and 109 mAh/g, respectively, even at a high sweep rate of 4 A/g. These results imply good rate capabilities for both hybrid electrodes. Moreover, good cycle stability with capacity retention at 97.2% for GF/CNTs/Ni(OH)<sub>2</sub>-0.9 (Fig. 5.4g) and 96% for GF/CNTs/Fe<sub>2</sub>O<sub>3</sub>-0.6 (Fig. 5.4h) after 1000 cycles have been demonstrated.

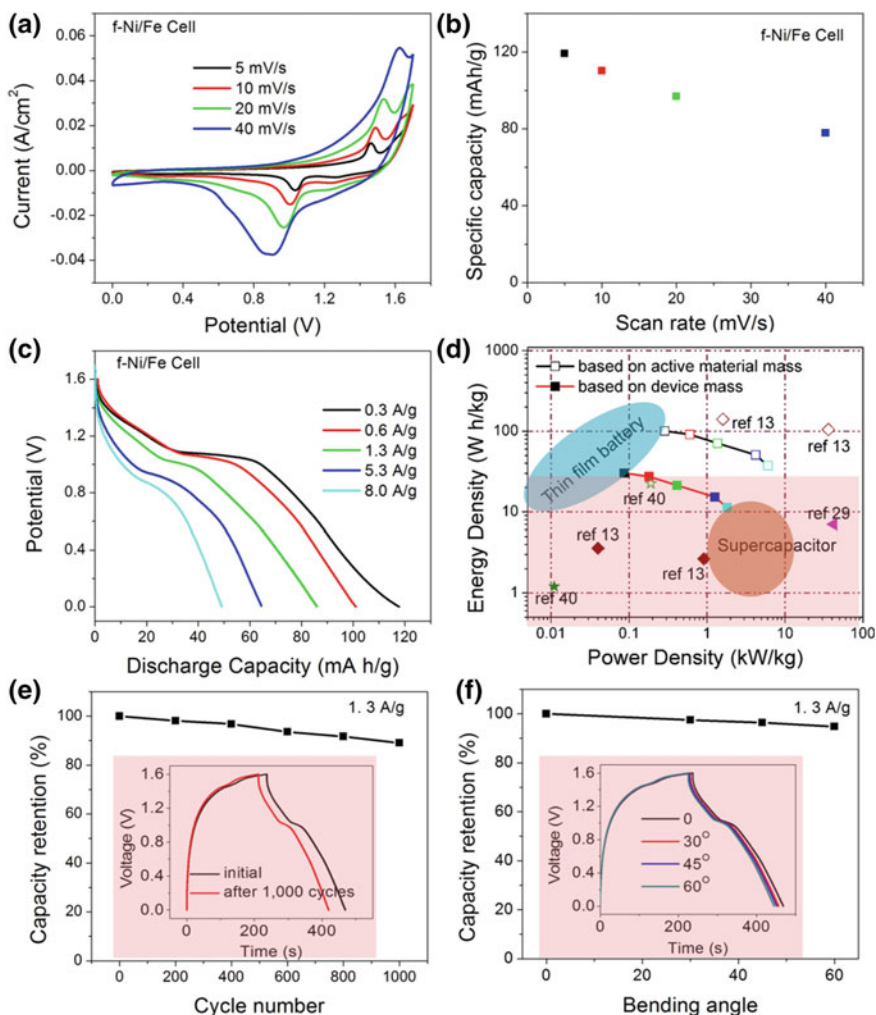
The electrochemical performance of hybrid electrodes is strongly affected by mass loading of active materials. Specifically, the gravimetric capacity and rate performance degrade with the increase in active materials loading, although the corresponding current response increases. The decrease in electric conductivity related to the increase in the active materials coating thickness takes responsibility for this. For example, the equivalent series resistance (ESR) increases from 2.9  $\Omega$  for GF/CNTs/Ni(OH)<sub>2</sub>-0.5 to 4.6  $\Omega$  for GF/CNTs/Ni(OH)<sub>2</sub>-1.2. Similar trend was also noted for GF/CNTs/Fe<sub>2</sub>O<sub>3</sub> electrodes with different mass loading. The dependence of electrochemical property on mass loading of active materials demonstrates the importance of electrode design to achieve optimized performance of full cells.

### 5.3.3 Electrochemical Performance of F-Ni/Fe Battery

Based on the results above, Ni/Fe full cells were fabricated by using GF/CNTs/Ni(OH)<sub>2</sub>-0.9 hybrid film as cathode and GF/CNTs/Fe<sub>2</sub>O<sub>3</sub>-0.6 as anode. These two electrodes were chosen because a good charge match has been achieved. The sweep rate dependent CV curves of the f-Ni/Fe are illustrated in Fig. 5.5a. Well-defined redox couples were observed, originating from the overall reaction in the Ni/Fe cell [12],



Similar to the individual electrode, the f-Ni/Fe cell exhibits an increase in the anodic peak and cathodic peak separation ( $\Delta E_{a,c}$ ) with increasing sweep rate. The  $I_{pa}$  versus  $v^{1/2}$  plot of f-Ni/Fe cell is also linear, indicating that a diffusion limited oxidization reaction takes place during the charging process [30–33]. The f-Ni/Fe cell delivers high specific capacity of 119 mAh/g at sweep rate of 5 mV/s and 78 mAh/g at sweep rate of 40 mV/s (Fig. 5.5b), implying its good rate capability. Typical galvanostatic discharge curves at different current densities are shown in Fig. 5.5c. Consistent to the CV curves, the discharge profiles exhibit good reversibility with distinct discharge voltage plateau from 0.9 to 1.1 V (depending on current density), demonstrating its application feasibility for energy storage [12, 13, 38]. The specific capacity decreases from 118 to 50 mAh/g when the current density increase from 0.3 to 8 A/g. The discharge process (Fig. 5.5c) completes in short times ranging from 20 min to 30 s, depending on the current density. These discharge time are much shorter than conventional Ni/Fe batteries that usually require hours. These values also outperform the Ni/Fe cell based on carbon fibers [12] with a specific capacity of 80 mAh/g and charge/discharge time of hours. The series resistance of the device is estimated to be 5.9  $\Omega$  ( $R_s = 3.8 \Omega$ ;  $R_{ct} = 2.1 \Omega$ ) from the EIS data. The relatively small serial resistances of the f-Ni/Fe cell ensure a fast charge transfer between the electrolyte and electrodes.



**Fig. 5.5** Performance of the flexible Ni/Fe full cells. Cyclic Voltammetry curves (a) and corresponding gravimetric capacity (b) at different sweep rates. c Galvanostatic discharge curves at various current densities and d The Ragone plot. Comparisons are made in two ways: based on the active material mass only (upper half), and based on the whole device mass (bottom shaded half). e Cycling performance of the f-Ni/Fe cell at a current density of 1.3  $\text{A}/\text{g}$  for 1000 cycles. Inset shows the charge/discharge curves for the 1st and 1000th cycles. f Cycling performance of f-Ni/Fe cell at different bending angles. Inset shows the charge/discharge curves at different bending angles. Figure reproduced from Ref. [41]

The Ragone plots, showing energy density and power density, are plotted in two ways, viz., one based on the active material mass only (open symbols); and the other based on the whole device mass (solid symbols) (Fig. 5.5d). The f-Ni/Fe cell delivers an energy density of 100.7  $\text{Wh}/\text{kg}$  at 287  $\text{W}/\text{kg}$  and 70.9  $\text{Wh}/\text{kg}$  at



1.4 kW/kg, respectively, based on the total mass of active materials. Even at a high power density of 6.0 kW/kg, an energy density of 37.4 Wh/kg can still be achieved. Considering the total mass of the cell, a gravimetric energy density of 30.3 Wh/kg is achieved, benefiting from the lightweight nature of GF/CNTs hybrid films current collector. This value is three folds that of typical commercial supercapacitors, and higher than that of Ni/Fe cells using nickel foams as the current collector [13]. The maximum power density of 1.8 kW/kg is comparable to that of commercial supercapacitor, and four-folds higher than that of lithium thin film battery.

In order to push the practical applications of the f-Ni/Fe cell, the volumetric energy/power densities based on the whole cell configuration were also calculated (Table 5.1). A maximum volumetric energy density of 16.6 Wh/l has been achieved, which is two-folds higher than the reported MnO<sub>2</sub>-based [40] and Ni(OH)<sub>2</sub>-based asymmetric supercapacitors [29], both are typical high-capacity supercapacitive materials. The maximum volumetric power density is 1.0 kW/l. Moreover, the f-Ni/Fe cell exhibits good cycling stability with capacity retention of 89.1% after 1000 charge/discharge cycles (Fig. 5.5e). This result is better than the recently reported Ni/Fe cells which showed 80% capacity retention after 800 cycles [13]. Moreover, the capacity could retain at 78% when the stability test extended further to 2000 cycles. And the CNTs-supported structures were well maintained although the surfaces of electrodes show some degree of aggregations during the long charge/discharge process.

The development of multifunctional flexible electronics requires power sources that are flexible and lightweight in addition to high performance. For practical

**Table 5.1** Parameters for the flexible Ni/Fe cell (f-Ni/Fe Cell) and the calculated gravimetric and volumetric energy/power densities based on the fully packaged cell

		Thickness ( $\mu\text{m}$ )	Density ( $\text{g}/\text{cm}^3$ )	Weight percentage (%)	Volume percentage (%)
Ni/Fe cell	Positive electrode (GF/CNTs/Ni (OH) <sub>2</sub> -0.9)	31	0.50	31.1	34.5
	Negative electrode (GF/CNTs/Fe <sub>2</sub> O <sub>3</sub> -0.6)	30	0.42	25.1	33.3
	Separator	29	0.39	22.6	32.2
	Electrolyte (6 M KOH)	–	1.23	21.2	–
		$E_{\text{max}}$ (Wh/kg)	$P_{\text{max}}$ (kW/kg)	$E_{\text{max}}$ (Wh/L)	$P_{\text{max}}$ (kW/L)
Ni/Fe cell	Active materials (Ni(OH) <sub>2</sub> + Fe <sub>2</sub> O <sub>3</sub> )	100.7	6.0	–	–
	Electrodes (including GF/CNTs films)	53.9	3.2	24.7	1.5
	Full cell	30.3	1.8	16.6	1.0

**Remarks** The electrolyte is absorbed by the electrodes and thus does not take up any volume in the packaged cell. For f-Ni/Fe Cell: total cell mass is 20.0 mg; total volume is 36.4  $\mu\text{L}$ ; density of packaged cell is 0.55  $\text{g}/\text{cm}^3$

application consideration, the f-Ni/Fe cells were mechanically bended during the charge/discharge measurements (Fig. 5.5f). Negligible changes in the charge/discharge curves under different bending angles (up to 60°) were identified, corroborating the good flexible feature of the f-Ni/Fe cell. The practical application of our f-Ni/Fe cell was further demonstrated by driving a fan or light-emitting diodes (LEDs) using two f-Ni/Fe cells connected in series. Benefiting from the high power/energy density, the f-Ni/Fe cell could power one red LED (1.8 V, 20 mA, 5 mm diameter) and one yellow LED (1.8 V, 30 mA, 5 mm diameter) simultaneously after charging for only 30 s, or drive a small rotation motor (3 V, 0.45 W) after charging for only a few seconds.

#### **5.3.4 Underlying Mechanism for Enhanced Electrochemical Performance**

The high performance Ni/Fe cells demonstrated here bridge the gap between conventional thin film Li-ion batteries and supercapacitors for flexible electronics. The nanostructured active materials are grown directly surrounding the highly-conductive CNTs. This feature contributed the following advantages: (1) It assures a favorable electric contact and facilitates the electron transportation. (2) It promotes good mechanical integrity, accounting for the high cycling stability and flexibility. (3) The lightweight and highly porous features of the GF/CNTs substrate significantly increases the mass loading of active materials as compared to direct growth onto the GF or a planar metallic current collectors [41]. This also eliminates the additives (e.g., carbon black and binder). Benefiting from the unique hierarchical design, the gravimetric energy density and volumetric energy density of the f-Ni/Fe cells are comparable to thin film lithium ion battery and better than typical commercial supercapacitors.

### **5.4 Conclusion**

In conclusion, flexible Ni/Fe cells are designed and fabricated successfully based on lightweight and flexible GF/CNTs current collectors without using any binders or carbon additives. The high volumetric energy/power densities, good cycling stability and flexibility of the f-Ni/Fe cell are clearly demonstrated. Such high-performance alkaline batteries could bridge the energy density gap between supercapacitor and thin film lithium ion battery, and be promising candidate for next generation flexible energy storage systems. The design we proposed is scalable for mass production and could be extended to the fabrication of other binder-free and flexible Ni/Metal alkaline batteries.

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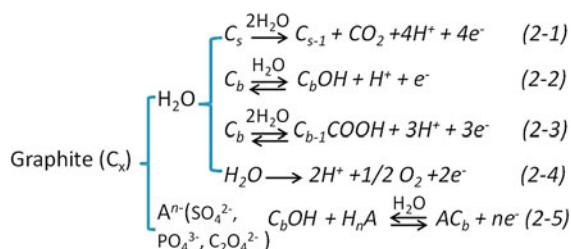
# Chapter 6

## Conclusions, Comments and Future Work

### 6.1 Conclusions

The synthesis and characterization of low-dimensional carbon materials, including graphene oxide/graphene, graphene foam (GF), GF/carbon nanotubes (CNTs) hybrids, and their composites with nanostructured metal oxides are conducted in this thesis. Their applications in energy storage devices, including lithium-ion battery, aqueous asymmetric supercapacitors and aqueous Ni/Fe battery, are explored.

- (1) **Electrochemical Exfoliation of Graphite.** High-quality graphene flakes is synthesized via a facile electrochemical exfoliation method. The underlying mechanism is discussed in detail. Specifically, electrochemical oxidation reactions triggered by the current flow which removes the electrons from anode may take place, including the anodic oxidation (Eq. 2.1), hydroxylation (Eq. 2.2) and carboxylation (Eq. 2.3) of graphite (as well as water oxidation, Eq. 2.4).



These processes occur initially at surface, grain boundary or structural defect sites, generating  $\cdot\text{OH}$ ,  $\cdot\text{COC}$ ,  $\text{CO}\cdot$ , and  $\text{COO}\cdot$  functional groups on the graphite surface.  $\text{CO}_2$  and  $\text{O}_2$  can be produced as the electrolysis products (Eqs. 2.1 and 2.4). Simultaneously, the release of gaseous bubbles was obviously observed during the electrochemical process, and became vigorous with increasing

exfoliation time, as if water boiled. The anodic corrosion/etching as well as the violent gas release open up the edge sheets on the graphite rod surface and facilitates the intercalation of bulky anions (as well as their solvated moieties) into the graphite layers, forming graphite-intercalation-compounds (GIC) ( $C + A^- \rightarrow CA + e^-$ ) (Eq. 2.5). The intercalation and the hydrolysis of the intercalated complex ( $CA + H_2O \rightarrow COH + H^+ + e^-$ ) lead to the expansion of graphene sheets and the cleavage/exfoliation of functional graphene sheets.

Various aqueous protonic acids with bulky anions including phosphoric acid, sulfuric acid, oxalic acid, were all proven to be effective during exfoliation process. The diverse choices of aqueous electrolyte provide us with more freedom to adjust the oxidization states of exfoliated graphene and reduce the production cost even further. Our present findings provide deep understanding of the underlying mechanism for electrochemical exfoliation of graphite, effective guides for optimized/controlled synthesis of graphene, and promising approaches for graphene commercialization in future.

- (2) ***Design High-Performance GF/Fe<sub>3</sub>O<sub>4</sub> composite Anode for Lithium-ion Battery.*** GF/Fe<sub>3</sub>O<sub>4</sub> hybrid electrodes have been prepared via atomic layer deposition approach. The formed GF/Fe<sub>3</sub>O<sub>4</sub> composite exhibits several characteristics: (i) the good electric conductivity and mechanical properties of GF provide efficient ion/electron transportation and mechanical integrity; (ii) the bi-continuous nanostructure Fe<sub>3</sub>O<sub>4</sub> formed by interconnected nanocrystallites are homogeneously distributed on the graphene foam surface with an intact physical contact. The direct contact and interconnection ensure an efficient lithium ion and electron transport between Fe<sub>3</sub>O<sub>4</sub> and graphene, as well as ion transport between the electrolyte and the active material. (iii) the binder and conducting agent-free design, as well as atomic layer deposition approach allow a high active material (Fe<sub>3</sub>O<sub>4</sub>) loading without sacrificing the flexibility of GF/Fe<sub>3</sub>O<sub>4</sub> electrodes. Benefiting from the rational design and the unique mesoscale structure, the GF/Fe<sub>3</sub>O<sub>4</sub> electrodes display remarkable rate and cycle performance. Our results provide efficient guides for optimized design of flexible electrodes.
- (3) ***Design High-Performance Asymmetric Supercapacitors based on GF/CNTs Hybrid Films.*** A novel electrode support (GF/CNTs) consisting of carbon nanotubes supported on graphene foam (GF) with covalent bonding has been prepared. The densely grown CNTs extend the 3D architecture of GF without sacrificing the good ohmic and mechanical contact between them, and provide a high surface-to-volume ratio that allows high active materials loading. The GF/CNTs hybrid films show several critical merits, including: (i) good electric conductivity; (ii) large specific surface area; (iii) high active materials mass loading, which could be 4–5 folds higher than pure GF (3–8 mg/cm<sup>2</sup>); (iv) Ultrathin and Lightweight with thickness range from 30 to 100 μm; (v) large size, good flexibility and mechanical integrity; and (vi) excellent

electrochemical stability. These features successfully overcome limitation of the insufficient surface area of these graphene/CNTs hybrid films prepared from traditional dip-coating or beam evaporation, and provide GF/CNTs hybrid film with great potential for applications in next-generation flexible energy storage devices. The assembled asymmetric supercapacitors (ASCs) (GF/CNTs/MnO<sub>2</sub>//GF/CNTs/Ppy) based on GF/CNTs electrode scaffolds display high energy/power density and are capable of repeated bending without structure failure and degradation in performance. These results presented here would no doubt provide a promising approach for flexible electrode design in future.

(4) ***Design High-Performance Ni/Fe Battery based on GF/CNTs Hybrid Films.***

In addition to the development of novel electrode scaffold (Chap. 4), it is equally important to explore the promising applications of traditional energy storage devices in modern energy supply systems. Along this line, the century-old Ni/Fe battery was revisited and re-discovered in this work. By employing Ni(OH)<sub>2</sub> nanosheets and porous Fe<sub>2</sub>O<sub>3</sub> nanorods grown on light-weight and flexible graphene foam (GF)/carbon nanotubes (CNTs) hybrid films as electrodes, we designed and fabricated a new type of flexible Ni/Fe cell. The assembled f-Ni/Fe cells deliver good electrochemical performance, benefiting from the unique electrode design. Moreover, the f-Ni/Fe cells can retain the electrochemical performance with repeated bendings. These features endow f-Ni/Fe cells a highly promising candidate for next generation flexible energy storage systems.

## 6.2 Comments and Future Work

### 6.2.1 *Electrochemical Exfoliation of Graphite*

Although electrochemical exfoliation of graphite has proved to be an effective method to prepare high-quality graphene flakes in an economical and environmentally-friendly way, several challenges are still remaining to be addressed: (i) the quality of graphene (size, thickness, defects, etc.) is subjected to the raw materials to some extent; (ii) the production is limited to lab-scale at the moment. Therefore, several further justifications are needed: (i) to investigate the effect of raw graphite materials on the quality of resulting graphene in a qualitative way via employing XPS, XRD, Raman spectroscopy and electrochemical characterization methods; (ii) to design and built equipments that are suitable for large-scaled production, optimize the synthesis conditions further, and evaluate the quality of resulting graphene in terms of size and thickness distribution, defects amount and electrochemical performance.



## **6.2.2 *GF and GF/CNTs Hybrid Film Based Flexible Energy Storage Devices***

The key challenges for flexible power sources lie in (i) the development of deformable electrodes with high energy density, and (ii) the understanding of underlying mechanism. In this thesis, we have developed a new kind of GF/CNTs hybrid film for flexible electrode scaffolds, and demonstrated its applications in several traditional energy storage systems. Although our designs and results are quite attractive, more research work are required to illustrate the underlying mechanism in a qualitative and quantitative way, and optimize electrochemical performance further.

### **6.2.2.1 Design Novel GF/CNTs/CNTs Hybrid Films for Flexible Electrode Scaffolds**

Our results in Chaps. 3, 4 and 5 indicates that the densely grown CNTs could extend the 3D architecture of GF without sacrificing the good ohmic and mechanical contact between them, which provides a high surface-to-volume ratio that allows high mass loading of active materials. Along this line, we try to design a new kind of GF/CNTs/CNTs hybrid films assisted by ALD method in order to increase the active materials loading further. ALD is a powerful tool to deposit nano-sized catalyst on the surface of GF/CNTs hybrid films, forming GF/CNTs/catalysts composites. The GF/CNTs/CNTs hybrid films is then achieved after the second-growth of CNTs on GF/CNTs/catalysts composites.

### **6.2.2.2 Explore the Underlying Mechanism of Flexible Energy Systems**

The electrochemical properties of active materials (e.g., specific capacity, reversibility, rate capability, cycling behavior, etc.) are strongly dependent on the structure and element changes during electrochemical reaction processes [1–4]. Therefore, the establishment of clear relationships between electrochemical and structural/element data is no doubt one key issue for better understanding and further improving the electrochemical performance of electrode materials.

In situ Raman spectroscopy is a convenient and non-destructive tool for studying electrochemical reaction processes within numerous electrodes in aqueous and non-aqueous energy storage devices [5, 6]. Raman spectroscopy has been found to be very sensitive to the state of metal oxide, with the Raman frequencies being dependent on the metallic oxidization state. Therefore, it is particularly suitable for the investigation of underlying mechanism for redox couples involved in many aqueous electrochemical capacitors, or metal-ion rechargeable batteries. Part of our future work will focus on this area.

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